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EXPERIMENTAL CAVITATION
AND FLASHING OF POTASSIUM
FLOWING ADIABATICALLY THROUGH
A VENTURI SIZED AS A BOILER INLET

by Orlando A. Gutierrez and David B. Fenn Lewis Research Center Cleveland, Ohio



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FLOWING ADIABATICALLY THROUGH A VENTURI SIZED AS A BOILER INLET

by Orlando A. Gutierrez and David B. Fenn Lewis Research Center

SUMMARY

Tests were conducted on the adiabatic initiation of vapor in a venturi with a 0.1015-inch (0.2578-cm) throat diameter, with high-purity potassium used as the test fluid. A venturi of this size could be used as a boiler tube inlet device. The inside surface of the venturi was machined and polished to a 6 rms finish. Data were obtained at constant flow rates and inlet temperatures by changing the pressure level in a recirculating loop. Flow rates ranged from 300 to 660 pounds mass per hour (38 to 83 g/sec) at inlet temperatures from 1140° to 1460° F (889 to 1066 K).

The behavior of the venturi in the all-liquid and two-phase states is presented, as well as data for incipient cavitation and flashing. Flow rate in the flashed condition is dependent only on inlet pressure and temperature. Nonequilibrium conditions at incipiency are correlated by a force-balance equation for vapor bubbles with critical radii between 1×10^{-4} and 0.5×10^{-4} inch $(2.54\times10^{-4}$ and 1.27×10^{-4} cm). These radii agree well with the maximum sizes of wall cavities detected by metallographic examination of the venturi inner surface. Some of the throat absolute pressures at incipiency are calculated to be below zero. The addition of an artificial cavity of 0.008 inch (0.020 cm) diameter in the wall at the venturi throat did not have any effect on incipient conditions. It did affect the flashed venturi performance, apparently by inducing vapor into the throat.

The incipient flashing data obtained adiabatically herein are compared with data on incipient boiling obtained with heat addition that are available in the literature for potassium.

INTRODUCTION

This investigation was conducted to study experimentally the conditions at initiation of two-phase flow in liquid potassium flowing adiabatically through a venturi sized as a

boiler tube inlet, as well as the flow behavior in the venturi before and after such an initiation.

Two of the problems encountered with once-through boilers for use in low-specific-weight, Rankine-cycle systems are boiler instability and the tendency of alkali metals used as cycle fluids to support large amounts of liquid superheat. Research has shown that the introduction of large pressure drops at the boiler inlet decreases the feed-system coupling instabilities. As for the second problem, the alkali metals considered as cycle fluids (potassium, sodium, etc.) tend to remain in the liquid phase at temperatures well above saturation temperature. This is caused by their high purity and low gas solubility as well as their ability to wet the walls and flood cavities which otherwise might act as nucleating sites. This characteristic of the alkali metals makes it hard for designers to predict the location in a boiler where the vapor phase will develop, with the possibility that large boiler lengths may become adiabatic.

A cavitating venturi is a converging-diverging nozzle of such size that initially subcooled liquid flowing through it will reach a local static pressure well below its saturation vapor pressure, thus causing the formation of the vapor phase. Such a venturi will have a large pressure drop. It will also force the formation of vapor at a well-determined location. Therefore, a cavitating venturi at the entrance of a boiler tube should aid in the solution of both previously mentioned boiler problems.

This investigation was conducted at the Lewis Research Center. The venturi used had a throat diameter of 0.1015 inch (0.2578 cm) and was machined from type-316 stainless steel to very close tolerances. The inside surface was highly polished. The venturi was tested with and without an artificial cavity at the throat. Tests were conducted on a forced-circulation, well-insulated, closed loop.

Data were obtained over a flow range of 300 to 660 pounds mass per hour (38 to 83 g/sec) and at fluid temperatures from 1140° to 1460° F (889 to 1066 K). Results are presented and discussed for incipient cavitation, incipient flashing, liquid and two-phase performance of the venturi, and effects of the artificial throat cavity. Results obtained in this investigation are compared with the nonadiabatic liquid superheat data for potassium that are available in the literature.

BACKGROUND

Stone and Sekas (refs. 1 and 2) studied the performance of a cavitating venturi as a water-boiler inlet device. They concluded that its use would greatly reduce the feed-system coupling instabilities described by Dorsch (ref. 3). Hammitt and Robinson (ref. 4) examined the flows of water and mercury in a cavitating venturi. Both refer-

ences 2 and 4 state that their flows behaved as "choked" (i.e., flow rate was independent of outlet pressure).

Ruggeri, Gelder, and Moore studied cavitation of water (ref. 5) and Freon-114 (ref. 6) in a large-diameter, small-area-ratio venturi and reported liquid tensions supported by both fluids.

Many researchers have studied the superheating of alkali liquid metals, with most of the investigations done nonadiabatically. The results obtained vary greatly because of the large number of variables affecting this problem. Hsu (ref. 7) presents a theory that predicts bubble initiation in ether, water, and pentane based on the size range of active cavity sites in the wall. Holtz (ref. 8) notes the importance of pressure-temperature history on liquid superheats, and defines factors necessary to make a physical cavity become an active nucleation site. Edwards and Hoffman (ref. 9) present data on the superheating of liquid potassium and sodium obtained in a natural-convection boiling loop. They show how the addition of a series of 0.006-inch- (0.015-cm-) diameter drilled holes reduced the obtainable liquid superheat. Chen (ref. 10) points out the following factors which contribute to the ability of a liquid to maintain superheat without boiling: surface cavities, gas entrapment in the surface, pressure-temperature history of the surface and fluid, and the gas content and impurities present in the liquid. The present authors were unable to find reference to any previous experimental work on boiling initiation in potassium through adiabatic means.

The terms "liquid superheat" and "liquid tension" appear in the literature and should be clarified. Liquid superheat is the temperature increment of the liquid in excess of the saturation temperature at the local pressure. Liquid tension is the pressure decrement of the liquid below the saturation pressure at the local temperature. Both terms denote a nonequilibrium condition in the liquid. The use of one term over the other has been dictated mainly by the experimental process involved and the reporter's point of view. Those studying the change in fluid pressures at constant temperatures use the liquid-tension term. Those changing temperatures at constant pressures tend to use liquid superheat to denote the nonequilibrium state. However, at absolute pressures below zero, liquid superheat becomes infinite and meaningless.

The existence of liquids at pressures below absolute zero, that is, under negative absolute pressure, has long been known. Blake (ref. 11) in his introduction states that under suitable conditions liquids can withstand very considerable <u>negative</u> external pressures without rupturing. He attributes this phenomenon to the considerable magnitude of the intermolecular cohesive forces. Many experimental measurements of these negative absolute pressures in liquid water appear in the literature, among them those by Briggs (ref. 12) and Gavrilenko and Topchiyan (ref. 13). Briggs (ref. 14) also measured negative absolute pressures on such organic liquids as acetic acid, benzine, aniline, carbon tetrachloride, and chloroform.

Two other terms that appear in this report should be defined: "cavitation" and "flashing." In referring to the venturi, the term cavitation is applied when formation and collapse of vapor is indicated, without the venturi deviating noticeably from its liquid flow - pressure-drop characteristics. The term flashing is used when the cavitation causes the pressure-drop characteristics to change appreciably from the liquid behavior.

APPARATUS

Test Facility

A schematic diagram of the equipment used for these tests appears in figure 1. The closed loop had an electromagnetic (EM) pump which forced liquid potassium at rates up to 700 pounds per hour (88 g/sec) through two electric heaters. The heaters had a maximum capacity of 10 kilowatts each and were mounted in series. The potassium then passed through the horizontal test section and returned to the pump, flowing through an air-cooled section. This air-cooled section lowered the potassium temperature to prevent cavitation at the pump inlet. An expansion tank, located above the highest point in the loop, was connected to the system at the cooler inlet. Loop pressure level was controlled through argon and vacuum lines connected to the top of this tank. Flow rate was controlled through a combination of throttle and bypass valves and pump speed control. Type-316 stainless steel was used throughout the loop. Piping size was primarily 0.50 inch outside diameter by 0.060 inch wall thickness (1.27 by 0.152 cm). The loop was heavily insulated except at the air cooler.

In addition, the test equipment incorporated a titanium-filled hot trap for liquid-metal purification. The hot trap was mounted on the pump bypass line. A sample tube that allowed sampling of the potassium while running and a dump tank to hold the potassium prior to fill completed the test loop.

There was an EM flowmeter located on the return line from the test section. The loop was also equipped with pressure and temperature instrumentation to facilitate operation. This instrumentation is not shown.

Test Section

The test section (fig. 1) consisted of two venturis of equal dimensions, mounted in series and separated by a valve. This valve was used for pressure and flow control (PFC). The PFC valve created enough pressure drop to allow the control venturi, lo-

cated upstream of the valve, to operate always above saturation vapor pressure even when the test venturi downstream of the valve was cavitating.

The main purpose of the control venturi was to provide a means of determining the throat pressure in the test venturi without need of instrument penetrations into the throat of the test venturi. Such penetrations might have changed the behavior of the venturi. The schematic diagram of the test section (fig. 2) shows how the test venturi throat pressure was obtained from the measured pressure at the control venturi throat and from the similarity of the two venturis.

The test section also included two flow-straightening assemblies, one ahead of each venturi. These flow-straighteners eliminated any vorticity in the potassium flow approaching the venturis. Details of the flow straighteners are shown in figure 3.

Venturis

The control venturi (fig. 4) and the test venturi (fig. 5) were two of a series of three identical venturis machined to the dimensions shown in figure 4. The inlet nozzle contour followed the dimensions of a 2:1 ellipse. The conical diffuser had an included angle of 11.5°. These two sections blended together tangentially without an appreciable length of constant cross section in between. They were formed from a single rod of type-316 stainless steel by electric discharge machining (EDM). The inside surfaces were lapped to a mirror finish. Measurements of the surface after lapping showed between a 5 and 6 rms finish. The minimum diameter measured between 0.1010 and 0.1020 inch (0.2565 and 0.2591 cm). A value of 0.1015 inch (0.2578 cm) was used as the actual throat diameter for all venturis.

The third venturi in the series was made so that a venturi could be retained in the "as-received" condition. This as-received venturi was used for destructive metallographic comparisons after completion of tests. A water flow calibration was conducted on this venturi also.

The only differences between the control and test venturis were on the penetrations made into each to incorporate instrumentation and inserts.

Control venturi. - Three penetrations were made into the control venturi (fig. 4). These penetrations were 0.04 inch (0.10 cm) in diameter. The holes were drilled before the surface was lapped. As shown in figure 4, the holes were located at the venturi inlet, outlet, and throat. All three holes were connected to pressure-measuring devices. Thermocouples were spot welded to the venturi outside surface at the inlet T_{C1} and the outlet T_{C2} .

Test venturi without artificial throat cavity. - The test venturi was tested first without any artificial throat cavities, as shown in figure 5(a). Only two holes were

drilled through to the inside surface: at the venturi inlet and outlet. Both holes were 0.04 inch (0.10 cm) in diameter and were connected to pressure-measuring devices. The inside surface of the test venturi was unbroken by any penetrations in the zone of reduced area. Four holes 0.070 inch (0.178 cm) in diameter were drilled to within 0.06 inch (0.15 cm) of the inside surface at the locations shown in figure 5(a). Thermocouples T_1 , T_2 , T_3 , and T_4 were spot welded at the bottoms of these holes. In addition, two thermocouples, $T_{\rm in}$ and $T_{\rm out}$, were spot welded to the outside surface of the venturi inlet and outlet, as was done on the control venturi. An accelerometer was mounted at the end of a 1/4-inch- (0.6-cm-) diameter, 10-inch- (25-cm-) long tube. This tube was attached to the test venturi near the throat area.

Test venturi with artificial throat cavity. - The test venturi was modified after the first series of experiments, as shown in figure 5(b). The hole located in the plane of the throat was drilled through and reamed to 0.076 inch (0.193 cm) diameter. A throat cavity insert was placed in this hole, replacing thermocouple T₁. The end of the insert was seal welded to the outside surface of the venturi. This throat cavity insert is detailed in figure 6.

All the machining necessary to install the cavity insert was done with the venturi installed in the loop. In addition to the 0.008-inch- (0.020-cm-) diameter reentrant cavity in the insert, there also was a 0.0005-inch- (0.0013-cm-) wide annular gap between the cavity insert and the hole drilled in the venturi wall after installation. Examination after completion of tests showed that the insert had twisted during mounting. This resulted in a mismatch of the contoured surfaces of insert and venturi. Part of the insert edge protruded into the flow passage as much as 0.005 inch (0.013 cm), while part of it was below surface level.

Research Instrumentation

The pressure-measuring devices were absolute pressure transducers of the unbonded strain-gage type. Their range was 0 to 50 psia (0 to 34.5 $\rm N/cm^2$) with a 0- to 10-millivolt output. All pressure transducers were mounted in a constant-temperature oven held at $190^{\rm O}$ F (361 K). Pressure transducers were connected by potassium-filled lines to the locations shown in figures 1, 2, 4, and 5. The signal from each transducer had two parallel readouts: a null-balance strip recorder and a multichannel oscillograph.

The pressure-recording system was calibrated after the loop was filled with potassium. Calibration was made by applying known gas pressures at the top of the expansion tank with no flow in the system. Gas pressure was measured with a 0- to 100-psia

 $(0-\text{to }68.9-\text{N/cm}^2\text{ abs})$ Bourdon-type gage accurate to 0.1 percent of full scale. Calibrations were performed before and after running the two series of tests. Straight-line, least-squares fit of all calibrations showed a deviation of ± 0.2 psi (0.14 N/cm^2) maximum and ± 0.1 psi (0.07 N/cm^2) average for the strip-recorder readings and double these figures for the oscillograph readings.

<u>Temperatures</u>. - Eight temperatures were measured, as shown in figures 4 and 5: outside wall temperatures at the control venturi inlet T_{C1} and outlet T_{C2} and at the test venturi inlet T_{in} and outlet T_{out} ; and four temperatures T_1 , T_2 , T_3 , and T_4 at the bottom of four holes drilled to within 0.060 inch (0.152 cm) of the inside surface of the test venturi. For the second series of tests, thermocouple T_1 was removed to make room for the cavity insert.

Chromel-Alumel thermocouples were used to measure all temperatures. The thermocouple wire had a diameter of 0.020 inch (0.051 cm) and was purchased to ISA type-K special limit of error ($\pm 3/8$ percent). Thermocouple bare junctions were spot welded to the points of measurement. Outputs were recorded in one null-balance multipoint strip recorder with a range of 0° to 1800° F (255 to 1255 K). The record span was 11 inches (27.9 cm), and the smallest division was 10° F (5.56 K).

Direct, in-place calibration of the thermocouples was not made because of the difficulty of introducing an accurate reference in the loop. However, the test venturi outlet thermocouple T_{out} was compared with the potassium saturation temperature corresponding to the test venturi outlet pressure P_5 on those runs where vapor phase was known to exist at that location. The measured temperature was 6.5° F (3.6 K) lower than the saturation temperature on the mean, with no allowances made for heat losses. In addition, a measure of the scatter between the six thermocouples around the test venturi was obtained by comparing their readings during liquid runs, when the venturi was isothermal. The mean deviations are all within the limit of error of the thermocouple wire. The results of these comparisons are discussed in more detail in appendix B. (Symbols are defined in appendix A.)

Flow. - Flow rate was measured by an electromagnetic (EM) flowmeter located downstream of the test venturi. The liquid-metal flow member of the flowmeter was a type-316 stainless-steel tube with a 0.500 inch (1.27 cm) outside diameter and 0.065 inch (0.165 cm) wall thickness. The maximum field strength was 3307 gauss (0.3307 T) with a variation of 1 percent of the maximum throughout the field. The output of the flowmeter varied between 149 and 153 pounds mass per hour per millivolt (18.8 and 19.3 g/(sec) (mV)) depending on the liquid-metal temperature. The electrical output was recorded on a null-balance strip recorder, as well as in one of the channels of the multichannel oscillograph which was also recording the pressure transducer signals.

The pressure drop across the control venturi, together with the water flow calibration of the as-received venturi, was used as a secondary flow reading for cases where

low-quality vapor flowing through the EM flowmeter distorted its output.

There was no direct calibration of the EM flowmeter. However, the flow rates measured by it and the flow rates obtained from the control venturi agree within 5 percent, as shown in appendix B.

Noise. - A high-sensitivity, general-purpose piezoelectric accelerometer was attached at the end of a 10-inch- (25-cm-) long tube. The accelerometer was capable of measuring vibrations to 1000 g's over the frequency range of 2 to 7000 hertz. The tube was welded to the body of the test venturi in the neighborhood of the throat area. The purpose of the accelerometer was to detect pressure pulses that might indicate the formation and/or collapse of bubbles.

The output of the accelerometer was routed through a charge amplifier to a channel of the multichannel oscillograph which was also recording pressures and flow signals. The signal was also paralleled to an oscilloscope for visual monitoring.

No calibration of this device was attempted, as its purpose was to give qualitative rather than quantitative data.

EXPERIMENTAL PROCEDURE

Two series of tests were made:

- (1) Test venturi without artificial throat cavity (series I)
- (2) Test venturi with artificial throat cavity (series II)

The same experimental procedure was followed for both series, unless otherwise specified. Considerable details are presented because of the possible effects of the pressure-temperature history of the surface and fluid on liquid superheats, as pointed out by Holtz (ref. 8) and Chen (ref. 10). However, only those steps in the procedure which may have bearing on the results are described.

The procedure can be divided into three parts: preoperative, data taking, and postoperative. It is worthwhile to note that operation of the loop was continuous for each series once liquid metal was introduced into the system.

Preoperative Procedure

The preoperative procedure was as follows:

- (1) The empty loop was pressurized with high-purity argon to 3 atmospheres, then evacuated to 0.030 torr. This step was repeated three times.
- (2) The empty loop was pumped down to 0.010 torr, heated to 400° F (477 K), and held under these conditions for 48 hours.

- (3) The potassium in the dump tank was melted and the liquid heated to 400° F (477 K) by trace heaters.
- (4) Liquid potassium was forced into the loop until a predetermined level in the expansion tank was reached.
- (5) The pressure level of liquid potassium was increased to 30 psia (20.7 N/cm^2) by applying argon pressure above the potassium in the inventory tank.
- (6) Liquid potassium was circulated at 700 pounds mass per hour (88 g/sec) and the temperature raised to 1300° F (978 K). Flow was maintained at these conditions for 60 hours for purification purposes. A potassium sample taken after this time showed an oxide concentration of less than 10 parts per million.
- (7) The temperature of the circulating potassium was decreased to 800° F (700 K) and flow stopped. Pressure transducers were calibrated by varying the argon pressure at the inventory tank from 0 to 50 psia (0 to 34.5 N/cm² abs).
- (8) Flow was reestablished. Temperature level and flow rate were brought to those values required for the acquisition of data.

Data-Taking Procedure

The data-taking procedure was as follows:

- (1) All-liquid performance curves of the venturis were obtained. The pressure level was maintained higher than the vapor pressure throughout the loop. Flow rate varied from 120 to 700 pounds mass per hour (15 to 88 g/sec).
- (2) Cavitation and flashing data on the test venturi were obtained. For each set of runs, a given flow rate and temperature were established. Starting with the minimum loop pressure (at the test venturi throat) above vapor pressure, the pressure level in the loop was decreased in small steps by reducing the gas pressure at the inventory tank. During time of change, an oscillograph recording was taken. After each change, a data point was recorded from the oscillograph as well as by readings from the strip recorders. This procedure was continued until cavitation and/or flashing developed. The change in system pressure affected the flow rate in some cases. If so, corrections were made to bring the flow rate and temperature back to the preestablished conditions before the steady-state data points were taken. Sometimes the set of data was ended as soon as flashing developed; at other times, the pressure level was decreased even further. In some series, the pressure level was raised again until all-liquid performance was clearly reestablished. Some "ramped" data sets were also taken. These data differ from the data just described in two respects: the decrease or increase in pressure level was continuous, and the loop was not readjusted when flow rate was affected. During these runs, a continuous oscillograph recording was taken.

(3) Another all-liquid performance curve of the venturis was obtained. After all the desired cavitation data were taken, the first step of the data-taking procedure was repeated. This step was not taken for the first series of tests, the one with the test venturi withoug artificial throat cavity.

Postoperative Procedure

The postoperative procedure was as follows:

- (1) Liquid-potassium temperature was decreased to 800^{0} F (700 K) and flow stopped. The pressure transducers were calibrated again.
- (2) Liquid potassium was forced from the loop into the dump tank by argon pressure. Argon pressure was maintained at 20 psia $(13.8 \text{ N/cm}^2 \text{ abs})$ in the empty loop.
 - (3) The post-test procedure differed in test series I and II.
 - (a) After series I (test venturi without artificial throat cavity), the insulation around the test section was removed. Thermocouple T₁ was pulled out and its blind hole drilled through to the inside of the venturi at the throat, as shown in figure 5(b). This operation was performed while the loop was pressurized above atmospheric pressure with argon. Care was exercised to minimize disturbances to the inside surface. The hole was drilled undersized and then reamed to required size with a series of drills. The cavity insert shown in figure 6 was installed and seal welded to the outside surface of the venturi. The test section was reinsulated; then the preoperational procedure already described was repeated for series II.
 - (b) After series II (test venturi with artificial throat cavity), the test section was cut out of the loop as one piece and capped while still full of argon gas. The control and test venturis were separated in a moisture- and oxygen-free atmosphere. Each of the venturis was placed in a vacuum and heated to evaporate any potassium traces. They were then sectioned to allow examination of the inside surface.

RESULTS AND DISCUSSION

The conditions and nature of the experimental data acquired in this program are summarized in table I. Detailed data for all the runs appear in tables II and III. The runs are listed in the same sequence in which data were acquired. The tabulated data are measured values, with the exception of the dynamic head q, the test venturi throat pressure P_t , the exit thermodynamic quality X, the overall pressure-drop ratio $(P_4 - P_5)/(P_1 - P_3)$, and the saturation pressures P_{vin} and P_{vout} , which are calculated from the measured data. Details of the calculations of q, P_t , and X appear in appendix C.

The results are separated into different sections for discussion purposes as follows:

- (1) General venturi behavior
- (2) Liquid performance
- (3) Flashed performance
- (4) Incipient characteristics
 - (a) Cavitation incipiency
 - (b) Flashing incipiency
 - (c) Comparison with heat-addition-data in the literature
- (5) Metallographic inspection

The effect of the artificial cavity at the venturi throat is discussed under each of these sections.

General Venturi Behavior

Classification of data points is given in the remarks column in tables II and III. The accelerometer output signal and the overall pressure-drop ratio form the basis for this classification. Liquid runs are those where the accelerometer outputs show no noise and the overall pressure-drop ratio of test to control venturi is approximately $1 (\pm 0.15)$. Cavitated runs show appreciable noise but no increase in the overall pressure-drop ratio. Flashed runs have an increase in overall pressure-drop ratio (larger than 1.4). The two remaining categories cover the conditions existing immediately before the appearance of noise (incipient cavitation), and before the change in overall pressure-drop ratio (incipient flashing).

Incipiency data were taken from oscillograms such as the one in figure 7. This particular oscillogram was taken during ramped change between runs 105 and 106. Two sections are shown: one covering the incipient cavitation point (run 105a), the other covering the incipient flashing condition (run 105b). The point where noise starts is obvious from the accelerometer trace, even though flow rate and pressure traces are undisturbed. With a further decrease in pressure, the high noise level becomes fully established until the point of incipient flashing is reached. At this point, the following events occur:

- (1) The high level of noise disappears.
- (2) Flow rate decreases.
- (3) Overall pressure drop in the control venturi $P_1 P_3$ decreases, reflecting the flow rate decrease.
- (4) Overall pressure drop in the test venturi P_4 P_5 increases. The point of incipient flashing, run 105b in this case, consists of the operating conditions existing just prior to these changes.

The general behavior of the venturi without the artificial throat cavity is shown in figure 8 by two typical sets of data. The throat pressure, calculated as shown in appendix C, was plotted against the outlet pressure for constant values of flow rate and inlet temperature after any necessary readjustments were made. In figures 8(a) and (b), the outlet pressure started at a high level, was decreased to a minimum, and then was raised again. The circles represent points taken during the pressure decreases; the squares are points taken during pressure increases. As the outlet pressure decreased. the throat pressure decreased an equal amount. This relation remained unchanged even after the appearance of cavitation. The incipiency of cavitation noise is shown by the first open circle encountered as the outlet pressure decreases. Figure 8 shows that cavitation did not appear until the throat pressure was appreciably below the vapor pressure corresponding to the inlet temperature P_{vin} . This indicated the liquid was under tension, at least in the throat area. Comparison of the outlet pressure P_5 with the value of P_{vin} (superimposed on both ordinates of fig. 8) shows that in one case (fig. 8(a)) cavitation occurred while the venturi outlet pressure was still above the vapor pressure. When the diffuser dimensions and the corresponding dynamic head recovery are taken into account, this means that part of the diffuser was also above vapor pressure. In the other case (fig. 8(b)), the venturi was all liquid even when the outlet pressure was below vapor pressure, which means that liquid tension existed throughout the diffuser. It is also worthy of note that three points in figure 8(b) show cavitation characteristics even though the whole diffuser is under tension.

Further decrease in outlet pressure resulted in a sudden and appreciable increase in throat pressure. After loop conditions were adjusted to restore the established values of flow rate and inlet temperature, any further decrease in outlet pressure did not affect the value of throat pressure, as shown in figure 8(a).

An appreciable hysteresis was encountered when the outlet pressure was increased. Increasing the outlet pressure from the flashed condition had no effect on the throat pressure, as shown by the square symbols in figure 8, until the outlet pressure reached a higher value than the value at which incipient flashing occurred during the pressure decrease. After deflashing, the venturi pressure-drop characteristics returned to original preflashed conditions, with the throat pressure again indicating liquid tension without cavitation when steady-state operating conditions were restored.

The limiting value of throat pressure achieved after flashing was slightly lower than the vapor pressure at inlet temperature P_{vin} . This difference could be the thermodynamic depression necessary to create vapor, as indicated in reference 6, and/or an indication of the vapor conglomeration (of whatever nature) occurring in the diffuser after a certain amount of pressure recovery had taken place.

Similar results for two sets of data for the test venturi with the artificial cavity at the throat are presented in figure 9. Each of these sets is composed of two different ex-

cursions in pressure. The cavitation characteristics for the venturi with the 0.008-inch (0.020-cm) artificial cavity were very similar to the ones obtained for the venturi without an artificial cavity: liquid tensions/superheats were observed, and the inception of cavitation did not change the pressure-drop characteristics. Again, a limiting calculated throat pressure was achieved after flashing. Flashing occurred sharply, as before. Hysteresis between flashing and unflashing points was again present. A major difference between the results in figure 9 and those described in figure 8 for the venturi without the artificial throat cavity was the level of the limiting throat pressure reached. For the venturi with the artificial throat cavity, the calculated throat pressure was higher than the vapor pressure at inlet temperature. This can be explained by the presence of vapor at the throat of the venturi, which would cause the effective minimum flow area to decrease. Therefore, equation (9) of appendix C is no longer applicable to the calculation of the throat pressure of the test venturi for flashed runs.

Another difference observed was that in some cases the venturi returned to a liquidtension (but cavitated) condition after deflashing. This is probably nothing more than an indication of randomness in the behavior of cavitation inception.

In figure 9(a), the point of incipient cavitation for the first decrease in the set (highest open circle) occurs at higher pressures than the second incipiency point (highest open triangle). However, the points of incipient flashing are very close for both excursions. Set 12 (fig. 9(a)) is the first set of cavitating runs obtained after the system was filled with potassium for the second series of tests. The appearance of early cavitation in this set can be the result of residual gas from the fill procedure. This gas, accumulating in large-size cavities, may induce early cavitation. However, these cavities will soon be deactivated, as the gas is transported away without being replenished.

Figures 8 and 9 are composed of data points taken after flow rate and inlet temperature were returned to the preestablished constant values. As such they do not reflect the actual uncorrected changes taking place in pressures, temperatures, and flow, especially during flashing. The best way to describe the behavior of the venturi during an imposed change in outlet pressure is to plot all the venturi variables as a function of time. Such a graph is shown in figure 10. This figure covers the data taken during the ramped change between runs 105 and 106. The pressure, flow rate, and noise traces were taken from a continuous oscillogram, the temperatures from the recorder output. The vapor pressures $P_{\rm vin}$ and $P_{\rm vout}$ are the values corresponding to inlet temperature $T_{\rm in}$ and diffuser outlet temperature $T_{\rm out}$, respectively. The pressure ramp was started at 0 seconds and continued until the venturi flashed (420 sec). At this time, the venturi outlet pressure was not reduced any further.

Figure 10 shows that from 0 seconds (at which time pressure level reduction started) to 330 seconds, all pressures were reduced equally, without any change in flow rate or temperature. The accelerometer trace gave no indication of pressure pulses associated

with the presence of bubbles. At 330 seconds, the throat pressure P_t indicated a large amount of tension. Actually, the indicated value of the throat pressure was below zero absolute pressure. At this time, the accelerometer trace increased in width, indicating bubble formation and/or collapse. This noise level was maintained until 420 seconds. During this interval, the pressures decreased in the same manner as before the appearance of bubbles; the temperatures were not affected, and the flow rate was not altered. Until this time, all the temperatures throughout the test venturi were equal. Flashing occurred at 420 seconds. The test venturi outlet pressure P_5 was the only variable that did not change during flashing as it was directly controlled by the bias gas pressure in the expansion tank. The rest of the pressures at both venturis increased with a jump, the flow rate decreased sharply, the noise level decreased, and the temperatures along the venturi wall took different values.

The decrease in flow rate is caused by the adjustment of the system to the higher pressure loss introduced by the flashed venturi. The reduced flow rate results in lower pressure drops in the all-liquid control venturi (P_1 , P_2 , and P_3). The test venturi pressure loss P_4 - P_5 has increased almost twofold. The calculated throat pressure P_t , which as indicated during the discussion of figure 9 is no longer a true estimate, appears higher than the vapor pressure at inlet temperature. The outlet pressure P_5 corresponds closely to the vapor pressure at the venturi outlet P_{vout} , indicating the presence of vapor at equilibrium conditions at the venturi outlet.

The increase in the temperature of the liquid potassium entering the control venturi T_{C1} is caused by the decrease in flow rate through the constant-heat-input electric heaters. The increase in temperature drop from control to test venturi is also a reflection of the reduced flow rate. The sudden drop occurring between the test venturi inlet temperature T_{in} and the venturi outlet temperature T_{out} is a measure of the thermodynamic depression necessary to produce the amount of vapor resulting from flashing (~1 percent quality at end of transient). The slow decay in the flow rate after flashing appears to be associated with the slow rise in inlet temperature T_{in} .

The nature of the change in the noise level can be explained by assuming that most of the pressure pulses are produced by bubble collapse, rather than formation. Before the appearance of vapor conglomerates, the bubbles are collapsing individually in essentially all liquid surroundings. After flashing, the compressible volume present dampens the pressure pulses.

All the data points obtained for the venturi with and without the artificial cavity at the throat are shown in figure 11. The overall pressure drop P_4 - P_5 is plotted as a function of superficial dynamic head at the throat q.

The nonflashed data, whether all-liquid or cavitated, fall along the solid lines in figures 11(a) and (b). Flashing runs fall to the right of the dashed lines. It was not possible to obtain any data in the region between the solid and dashed lines, because the

system jumped from the liquid line to the flashed area and the reverse. This jump, during the onset of flashing as well as during deflashing, was very sharp and it was not accompanied by oscillations between the two states, even though figure 7 shows small local fluctuations in the pressure traces. Stone and Sekas (ref. 2), performing similar tests in water, did not consistently experience the jump between liquid-cavitated and flashed conditions. Whenever they observed a jump, its magnitude was small. Also, their data at the inception of flashing were highly oscillatory, as a rule. The difference in behavior between potassium and water (as to the irreversibility of the jump during flashing and deflashing) seems to depend on the properties of potassium, which allow large liquid superheats/liquid tensions, with the consequent storage of energy in a metastable condition. Among these properties of potassium are the purity of the liquid phase and the low solubility of gases, which eliminates potential nucleating sites within the liquid bulk; its high surface tension and ability to destroy oxide films from the containing walls, which drowns out most of the potential nucleating sites at the wall; and its high thermal conductivity, which allows the transfer of the stored energy to the vapor phase (once it is formed) with a minimum of temperature drop across the liquid bulk.

Liquid Performance

The solid lines in figures 11(a) and (b) represent the pressure-flow performance of the venturi when it is operating with potassium in the liquid phase. These liquid lines, over the Reynolds number range covered, indicate a constant loss coefficient

$$\frac{\mathbf{P_4} - \mathbf{P_5}}{\mathbf{q}} = \mathbf{C} \tag{1}$$

Equation (1) neglects the difference in dynamic head between the venturi inlet and outlet, even though the two diameters are not equal (see fig. 4). The maximum value of this difference over the flow range studied was about 0.15 psi (0.1 N/cm^2) , which is smaller than the scatter in the pressure readings.

The liquid data for the venturi without the artificial throat cavity (sets 1 to 10, fig. 11(a)) are correlated by

$$\frac{P_4 - P_5}{q} = 0.44 \tag{2}$$

while the liquid data for the venturi with the artificial throat cavity (sets 11 to 20, fig. 11(b)) fit the relation

$$\frac{P_4 - P_5}{q} = 0.50$$
 (3)

which represents about a 13 percent increase in pressure losses over the venturi without the throat cavity (eq. (2)). This increase in losses is attributed to the small protrusion of the cavity insert into the flow channel, as described under Test Section.

It should be noted that the loss coefficient for the control venturi had a constant value of 0.48. This value of 0.48 for the control venturi with the very-sharp-edged pressure tap at the throat fell between the 0.44 obtained for the test venturi without a throat cavity and the 0.50 for the test venturi with the somewhat irregular throat cavity insert.

Flashed Performance

The pressure-flow characteristics of the venturi after flashing were quite different from those during liquid flow conditions. After flashing, the superficial dynamic head at the throat q is no longer a function of the venturi overall pressure drop (fig. 11). The overall pressure drop is now much larger than during the all-liquid operation. Different values of overall pressure drop were obtained for a given value of q.

The difference in behavior shown in figure 11 between the flashed and the liquid data indicates that the relation between venturi upstream and downstream pressures is no longer controlled by liquid loss mechanisms, but by some other independent factor. This independent factor could be the presence of a vapor continuum somewhere in the small flow area of the venturi. This being the case, the flow rate after flashing should become a function of some value of the potassium saturation vapor pressure and the inlet pressure P_4 . Figure 12 shows that the flow rate after flashing is a function of the difference between the inlet pressure P_4 and the potassium vapor pressure corresponding to the inlet liquid temperature P_{vin} . Plots similar to figure 12, but using vapor pressures corresponding to diffuser wall temperature P_{v2} , and outlet temperature P_{vout} , showed that the flow rate did not correlate with these vapor pressures when these were different from P_{vin} . This leads to the possible conclusion that during flashed operation the liquid potassium reaches saturated liquid conditions before vaporizing and the flow rate is determined by the difference between venturi inlet pressure and the vapor pressure at the inlet liquid temperature.

Figure 12 also shows that during flashed operation the relation between flow and inlet overpressure P_4 - P_{vin} is greatly affected by the presence of the artificial cavity

at the throat. This is evidenced by the difference in slope between the two correlating lines.

Figure 13 compares, against superficial dynamic head at the throat, the difference between inlet and throat pressure P_4 - P_t for the liquid data, and the difference between inlet pressure and inlet temperature vapor pressure P_4 - P_{vin} for the flashed data.

For the venturi without the artificial throat cavity, the liquid pressure drop to the throat $P_4 - P_t$ is higher than the inlet overpressure during the flashed runs $P_4 - P_{vin}$, as shown in figure 13(a). Assuming that the liquid potassium is at equilibrium at the flashing location, the slight tension at the throat means that the equilibrium condition occurs downstream of the throat, after some pressure recovery has taken place. From the slope of the two curves in figure 13(a) and the geometric characteristics of the diffuser, and with the additional assumption that the nozzle performance did not change from the liquid condition, a distance of about 0.1 inch (0.25 cm) minimum between the throat and an effective interface location was estimated. This means, of course, that during flashed operation the liquid potassium remained under slight tension (equal to $P_{vin} - P_t$) while going through the venturi throat. Furthermore, the temperature readings at To, located 0.4 inch (1.0 cm) downstream of the throat, show the presence of vapor continuum at this location already, when there is net vapor quality at the venturi outlet. Therefore, the location of the equivalent interface should be between a minimum of 0.1 inch (0.25 cm) downstream of the throat, as indicated by the pressure curves, and a maximum of 0.4 inch (1.0 cm) as indicated by the diffuser wall temperatures.

For the venturi with the artificial throat cavity, the results are reversed, as shown in figure 13(b). The inlet overpressure P_4 - $P_{\rm vin}$ during flashing is higher than the liquid nozzle pressure drop P_4 - P_t for a given value of superficial velocity head. This change can be explained by assuming that the artificial cavity induces vapor into the throat, thereby changing the minimum liquid flow area. Consequently, the superficial dynamic head at the throat q is no longer the maximum velocity head. If it is assumed that (1) the liquid at the throat is at equilibrium and (2) the difference in slope of the curves in figure 13(b) is the measure of the change in throat dynamic head, a throat area reduction of 7.3 percent would explain the results. To indicate the absolute magnitude of this change, it could be expressed as an annular vapor ring thickness of only 0.0019 inch (0.0048 cm) at the throat.

The behavior of the diffuser portion of the venturi during flashing is shown in figure 14. The difference between inlet pressure and inlet temperature vapor pressure $P_4 - P_{vin}$ is plotted as a function of overall pressure drop $P_4 - P_5$ in figure 14(a). The difference between inlet pressure and diffuser outlet vapor pressure $P_4 - P_{vout}$ is plotted in figure 14(b), also as a function of overall pressure drop. The solid symbols in both figures indicate those runs with a measurable temperature depression; that is, where temperature T_2 in the diffuser was lower than the inlet liquid temperature.

Figure 14(a) shows that the diffuser had a net pressure drop $[(P_4 - P_5) > (P_4 - P_{vin})]$ for those data where a temperature drop was measured. This diffuser net pressure drop, occurring with or without the artificial cavity at the throat, is to be expected for the higher fluid velocities associated with an exit vapor phase. As shown in tables II and III, vapor qualities as high as 1.3 percent were obtained at the diffuser exit. The diffuser net pressure drop changed with the values of quality calculated from the temperature depression. For the flashed data in which no temperature depression was observed, the diffuser had a pressure recovery $[(P_4 - P_5) < (P_4 - P_{vin})]$ meaning that very little vapor phase is being generated, and that the flow is returning to the all-liquid condition before leaving the diffuser. The change in magnitude of the pressure recovery indicates that the return to the all-liquid state occurs at variable positions within the diffuser.

The plot of pressure difference between inlet pressure and vapor pressure at outlet temperature P_4 - P_{vout} as a function of overall pressure drop (fig. 14(b)) shows that for the flashed runs where a temperature depression existed, the outlet venturi pressure was at equilibrium with its vapor pressure P_4 - P_{vout} = P_4 - P_5 . For those cases where no temperature depression existed, the outlet pressure P_5 was higher than the vapor pressure at outlet temperature.

The behavior of the flashed venturi can be summarized as follows:

- (1) The overall flow rate is determined by the difference between the inlet pressure and the vapor pressure corresponding to the inlet liquid temperature.
- (2) The overall pressure drop in the venturi determines the conditions of the mixture leaving the venturi. If the back pressure is higher than the vapor pressure at inlet temperature, the vapor phase will collapse someplace in the venturi; if it is lower, it will generate an equilibrium two-phase mixture, with the quality being dependent on the difference between outlet pressure and inlet vapor pressure. During these tests, exit qualities as high as 1.3 percent were measured.
- (3) The location where flashing starts appears to be slightly downstream of the throat in the smooth venturi and at the throat when the artificial cavity is installed at the throat. For the smooth venturi, pressure recovery characteristics locate the interface at least 0.1 inch (0.25 cm) downstream of the throat; the temperature data indicate that it is no more than 0.4 inch (1.0 cm) from the throat.

Incipiency Characteristics

An important aspect of the cavitating venturi as a potassium boiler inlet device is its behavior at the initial appearance of the vapor phase. The maximum amount of liquid tension/superheat supported before incipiency of vapor is of prime importance in deter-

mining how far a cavitating venturi backpressure must be lowered, or its flow rate increased, before two-phase flow is developed.

Two different types of incipiency points were detected during this experimental program:

- (1) Cavitation incipiency: Determined by the output of the accelerometer attached to the venturi body. The sudden increase in amplitude of the "noise" signal was taken as an indication of bubble collapse.
- (2) Flashing incipiency: Determined by the sudden change in pressure-drop characteristics of the venturi. In some instances, as shown in the remarks column in table II, the cavitation and flashing incipiency points coincided; in other cases, cavitation was detected prior to flashing.

The two-phase incipiency results obtained are presented in figures 15 to 17 in plots of pressure at the throat P_t as a function of inlet liquid temperature. This type of presentation permits direct comparison of the data obtained in this project for potassium flowing adiabatically through a variable pressure field with the incipient data obtained by Chen (ref. 10), Edwards and Hoffman (ref. 9), and others, in a constant-pressure field with heat addition.

Cavitation incipiency. - The minimum values of throat pressure P_t obtained before cavitation noise was detected by the accelerometer are plotted in figure 15 as a function of inlet temperature T_{in} . The throat pressures were determined from the venturi liquid characteristics, using equation (9) of appendix C. The results appearing in figure 15 cover both series of runs: with and without the artificial throat cavity. Also individually identified in this figure are the first and second chronological cavitation incipiency points obtained for each series. Superimposed on the data appear two types of reference curves:

- (1) The potassium vapor pressure curve (solid)
- (2) A family of pressure-temperature curves (dashed) representing the liquid pressures necessary to maintain a force balance around vapor bubbles of different radii at thermal equilibrium with the liquid. The liquid pressures for this family of curves were obtained from

$$P = P_{v} - \left(\frac{2\sigma}{r}\right)_{T_{v}}$$
 (5)

for values of r ranging from 1.0×10⁻³ to 1.0×10⁻⁵ inch (2.54×10⁻³ to 2.54×10⁻⁵ cm). The potassium vapor pressure curve, of course, agrees with equation (5) for a value of $r = \infty$.

The following conclusions can be drawn from figure 15:

- (1) Fluid conditions at the throat of the venturi were not at equilibrium at cavitation incipiency. This nonequilibrium condition, for most of the data, fell between the curves obtained from equation (5), with the critical radii between 1.0×10^{-4} and 0.5×10^{-4} inch (2.54×10⁻⁴ and 1.27×10⁻⁴ cm). A few data points did not show this trend. These exceptions are discussed in conclusions 2 and 3.
- (2) The first cavitation incipiency points in each series, with and without the artificial throat cavity, occurred very close to the potassium vapor pressure curve (see runs 4 and 77 in table II). These two points definitely did not follow the depression pattern of the rest of the cavitation incipiency data. This difference in behavior appeared to be caused by the residual argon gas trapped in the surface cavities during fill (see section EXPERIMENTAL PROCEDURE). The residual argon must have accumulated in surface cavities of large size, preventing them from flooding and thus making them active cavitating sites, as indicated by Chen (ref. 10). During the first pressure decrease, the larger-size cavities probably caused cavitation at near-equilibrium conditions. After the first flashing and deflashing cycle, most of the large-size cavities were depleted of gas and were flooded, becoming inactive sites. Therefore, in successive pressure decreases the remaining smaller cavities caused larger decreases in pressure to be necessary in order to trigger cavitation.
- (3) The artificial cavity at the throat of the venturi did not have any effect on the mean value of the liquid tension obtained. This means that in an adiabatic field, where the walls were not hotter than the fluid bulk, neither the 0.008-inch- (0.020-cm-) diameter reentrant hole, nor the 0.0005-inch (0.0015-cm) annular gap between the cavity insert and the drilled hole, were dependable active cavitation sites. However, a few of the incipiency points obtained with the insert (other than the first of the series) approached the $r = 0.5 \times 10^{-3}$ inch $(1.27 \times 10^{-3} \text{ cm})$ line, indicating that the artificial cavity did act occasionally as a nucleating site.
- (4) It can be seen that some points fall at a liquid pressure below absolute zero. These points can be described as having a finite liquid tension, but the corresponding liquid superheat would be infinite and meaningless.

<u>Flashing incipiency</u>. - The results obtained on flashing incipiency are presented in figure 16. The reference curves in this figure are the same as those already described for figure 15. The incipient flashing data consist of the pressure calculated at the venturi throat P_t immediately before the sudden change in venturi pressure-drop characteristics, as a function of inlet liquid temperature. As before, throat pressure was calculated by using equation (9) of appendix C. If the cavitating venturi is to be used as a boiler inlet, its flashing incipiency characteristics are more important than the point where cavitation noise first develops, but without vapor agglomeration.

The following conclusions can be drawn about the flashing incipiency:

(1) Fluid conditions at the throat of the venturi were not at equilibrium at flashing

incipiency. Throat pressures P_t as much as 16.1 psi (11.1 N/cm²) below vapor pressure were measured. This occurred at a 1460° F (1066 K) liquid temperature.

- (2) The point conditions at flashing incipiency also follow the surface-tension curves obtained from equation (5) for a critical radius between 1.0×10^{-4} and 0.5×10^{-4} inch (2.54×10⁻⁴ and 1.27×10⁻⁴ cm). No appreciable difference in the mean value of correlating critical radius between the flashing incipiency data and the cavitation incipiency data can be noted.
- (3) There is no effect at all of the artificial throat cavity on the values obtained for pressure and temperature at flashing incipiency.
- (4) Some of the throat pressures reached at flashing incipiency show large values of negative absolute pressure, as much as -6.5 psia (-4.5 N/cm^2 abs).
- (5) The incipient flashing points (fig. 16), without exception, follow the trend indicated by the constant critical radius lines. Some of the incipient cavitation points (fig. 15), as discussed previously, deviate appreciably from the mean critical radius values. This appears to be the biggest difference between the incipient flashing and the incipient cavitation results.

Comparison of incipiency results with heat-addition data in the literature. - The incipient flashing results obtained in this project are replotted in figure 17, together with other potassium boiling incipiency data available in the literature. The reference curves shown are the same as those used in figures 15 and 16.

A search of the literature for potassium flashing initiation data did not yield any data obtained adiabatically through pressure decreases. A few investigators, however, have published data on the boiling incipiency of potassium with heat addition. Shown in figure 17 are data published by Edwards and Hoffman (ref. 9); Chen (ref. 10); Spiller, et al. (ref. 15); and Grass, et al. (ref. 16). The methods used by these investigators to promote boiling and to determine the point of incipiency are quite varied. Great variation also exists in the type of surfaces used, the range of heat fluxes, the potassium purity, gas content, and fluid velocity, among other factors, as pointed out by Fauske in reference 17. Some of these conditions for the data shown in figure 17 are summarized in the following table:

	Edwards and Hoffman (ref. 9)	Chen (ref. 10)	Spiller, et al. (ref. 15)	Grass, et al. (ref. 16)	This report
Test method	Heat addition	Heat addition	Heat addition	Heat addition	Adiabatic pres- sure decrease
Potassium flow Natural circulation Forced circulation Stagn		Stagnant	Natural and forced circulation	Forced circulation	
Heating method Electric clam-shell heaters around wall		Electric clam-shell heaters around wall	Electric current flowing through wall and liquid; heat generated mostly within fluid	Same as ref. 15	None
Heat-flux range, 16 000 to 37 000; 2 000 to 50 000 Not ap (50 400 to 116 600) (6 300 to 157 500)		Not applicable Not applicable		None	
	type-347 stainless steel; Haynes alloy 25; accor		Not important according to author as it is colder than fluid	Tube; 0.276-in. (0.7-cm) i.d.; 78.7 in. (200 cm) long	Machined venturi, 5 to 6 rms surface finish; 0.1015-in. (0.2578-cm) throat diam; type-316 stain- less steel: (a) As received (b) With 0.008-in (0.020-cm-) diam reentrant throat cavity (EDM)
Determination of superheat			Change in electric potential distribution along test section		Pressure and temperature measurements
Pressure-temperature history	Not given	Detailed	Not given	Not given	Given

The data of Spiller, et al. (ref. 15) on stagnant potassium, show a large scatter, and the results appear to have no relation to the surface-tension curves. The rest of the data appear to follow the surface-tension trends. However, the values of critical bubble radius vary largely from investigator to investigator. The adiabatic flashing data obtained herein seem to agree best with the data obtained by Chen (ref. 10). This result should be expected, because in his tests the fill and testing procedure and the nature of the test surface more closely approximated the conditions of the adiabatic tests in the venturi.

Comparison of our adiabatic results with those of Edwards and Hoffman (ref. 9) shows the difference in effect of relatively large-size cavities at the wall between the heat-addition case and the adiabatic case. With heat addition, the presence of eight 0.006-inch- (0.015-cm-) diameter holes in the wall decreased the superheat at incipiency very markedly. Our adiabatic data, on the other hand, showed no effect whatsoever on incipiency from a reentrant cavity of 0.008 inch (0.020 cm) diameter or the annular gap 0.0005 inch (0.0012 cm) wide around the cavity insert. This indicates that potassium floods cavities of this size. These cavities may become active cavitation sites if heated, but will not do so adiabatically.

It should be noted that Chen's data (ref. 10) indicate a critical radius of 10^{-4} inch $(2.54\times10^{-4} \text{ cm})$, similar to our data; Edwards (ref. 9) suggests a critical radius smaller than 10^{-5} inch $(2.54\times10^{-5} \text{ cm})$ for the as-received surface, while the stagnant potassium data of reference 15 show no critical radius value whatsoever, but indicate very high superheats.

Metallographic Inspection

After completion of the tests, the inside surfaces of the test and control venturis were inspected. Also inspected was the venturi not used in the potassium tests (the asreceived venturi). The results of these inspections appear in figures 18 and 19. The venturis were sectioned longitudinally. Figure 18(a) shows views normal to the diffuser surfaces of the three venturis. This figure shows what was apparent to the unaided eye: the surface finish had changed after approximately 250 hours of operation with potassium. The as-received surface had a high shine, whereas surfaces on test and control venturis had a dull finish.

Larger magnifications (\sim 35×) of the same inside surface of the diffusers are shown in figure 18(b). The as-received venturi diffuser shows circumferential scratches caused by the polishing process. It also shows large-size pits, greater than 4×10^{-4} inch (1.02×10⁻³ cm). Both the polishing scratches and large-size pits are absent from the surfaces of the control and test venturis. This must be attributed to the effect of liquid

potassium flow rather than cavitation or flashing, as the control venturi was not cavitated during operation.

The test and as-received venturis were cross sectioned at the beginning of the diffuser (near the throat). Photomicrographs (fig. 19) were taken of the inside surfaces of the venturis. The inside surfaces shown are perpendicular to the direction of flow. The surface of each venturi was observed under the microscope, and typical cross sections are shown. The inside surface of the test venturi appeared rougher than that of the as-received venturi at this magnification. It shows many cavities in the 10^{-4} - to 10^{-5} -inch $(2.54\times10^{-4}$ - to 2.54×10^{-5} -cm) size range, which coincides with the critical radii curves correlating the data in figures 15 and 16. Very few cavities of this type can be seen on the as-received surface. The cavities appearing on the test venturi surface cover a gamut of shapes: conical, spherical, reentrant. However, they did not penetrate deeply into the wall.

Of secondary importance is the change in structure noted in the type-316 stainless steel. The as-received venturi had a large grain structure with no carbide precipitation. After 250 hours of operation, mostly between 1300° and 1500° F (978 and 1089 K), there was a large amount of intergranular and matrix carbide precipitation. The grain size seemed to have decreased considerably. All venturis were made from the same bar of material and exposed to the same metalworking processes. There is no reason to believe that the structure of the test venturi was different at the start from that shown in figure 14(a).

CONCLUDING REMARKS

The behavior of an adiabatic venturi with subcooled-liquid-potassium feed was studied experimentally before, during, and after the development of two-phase flow. The results indicate that a venturi inlet that will cause flashing of the subcooled liquid into two-phase flow, without oscillations and with large pressure drops, can be designed for a potassium boiler tube. Prior to the start of flashing, a metastable condition with large liquid tensions/superheats may be encountered. After flashing, only a small amount of tension/superheat, if any, will be found, and the total liquid flow rate will be independent of downstream conditions and influenced only by the liquid temperature and inlet pressure.

The large pressure drop at the boiler tube inlet tends to improve boiler stability, as indicated by other investigators. The total flow rate independence from downstream pressure, also noted in water flow by others, should be most advantageous in establishing good flow distribution in multitube boilers, where differences in downstream condi-

tions between the parallel tubes are caused by such factors as mechanical tolerances, poor distribution of heating fluids, and wall deposits.

The lack of oscillations during flashing noted with the potassium venturi is a further advantage, not typically found in water tests by others. The sharpness of the potassium flashing initiation is attributed to the hysteresis encountered between flashing and unflashing conditions. This hysteresis, in turn, is probably a result of the thermophysical properties of potassium, which allow the high local liquid superheats observed prior to flashing. However, this same superheating presents some startup difficulties which must be taken into consideration when establishing operating procedures.

Not evaluated in this study were the nature of the flow patterns obtained with twophase flow or the behavior of the venturi with heat addition.

SUMMARY OF RESULTS

Experimental data were obtained on the flow of subcooled potassium through an adiabatic, smooth-wall venturi with a throat diameter of 0.1015 inch (0.2578 cm). This venturi is in the size range suitable for use as a liquid-metal-boiler inlet device. Data were taken at flow rates ranging between 300 and 660 pounds mass per hour (38 to 83 g/sec) and fluid temperatures from 1140° to 1460° F (889 to 1060 K). Behavior of the venturi in the all-liquid and flashed states, as well as at incipient cavitation and flashing conditions was observed with the following major results:

- 1. Nonequilibrium conditions were measured in the venturi at flashing incipiency. This nonequilibrium consisted of liquid in tension at pressures below the vapor pressure corresponding to the liquid saturation temperature, as much as 16.1 psi (11.1 N/cm^2) at a 1460° F (1066 K) liquid temperature.
- 2. Incipient cavitation and flashing pressures below saturation vapor pressure followed the trends predicted by a force-balance equation across bubbles of critical radii between 1×10^{-4} and 0.5×10^{-4} inch $(2.54\times10^{-4}$ and 1.27×10^{-4} cm). Metallographic inspection of the inside surface of the venturi showed the largest cavities to be in the 10^{-4} to 10^{-5} -inch $(2.54\times10^{-4}$ to 2.54×10^{-5} -cm) range.
- 3. Pressures lower than absolute zero existed at the venturi throat at some flashing incipiency conditions. The largest negative absolute pressure calculated was -6.5 psia $(-4.5 \text{ N/cm}^2 \text{ abs})$.
- 4. Total potassium flow rate through a flashed venturi with subcooled inlet conditions and a particular geometry is determined exclusively by the inlet pressure and the inlet temperature, which determine the vapor pressure at the interface. The effect of the backpressure on the flashed venturi behavior is limited to controlling either the quality

of the two-phase mixture leaving the venturi, or the location in the diffuser where the vapor phase will collapse. Exit vapor qualities as high as 1.3 percent were calculated.

- 5. Neither the unheated reentrant 0.008-inch- (0.020-cm-) diameter artificial throat cavity nor the 0.0005-inch- (0.0013-cm-) wide annular gap had any effect on incipiency conditions. The artificial cavity did appear to induce vapor into the throat area after flashing, thereby producing a larger pressure drop for a given flow rate.
- 6. The data obtained adiabatically in this investigation were compared with data available in the literature for potassium boiling initiation through heat addition. Both types of data show similar trends, except for some data on boiling stagnant potassium of high purity.
- 7. The flow of hot liquid potassium through the venturi for a period of 250 hours changed the surface finish on the type-316 stainless-steel venturi. Large-size pits and polishing marks disappeared, and small cavities of the 10^{-4} to 10^{-5} -inch $(2.54\times10^{-4}$ to 2.54×10^{-5} -cm) diameter range were formed or exposed at the surface.

Lewis Research Center,

National Aeronautics and Space Administration, Cleveland, Ohio, November 10, 1969, 120-27.

APPENDIX A

SYMBOLS

c c ₁	constant dimensional factor in eq. (10) of appendix C, 144 in. 2/ft2;	P_{v2}	potassium vapor pressure corresponding to temperature \mathbf{T}_2
d	10 ⁴ cm ² /m ² diameter at venturi throat, in.; cm	P _{vin}	potassium vapor pressure cor- responding to temperature T _{in}
$^{ m g}{}_{ m c}$	gravitational conversion factor, 4.173×10 ⁸ (lbm-ft)(hr ²)/lbf;	P _{vout}	potassium vapor pressure corresponding to temperature \mathbf{T}_{out}
h	1(kg-m)(sec ²)/N saturated liquid enthalpy of	P ₁	measured pressure at control venturi inlet (fig. 4)
^h fin	potassium at venturi inlet temperature T _{in} , Btu/lbm;	P_2	measured pressure at control venturi throat (fig. 4)
h _{fout}	J/kg saturated liquid enthalpy of	P_3	measured pressure at control venturi outlet (fig. 4)
Tout	potassium at venturi outlet temperature Tout,	P ₄	measured pressure at test venturi inlet (fig. 5)
h _{fg, out}	Btu/lbm; J/kg heat of vaporization of potas-	P ₅	measured pressure at test venturi outlet (fig. 5)
	sium at venturi outlet temperature T _{out} , Btu/lbm; J/kg	q	superficial dynamic head at venturi throat, psi; N/cm ²
N	number of runs	r	bubble radius, in.; cm
P	pressure, psia; N/cm ² abs	${f T}$	temperature, ^o F; K
$\mathbf{P}_{\mathbf{t}}$	pressure at test venturi throat, calculated from the five	T _{C1}	measured wall temperature at control venturi inlet
	measured pressures (eq. (9) of appendix C)	$^{\mathrm{T}}\mathrm{C2}$	measured wall temperature at test venturi inlet
$\mathbf{P}_{\mathbf{v}}$	potassium vapor pressure at saturation temperature T_{v}	T _{in}	measured wall temperature at control venturi outlet
		Tout	measured wall temperature at test venturi outlet

$\mathbf{T}_{\mathbf{v}}$	potassium saturation tempera- ture	W	potassium liquid flow rate, lbm/hr; g/sec
T ₁	measured wall temperature at test venturi, 0.50 in. (1.27 cm) from inlet	w _v	potassium flow rate calculated from venturi characteristics, lbm/hr; g/sec
$\mathbf{T_2}$	measured wall temperature at test venturi, 0.90 in.	X	thermodynamic quality at ven- turi outlet, percent
T ₃	(2.29 cm) from inlet measured wall temperature at	γ	standard deviation as defined by eq. (7), ^O F; K
J	test venturi, 1.30 in. (3.30 cm) from inlet	ρ	potassium liquid density, lbm/ft^3 ; g/m^3
Т4	measured wall temperature at test venturi, 1.70 in. (4.32 cm) from inlet	σ	potassium surface tension, lbf/in.; N/cm

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APPENDIX B

ACCURACY OF TEMPERATURE AND FLOW MEASUREMENTS

As indicated in the Research Instrumentation section of the main text, no direct calibration of the temperature- or flow-measuring devices was attempted. However, indirect observations of the readings obtained give indications of their own validity.

Temperatures

The thermocouple readings of interest are the six around the test venturi (T_{in} , T_{1} to T_{4} , and T_{out}). The data presented in tables II and III allow two comparisons to be made to show the validity of these temperature readings:

- (1) Comparison of T_{out} with the saturation temperature of potassium corresponding to the measured outlet pressure P_5 in those runs which show a net vapor quality leaving the venturi. This comparison measures the accuracy of the thermocouple T_{out} .
- (2) Comparison of the other five thermocouples with T_{out} on the all-liquid runs. These runs are very near isothermal, as the potassium flow rates are large enough to prevent heat losses from creating a large temperature drop along the venturi length. This type of comparison shows the scatter in readings among the six thermocouples.

Comparison of T_{out} with saturation temperature of potassium. - The readings obtained from thermocouple T_{out} are plotted in figure 20 against the values of potassium saturation temperature at the outlet pressure P_5 , for all the runs where net quality at the outlet was observed. Saturation temperatures were obtained from the potassium vapor curve reported in reference 14. The values of the measured temperature T_{out} were 6.5° F (3.6 K) lower on the mean than the saturation temperature. The standard deviation of the mean difference was 3.5° F (1.9 K).

About 3° F (1.7 K) of the mean difference in temperature can be accounted for by heat losses. At the operating temperature level there should be about a 1.5° F (0.8 K) temperature drop across the stainless-steel wall. This would be the result of the heat leakage by conduction through 7 inches of ceramic fiber insulation. An additional 1.5° F (0.8 K) error should be expected from the thermocouple as a result of heat leakage by conduction along the leads. The additional error encountered is well within the combined limit of error of the thermocouple wire and the calibration error of the pressure-measuring device.

As shown in figure 20, the readings with the larger discrepancies are those where the estimated exit quality is smaller than 0.4 percent. It is possible that in these runs

the venturi exit is no longer at saturation, making the comparison not applicable.

Comparison of other thermocouples with T_{out} . - Comparison of the other five thermocouples, T_{in} and T_1 to T_4 , with T_{out} for those runs where the test venturi should be nearly isothermal gives an indication of the relative accuracy of the six thermocouples involved. Thermocouple T_{out} is singled out as the basis for comparison because its absolute accuracy was established from the potassium vapor pressure curve, as already described.

The test venturi should be isothermal during the all-liquid runs, when no change in phase occurs. The only deviation from constant temperature is that created by the heat losses through the insulated walls of the venturi. This small deviation from isothermal conditions along the length of the venturi was estimated for each of the five thermocouple stations. This estimate was obtained by a balance between the heat losses across the venturi wall and the 7 inch (18 cm) thickness of insulation and the temperature drop of the potassium flowing along the venturi. The correction, a function of potassium flow rate and temperature, was applied to each thermocouple reading before it was compared with $T_{\rm out}$.

The results of the comparisons are summarized in figure 21. The mean difference $\overline{\Delta}$ between each temperature and T_{out} is the arithmetic mean of the differences for all the liquid runs

$$\overline{\Delta}_{i} = \frac{\sum (T_{i} - T_{out})}{N}$$
 (6)

where i denotes one of the subscripts in, 1, 2, 3, or 4. The number of all-liquid runs N was 158 for all the thermocouples, except T_1 which was removed early in order to install the throat cavity insert. Only 56 runs were used to evaluate the mean difference between T_1 and T_{out} . As shown in figure 21, the mean differences between T_{out} and the other thermocouples were less than 1.5° F (0.8 K), except for T_3 which had a larger error.

The standard deviation from the mean difference γ was estimated from

$$\gamma_{i} = \left[\frac{\sum (\Delta_{i} - \overline{\Delta}_{i})^{2}}{N}\right]^{1/2} \tag{7}$$

where $\Delta_i = T_i - T_{out}$ and i denotes one of the subscripts in, 1, 2, 3, or 4. As shown in figure 21, the standard deviations range from 1.1° F (0.6 K) for T_4 to 2.2° F (1.2 K)

for T_3 . The distribution of runs for all five deviations is equal, with 73 percent of all readings being within 1γ of the mean difference.

These differences between the six thermocouples are well within the limits of error of the thermocouple wire. The temperature readings reported on all data tables are uncorrected values obtained from the thermocouples.

Flow

No direct calibration of the electromagnetic (EM) flowmeter was attempted. An indication of the reliability of flow rate results is given by comparison of the EM flowmeter readings with the flow rates obtained from the inlet-to-throat pressure drop in the control venturi.

The control venturi was not calibrated directly. However, a flow calibration was run on the as-received venturi using water and a weight tank. Flow coefficients obtained from the water calibration of the as-received venturi, when used with the pressure drops $P_1 - P_2$, obtained in the control venturi during operation, provided a second source of flow measurement. The data shown in figure 22 for the all-liquid potassium runs show that the flow rates from both sources agree within 5 percent throughout the entire operating range.

The flow rates reported in the data tables are the values obtained from the EM flow-meter. For the runs where the EM flowmeter output was distorted, the pressure drop on the control venturi was used to determine the flow rate. In these cases, however, the flow rate was corrected by using the ratio of 0.95 from figure 22.

APPENDIX C

CALCULATION OF TEST VENTURI THROAT PRESSURE, DYNAMIC HEAD, AND THERMODYNAMIC EXIT QUALITY

Test Venturi Throat Pressure

The test venturi throat pressure P_t was obtained from the measured pressures in the control and test venturis. It was not measured directly as no instrument penetrations into the reduced-area section of the test venturi were allowed. In figure 2, pressures P_1 to P_5 are the measured values. The control and test venturis are dimensionally equal. If there were absolutely no difference at all, P_t could be obtained from

$$P_{t} = P_{4} - (P_{1} - P_{2}) \tag{8}$$

However, a small difference between the two venturis existed. Because of the small diameter at the throat of the venturis, even the close specified tolerances allowed a difference in overall performance between the two venturis. This is indicated by the overall pressure-drop ratio $(P_4 - P_5)/(P_1 - P_3)$. If it is assumed that the overall pressure losses are a function of the dynamic head at the minimum throat diameter and that the pressure-drop distribution of the two venturis is similar, the test venturi throat pressure can be calculated from

$$P_{t} = P_{4} - (P_{1} - P_{2}) \frac{P_{4} - P_{5}}{P_{1} - P_{3}}$$
(9)

Equation (9) is applicable to runs where flow is in the liquid phase through both venturis, and to those cavitating runs where the overall pressure-drop ratio does not deviate from the all-liquid value. For the runs where the overall pressure-drop ratio does vary from the all-liquid value, equation (9) was still used to calculate the throat pressure. For these cases, however, the value of the overall pressure-drop ratio from the preceding all-liquid run was used.

Dynamic Head at Venturi Throat

The dynamic head q was calculated as a superficial value at the test venturi throat:

$$q = C_1 \frac{8}{\pi^2} \frac{W^2}{g_c \rho d^4}$$
 (10)

The diameter d used for calculating the superficial dynamic head was the nominal room-temperature value of 0.1015 inch (0.2578 cm). The potassium liquid density was evaluated at the test venturi inlet temperature $T_{\rm in}$. The potassium density, as well as all other thermodynamic and transport properties, was obtained from reference 14.

Thermodynamic Quality at Venturi Exit

The thermodynamic quality of potassium at the venturi exit X was calculated from

$$X = \frac{(h_{fin} - h_{fout}) \times 100}{h_{fg, out}}, \text{ percent}$$
 (11)

The values of enthalphy were all evaluated from the corresponding temperature readings. It was decided, after the results of appendix B were studied, that discrepancies obtained in this way would be smaller than if some enthalpies obtained from pressure readings were compared with others obtained from temperature sources. However, the results obtained at quality values below 0.4 percent border on the value of possible error.

The effect of axial heat conduction along the thick venturi wall on T_{out} was neglected as the flashed data showed very small differences between the readings of thermocouples T_4 and T_{out} . The inlet temperature T_{in} was measured too far upstream of the area where temperature changes occurred to be affected by the gradient.

REFERENCES

- Stone, James R.; and Sekas, Nick J.: Tests of a Single Tube-in-Shell Water-Boiling Heat Exchanger with a Helical-Wire Insert and Several Inlet Flow-Stabilizing Devices. NASA TN D-4767, 1968.
- 2. Stone, James R.; and Sekas, Nick J.: Water Flow and Cavitation in Converging-Diverging Boiler-Inlet Nozzle. NASA TM X-1689, 1968.
- 3. Dorsch, Robert G.: Frequency Response of a Forced-Flow Single-Tube Boiler.

 Presented at Symposium on Two-Phase Flow Dynamics, Technological University of Eindhoven and Euratom, Eindhoven, The Netherlands, Sept. 4-9, 1967.
- 4. Hammitt, Frederick G.; and Robinson, M. John: Choked Flow Analogy for Very Low Quality Two-Phase Flows. Rep. 03424-18-T, Univ. Michigan (NASA CR-75127), Mar. 1966.
- 5. Ruggeri, Robert S.; and Gelder, Thomas F.: Effects of Air Content and Water Purity on Liquid Tension at Incipient Cavitation In Venturi Flow. NASA TN D-1459, 1963.
- 6. Gelder, Thomas F.; Ruggeri, Robert S.; and Moore, Royce D.: Cavitation Similarity Considerations Based on Measured Pressure and Temperature Depressions in Cavitated Regions of Freon-114. NASA TN D-3509, 1966.
- 7. Hsu, Y. Y.: On the Size Range of Active Nucleation Cavities on a Heating Surface.
 J. Heat Transfer, vol. 84, no. 3, Aug. 1962, pp. 207-216.
- 8. Holtz, Robert E.: The Effect of the Pressure-Temperature History Upon Incipient-Boiling Superheats in Liquid Metals. Rep. ANL-7184, Argonne National Lab., June 1966.
- 9. Edwards, J. A.; and Hoffmann, H. W.: Superheats with Boiling Alkali Metals.

 Proceedings of the Conference on Application of High Temperature Instrumentation to Liquid-Metal Experiments. Rep. ANL-7100, Argonne National Lab. (NASA CR-76450), 1965, pp. 515-534.
- 10. Chen, J. C.: Incipient Boiling Superheats in Liquid Metals. J. Heat Transfer, vol. 90, no. 3, Aug. 1968, pp. 303-312.
- 11. Blake, F. G., Jr.: The Tensile Strength of Liquids: A Review of the Literature. Tech. Memo 9, Harvard Univ., Acoustic Res. Lab., June 11, 1949.
- 12. Briggs, Lyman J.: Limiting Negative Pressure of Water. J. Appl. Phys., vol. 21, no. 7, July 1950, pp. 721-722.

- 13. Gavrilenko, T. P.; and Topchiyan, M. E.: Dynamic Tensile Strength of Water. J. Appl. Mech. Tech. Phys., vol. 7, no. 4, July-Aug. 1966, pp. 128-129.
- 14. Briggs, Lyman J.: The Limiting Negative Pressure of Acetic Acid, Benzene, Aniline, Carbon Tetrachloride, and Chloroform. J. Chem. Phys., vol. 19, no. 7, July 1951, pp. 970-972.
- 15. Spiller, K. H.; Grass, G.; and Perschke, D.: Superheating and Single Bubble Ejection in the Vaporization of Stagnating Liquid Metals. Rep. AERE-Trans-1078, United Kingdom Atomic Energy Authority, June 1967.
- 16. Grass, G.; Kottowski, H.; and Warnsing, R.: Boiling of Liquid Alkali Metals. Rep. ANL-Trans-390, Argonne National Lab., Sept. 1966.
- 17. Fauske, Hans K.: Liquid Metal Boiling in Relation to Liquid Metal Fast Breeder Reactor Safety Design. Chem. Eng. Progr. Symp. Ser., vol. 65, no. 92, 1969, pp. 138-149.
- 18. Weatherford, W. D., Jr.; Tyler, John C.; and Ku, P. M.: Properties of Inorganic Energy-Conversion and Heat-Transfer Fluids for Space Applications. Southwest Research Inst. (WADD-TR-61-96), Nov. 1961.

TABLE I. - SUMMARY OF EXPERIMENTAL DATA

(a) U.S. customary units

(b) SI units

										(0) 111			
Set	Runs	Pressure change	Flov	v rate		perature, F	Set	Runs	Pressure change	Flo	ow rate		perature, C
			Mode	Range,	Minimum	Maximum			'	Mode	Range,	Minimum	Maximum
			Ĺ	lbm/hr		Ĺ <u></u>			[g/sec		
	Series I	: Test ven	turi witho	<u>ut</u> artificial	throat cav	ity		Series	I: Test ve	enturi <u>with</u>	out artificial	throat cavi	ty
1	a to g	(a)	Variable	125 to 700	1128	1330	1	a to g	(a)	Variable	15.8 to 88.2	882	994
2	1 to 8	Steps	Constant	635 to 662	1174	1199	2	1 to 8	Steps	Constant	80.0 to 83.4	908	921
3	9 to 19			522 to 533	1142	1193	3	9 to 19		1	65.8 to 67.2	890	918
4	20 to 29			406 to 410	1210	1230	4	20 to 29			51.2 to 51.7	928	939
5	30 to 36		1 1	515 to 527	1458	1462	5	30 to 36			64.9 to 66.4	1065	1068
6	37 to 40			443 to 447	1430	1460	6	37 to 40			55.8 to 56.3	1050	1066
7	41 to 55			493 to 498	1312	1325	7	41 to 55			62.1 to 62.7	984	991
8	56 to 68	\	}	370 to 375	1311	1330	8	56 to 68	\	₩ .	46.6 to 47.3	984	994
9	69 to 70	Ramp		493 to 445	1221	1261	9	69 to 70	Ramp		62.1 to 56.1	934	956
10	71 to 72	Ramp		498 to 398	1349	1375	10	71 to 72	Ramp		62.7 to 50.1	1005	1019
	Series	II: Test ve	enturi <u>with</u>	artificial t	hroat cavi	ty		Serie	s II: Test	venturi <u>wi</u>	th artificial th	roat cavity	7
11	h to r	(a)	Variable	119 to 600	1346	1388	11	h to r	(a)	Variable	15.0 to 75.6	1003	1026
12	73 to 104	Steps	Constant	483 to 489	1289	1321	12	73 to 104	Steps	Constant	60.9 to 61.6	971	989
13	105 to 107	Ramp		490 to 368	1308	1345	13	105 to 107	Ramp		61.7 to 46.4	982	1003
14	108 to 123	Steps	Constant	355 to 363	1240	1271	14	108 to 123	Steps	Constant	44.7 to 45.7	944	961
15	124 to 144			355 to 363	1301	1318	15	124 to 144		1	44.7 to 45.7	978	988
16	145 to 176			352 to 362	1408	1445	16	145 to 176			44.4 to 45.6	1038	1058
17	177 to 204			478 to 485	1391	1418	17	177 to 204			60.2 to 61.1	1028	1043
18	205 to 214	♥	\ \	421 to 429	1398	1411	18	205 to 214	♦	\	53.0 to 54.1	1032	1039
19	215 to 219	Ramp		424 to 427	1390	1410	19	215 to 219	Ramp		53.4 to 53.8	1028	1039
20	s to x	(a)	Variable	129 to 660	820	949	20	s to x	(a)	Variable	16.3 to 83.2	711	783

^aNot applicable, all-liquid run.

TABLE II. - DETAILED DATA FOR VENTURI WITHOUT ARTIFICIAL THROAT CAVITY (SERIES I)

(a) U.S. customary units

Set	Run	Flow	Dynamic	1	Con	rol vent	uri					-	rest ven	turi				Noise	Pressure-	Vapor	Vapor	Exit	Remarks
		rate. W.	head,		Pressure		Tempo	rature,		Pressu	re,		_	Tempe	erature,			indica -	drop	pressure	pressure	quality, X,	
-		lbm	q.		psia		(F P		psia				(°F			tion	P ₄ - P ₅	at T _{in} ,	at T _{out} ,	percent	
		hr	·	Inlet,	Throat,	Outlet,	Inlet,	Outlet,	Infet,	Outlet,	Throat,	Inlet,		Distance (rom inlet		Outlet,		$\frac{4}{P_1} - \frac{5}{P_3}$	P _{vin} ,	vout '		
-	1		ļ	P,	P ₂	Р3	T _{C1}	T _{C2}	P ₄	P ₅	Pt	T.					Tout		1 1 3	psia	psia		
				1 '	٤	J	CI	C2	7	J	`	""	0.5 in.,	0.9 in.,	1.3 m.,	1.7 in.,	out					:	
						L							T ₁	T ₂	Т3	T ₄		ļ			<u> </u>		
1		580	21.1	48.5	24.6	38.4	1342	1342	36.6	27.9	16.0	1330	1330	1330	1330	1330	1330	None	0, 87	10.3	;		All-liquid flow
	b	125	. 9	26.9	25.8	26.3			26.3	25.9	25.3	1202	1202	1202	1202	1202	1201		. 54	4.9			calibration
	i C	255 375	3.9	30, 1	25.8 25.6	28.2 31.0	1140	1140	27.9	26. 2 26. 6	24, 2 22, 0	1128	1128 1159	1128 1159	1128 1159	1128 1159	1128		. 86 . 85	3.0			
	'd e	494	8.5 14.8	35.4 42.8	25, 9	35.5	1170	1170 1176	30.3	28.0	19.6	1168	1168	1168	1168	1170	1157	ļ	.87	3.7 3.9			
	f	610	22,6	50.9	25.0	39.9	1195	1194	38.0	28.5	15.7	1188	1188	1188	1188	1189	1187		. 86	4,4			
	g	700	30.2	58. 2	23, 8	43.7	1248	1248	41.3	28.9	11.8	1240	1240	1240	1240	1241	1240	†	. 86	6, 1			. •
	ı	662	26.8	56, 2	25, 8	43.3	1209	1206	39.1	28. l	13. 1	1199	1199	1200	1200	1200	1198	None	0.86	4,8		 	Liquid
-	2	662	26.8	53, 6	22,9	40.7	1205	1203	36, 4	25.3	10.0	1196	1196	1198	1198	1199	1197	None	. 86	4. 7			Liquid
	3	659	26,6	50, 6	20, 1	37.8	1200	1200	33.6	22, 5	7. 2	1190	1190	1191	1191	1192	1190	None	. 86	4. 5			Liquid
	4	655	26.2	47.5	17.4	35.0	1195	1194	30, 7	19.7	4.4	1187	1187	1188	1188	1189	1188	High	. 87	4.5			Incipient cavitation
	5	655	26.2	45, 3	15. 1	32,9	1193	1191	28.7	17.6	1.7	1184	1184	1185	1185	1185	1184	Ì	. 89	4.4			Cavitated
	6	659	26, 5	43.3	13.1	30.9	1191	1190	26.7	15.7	0.0	1183	1183	1184	1184	1185	1186		. 88	4.4			Cavitaled
	7	654	26.0	40.0	9.8	27.4	1188	1187	23.2	12. 4	-2.9	1176	1176	1178	1178	1179	1177	¥	. 87	4.1		1	Cavitated
	7a 8	654 635	26, 0 24, 5	36.6	6.4	24.1 29.8	1183	1181	19.7	8.9 9.2	-6.5 1.8	1174 1174	1174	1173	1174	1175	1173	Medium Medium	. 86	4.1			Incipient flashing
			24. 3	41.8	13.5	29.0	1103	1101	20.0	9.2	. 1.0	1174	1114	1173	11/4	1175	1173	Medium	1, 40	4. 1	4.1	·	Flashed
3	9	527	16.9	41.1	21.5	32.8	1200	1200	30.0	23.0		1190	1190	1190	1190	1191	1190	, None	0.84	4.5			Liquid
:	10	-		37.3	17, 7	29.0	1202	- 1	26.2	19.2	9.5		- 1		ļ	1	1189		. 85	l	·		
	11			35.1	15.5	26.8	1201	1	24.1	17.0 15.8	7.3 6.4	.	Ţ	Ĺ	1	. [1190 1191	į l	.86		1		
	12 13			34.0 32.2	14.3 12.6	25. 6 23. 9	1201	¥ 1201	21.2	14.0	4.2	1191	1191	1191	1191	1192	1190	ļ v	.86	4.6		1	(]
	14	ł		30, 2	10. 5	21.8	1202	1201	19. 1	12.0		1191	1191	1191	1191	1192	1189	Low	. 85	1.0			Incipient cavitation
	15	525	16.8	28.8	9.5	20.7	1203	1202	18.0		1.0	1192	1192	1192	1192	1194	119)	High	. 88	!			Cavitated
	16	524	16.8	27.6	8.3	19.4	1203	1202	16.7	9.7	. 4	1193	1192	1192	1192	1194	1192	High	. 84	;			1 1
	. 17	522	16.7	26.0	6,6	17.6	1203	1202	14.9	7.9	-1.9	1192	1192	1192	1192	1194	1192	High	. 84				
	18	530	17. 1	25.5	1	17.1	1200	1200	14.3	7.0	-3.2	1191	1191	1191	1191	1191	1190	Medium	. 87	7		!) •
	18a		17.1	23.6		15.3	1.50	1150	12.4	5, 2	-4.7	1185	1141	1141	11111	1141	1120	Medium	: .87	4.4	i a a	·	Incipient flashing
	119	533	17.2	29,5	9, 7	21.1	1150	1150	18. 2	4.8	. 6	1142	1141	1141	1141	1141	1139	Medium	1.59	3. 2	3.2	:	Flashed
	20	407	10.2	36.9	25.8	32.1	1224	1222	28.2	23.8	18.1	1210	1210	1210	1210	1211	1212	None	0.90	5. 1		:	Liquid
	21	409	10.3	24.9	13.6	20.0	1229	1226	16. L	1	5.7	1211	1212	1212	1212	1215	1214		.91	5.2			1 1
	22	407	10.2	21.0		16. 2	1229	1226	12.3	7.9	2.0	1214	1215	1215	1215	1217	1217		. 93	5. 3			
	23	, 406 I	10.1	19.5		14.7	1229 1230	1226	10,8	6.4	.7	1215	1215 1215	1215 1216	1215	1219	1219 1219	1	. 90	5.3		:	1 1
	25		i [17.9 17.5		12.7	1235	1232	8.8	4.8	-1. 3	1220	1213	1220	1210	1219 1220	1219	High	.92	5.3			Incipient cavitation
	26		! [17.2		12.2	1245		8.3	4.0	-1.3	1230	1231	1231	1231	1231	1230	High	.86	5.8		1	Cavitated
	26a	j ∳		17.0		12.5			8.3	1	-2.0	1225						Medium	. 96	5. 6			Incipient flashing
:	27	410	10, 3	22.7	11.6	17. 9	1235	1235	14.0	1	4.3	1220	1221	1219	1219	1219	1220	Medium	1.84	5. 5	5, 5		Flashed
i	28	406	10.1	22.7	1	17.9	1232	1230	14.0	6.4	4.2	1219	1219	1219	1219	1219	1219	Medium	1, 56	5. 4	5.4		Flashed
	29	409	10.3	23.0	11.6	18.0	1230	1230	14.0	9.6	3.9	1218	1219	1219	1219	1220	1220	None	. 89	5.4			Liquid

								-														
5 30	527	17.9	49.7	30.3	41.4	1473	1472	35.0	27.6	17.8	1456	1455	1456	1455	1456	1455	None	0.89	19.7			Liquid
31	526	17.8	45, 3	26.0	37.1	1477	1475	30, 7	23.2	13. 1	1461	1460	1460	1460	1462	1460	None	. 92	20.1			Liquid
32	526	17.8	42,4	23, 0	34.2	1476	1475	27.8	20.3	10. 1	1458	1459	1460	1460	1462	1461	None	. 91	20.1			Incipient cavitation
33	521	17.5	39.0	20. 1	31.0	1478	1478	24.7	17.4	7.5	1461	1462	1462	1463	1464	1462	High	.91	20.3			Cavitated
34	520	17.4	38, 2	19, 2	30, 1	1478	1478	23.8	16.5	6.8	1462	1462	1463	1465	1466	1463	High	. 89	20.3			Cavitated
35	520	17.4	36.7	18.0	28.7	1481	1480	22, 5	15. 2	5.6	1464	1464	1466	1466	1468	1467	Medium	. 90	20, 5			Cavitated
36	515	17. 1	34.9	16, 3	26, 9	1478	1477	20.8	13.6	4.0	1460	1460	1461	1463	1464	1463	Medium	. 90	20.1			Incipient flashing
6 37	447	12.8	42, 1	28.1	36.0	1489	1488	31.4	18.9	18.6	1461	1462	1448	1439	1439	1438	Medium	2,00	20.3	18.2	0, 51	Flashed
38	446	12.7	40.2	26.4	34.3	1450	1449	29.7	18, 4	17. 1	1431	1431	1431	1431	1432	1431	Medium	1.93	17.6	17.6		Flashed
39	443	12.5	39.9	26.3	34, 1	1452	1450	29.6	20.9	17.1	1431	1432	1432	1434	1435	1435	High	1.48	17.7	17.9		Flashed
40	446	12.7	37.5	23.7	31.6	1448	1446	27.0	21.6	14.3	1430	1429	1430	1430	1432	1431	None	.92	17.4			Liquid
7 41	498	15, 5	51.3	33.9	43.8	1339	1338	36.6	29, 5	20.2	1324	1322	1322	1321	1325	1323	None	0,94	9.9			Liquid
42	495	15. 3	42.0	24, 5	34, 3	1338	1338	27, 1	20, 0	11.1	1321	1320	1320	1320	1321	1321	1	.92	9.8			Liquid
43	1	1	37.7	20. 3	30.1	1332	1332	22.8	15.7	6.6	1312	1312	1312	1310	1315	1316		. 93	9.3			1 1
44	11		35.7	18.3	28.1	1334	1335	20.8	13, 6	4.3	1319	1319	1319	1319	1320	1319	1 1	.94	9.7			↓ ♦
44a	Ш	1	33.6	16. 2	26.0			18.6	11.6	2. 4	1319						Medium	.92	9.7			Incipient flashing and cavitation
45	\ ♦	♦	39.4	21.7	31.5	1335	1335	24.6	10.3	8. 1	1317	1316	1316	1314	1318	1316	1	1, 82	9.5	9.5		Flashed
46	494	15. 2	38.9	21.6	31.3	1335	1335	24. 1	10.1	8.0	1316	1316	1315	1312	1315	1315		1.85	9.5	9.5		
47	495	15.3	38.9	21, 4	31.3	1335	1335	24.0	9.1	7.6	1311	1311	1302	1299	1300	1299	†	1,96	9.3	8.6	0, 27	
48	495	15.3	38.4	20.9	30.6	1342	1340	24.3	8.6	7.9	1319	1319	1309	1290	1290	1290	Low	2.02	9.7	8.2	. 64	1
49	497	15.5	37.9	20.6	30.3	1343	1342	24.4	8.6	8, 2	1321	1320	1310	1290	1290	1289		2,07	9.8	8.1	. 69	i [
50	496	15.4	36.3	18.9	28.8	1345	1342	24.6	8.6	8.3	1321	1320	1310	1290	1289	1288		2. 14	1	8.1	. 71	1 1
51	493	15.2	38.5	21.1	30.9	1345	1345	24.4	8.8	8.1	1320	1320	1310	. 1291	1289	1289	l 🕴 🔝	2.05		8.1	. 66	l
52	11	15.3	39.0	21.5	31.3	1342	1342	24.8	10.4	8.5	1322	1321	1321	1319	1322	1320	Medium	1.86		9.8		1 I
53	11	1	38.9	21.5	31.3	1345	1345	25.0	13.2	8.7	1325	1325	1325	1325	1329	1328	High	1.54	10.0	10, 2		} *
54	🕴		35, 0	17.9	27.4	1342	1340	21.0	14.0	5. 2	1324	1322	1322	1321	1329	1327	None	. 93	9.9			Liquid
55	495	} 7	45. 5	28. 1	37.8	1340	1338	31.6	24.6	15.8	1321	1320	1320	1320	1321	1320	None	. 91	9.8			Liquid
8 56	373	8.7	36.0	25, 8	31.5	1351	1350	28. 1	23.9	18.4	1330	1329	1329	1329	1330	1329	None	0, 96	10. 3			Liquid
57	370	8.6	27.8	18. 1	23.5	1352	1350	20, 2	16, 1	11.1	1330	1330	1330	1329	1330	1330	1	.94	10, 3			i i
58	370	8.6	23. 2	13.4	18.9	1347	1345	15.7	11.6	6.3	1326	1325	1325	1322	1325	1323		. 96	10.0			1 1
59	373	8.7	21.5	11.7	17.2	1350	1350	13.9	9.8	4.6	1326	1325	1325	1324	1329	1326		.94	10.0			} }
60	373	1 1	19.7	9.9	15.3	1342	1342	12.1	8.0	3.0	1321	1320	1320	1320	1321	1320		, 93	9.8) †
61	372		17.9	8.0	13, 5	1347	1345	10. 1	6.0	. 9	1323	1322	1322	1321	1325	1323	None/High	. 93	9.9			Incipient cavitation
62	11		17.7	7.9	13.4	1342	1340	10.2	6.0	. 8	1320	1320	1320	1319	1321	1320	High	.96	9.8			Cavitated
63) †	17.3	7.3	13.1	1342	1340	9.5	5.4	3	1320	1320	1320	1320	1321	1320	Low	. 98	9.8			Incipient flashing
64		8.6	24.6	14.9	20.3	1342	1340	17.0	7.3	7.7	1311	1310	1292	1270	1266	1264	1 1	2, 23	9.2	7.1	1.03	Flashed
65	11	8.6	24.1	14.3	19.8	1343	1343	16.9	7.5	7.9	1312	1312	1293	1272	1268	1266		2.33	9.3	7.1	1.00	
66	1	8.6	25.7	15.7	21.3	1345	1345	17.3	7.5	7. B	1312	1313	1298	1273	1272	1271	🕴	2, 25	9.3	7.3	. 89	
67	375	8.8	27.7	17.7	23.2	1342	1340	17.4	9.0	7.7	1315	1315	1303	1295	1298	1297	Medium	1.86	9.4	8.5	. 39	[. Y
68	375	8.8	27.3	17. 2	22.9	1341	1340	17. 3	12.7	7, 3	1321	1320	1319	1318	1320	1320	None	. 96	9.8			Liquid
9 69	493	14.9	42.8	25, 4	35.2	1243	1240	26, 9	20.0	11, 2	1221	1222	1223	1222	1225	1223	None	0, 90	5, 6			Liquid
69a	493	14.9	31,9	14. 5	24, 5			16. 1	8.9	-, 8	1239						High	.97	6.2			Incipient cavitation Pressure
69b	493	14.9	31.1	13.9	23.8			15.4	8.5	9	1248						Low	. 95	6.4			Incipient flashing ramp
70	445	12.3	31.9	17.6	25. 6	1281	1279	18.7	7.4	5.7	1261	1260	1260	1258	1261	1260	Low	1.80	6.9	6.9		Flashed
10 7	400	15.	40.0	20.5	20.0	1070	1272	21 0	24.0	15.0	1250	1955	1350	1353	1358	1356	None	0.92	11, 9			Liquid
10 71	490	15.1	46.8	29.5	39.3	1373	1373	31. 2 19. 2	24. 2 12. 2	15. 2 2. 7	1356 1349	1355	1358	1353	1358	1356	None High	.96	11.9			Incipient cavitation Pressure
71a	490 490	15, 1 15, 1	34.6 32.0	17. 4 14. 8	27.3			16.5	9.5	2.7	1349						Medium	.96	11.4			Incipient flashing ramp
71b	398	10.0	33.0	21.5	28.0	1410	1408	22.6	10.4	11.9	1375	1375	1355	1328	1324	1322	Low	2.44	13, 3	9,9	1. 15	Flashed
	1			21. 3	20.0	1410	1400	22.0	10.4	11.0	1010	2010	1000	1010	1021	1000						,
Shown	only for	r flashed	runs,																			

(b) SI units^a

Set	Run	Flow	Dynamic		Cor	ntrol ven	turi					———	Test ver	ıturi				Noise	Pressure-	Vapor	Vapor
		rate, W, g/sec	head, q, N/cm ²		Pressur N/cm ² a			rature,		Pressur N/cm ² a				•	erature, K			indica - tion	drop ratio, P ₄ - P ₅	pressure at T _{in} , P _{vin} ,	pressure at T _{out} , P _{vout} ,
				Inlet,	Throat,	Outlet,		Outlet,	Inlet,	Outlet,	Throat,	Inlet,	I	Distance i	rom inle	 t	Outlet.		$\frac{4}{P_1} - P_3$		N/cm ² abs
				P ₁	P ₂	P ₃	T _{C1}	T _{C2}	P ₄	P ₅	P _t	T _{in}	1.3 cm,	2.3 cm, T ₂	3.3 cm, T ₃	4.3 cm, T ₄	Tout				
1	a b	73. 1 15. 8	14, 5	33.4 18.5	17.0 17.8	26.5 18.1	1001	1001	25. 2 18. 1	19. 2 17. 9	11.0 17.4	994 923	994 923	994 923	994 923	994 923	994 923	None	0.87	7. 1 3. 4	
	c d	32. 1 47. 3	2.7 5.9	20.8	17.8 17.7	19, 4 21, 4	889 905	889 905	19, 2 20, 9	18, 1 18, 3	16.7 15.2	882 899	882 899	882 899	882 899	882 899	882 898		. 86 . 85	2. 1 2. 6	
	e f	62, 2 76, 8	10.2 15.6	29.5	17.9	24. 5 27. 5	911 919	909 919	23.7 26.2	19.3 19.7	13. 5 10. 8	904 915	904 915	904 915	904 915	905 916	904		. 87	2.7	
	g	88.2	20.8	40. 1	16.4	30.1	949	949	28.5	19.9	8.1	944	944	944	944	945	944	+	. 86	4.2	
2	1 2	83.4 83.4	18.5 18.5	38.7 37.0	17.8 15.8	29.9 28.1	927 925	925 924	27.0 25.1	19.4 17.4	9.0 6.9	921 920	921 920	922 921	922 921	922 921	921 920	None None	0.86	3.3 3.2	
	3 4	83.0 82.5	18.3 18.1	34.9 32.8	13.9 12.0	26. 1 24. 1	922 919	922 919	23.2 21.2	15.5 13.6	5. 0 3. 0	916 915	916 915	917 915	917 915	918 916	916 915	None High	. 86 . 87	3. 1 3. 1	
	5 6	82.5 83.0	18.1 18.3	31.2 29.9	10.4 9.0	22, 7 21, 3	918 917	917 916	19.8 18.4	12.1 10.8	1, 2 0	913 913	913 913	914 913	914 913	914 914	913 914		. 89 . 88	3.0	
	7 7a	82.4 82.4	17.9 17.9	27.6 25.2	6.8 4.4	18.9 16.6	915	915	16.0 13.6	8.5 6.1	-2.0 -4.5	909	909	910	910	910	909	Medium	. 87 . 86	2.8 2.8	
	8	80.0	16.9	28.8	9.3	20.5	913	911	20.7	6.3	9.3	908	908	907	908	908	907	Medium	0.84	2.8 3.1	2.8
3	10	66.4	11.7	28.3 25.7 24.2	14.8 12.2 10.7	20.0	923	922	18. 1 16. 6	13.2	6.6 5.0			1			916 916		.85	.	
	11			23.4	9.9	17.7		923	15.8 14.6	10.9	4.4	917	917	917	917	918	917 916		. 84	3, 2	
	13 14			20.8	7. 2	15.0	924	323	13.2	8.3	1.7	917 918	917 918	917	917 918	918 919	916 917	Low	.85	.	
	15 16	66. 2 66. 0	1	19.9	6. 6 5. 7	14.3 13.4 12.1	924 924 924		11.5	6.7	.3	918 918	918 918	918 918	918 918	919 919	918 918	High High	. 84 . 84		
	17 18	65.8	11.8	17.9		11.8	922	922	9.9	4.8	-2.2	917 914	917	917	917	917	916	Medium	. 87	3, 0	
	18a 19	66.8 67.2	1	16.3 20.3	2.6 6.7	14.5	894	894	12.5	1	.4	890	889	889	889	889	888	Medium	1. 59	2, 2	2.2
4	20 21	51.3 51.5	7.0	25. 4 17. 2	1	22. 1 13. 8	935 938		19.4 11.1		12. 5 3. 9	928 928	928 929	928 929	928 929	928 930	929 930	None 	0.90 .91	3.5 3.6	
	22 23	51.3 51.2	7.0	14.5 13.4	6,8	11.2 10,1	938 938	1	8, 5 7, 4		1.4	930 930	930 930	930 930	930 930	931 933	931 933		. 93	3.7 	
	24 25			12.3 12.1	4. 7 4. 4	9.0	939 941	1	6. 4 6. 1	1	-, 6 -, 9	930 933	930 933	931 933	931 933	933 933	933 933	♥ High	. 92 . 92	↓	
	26 26a			11.9 11.7		8. 4 8. 6	947	947	5. 7 5. 7		9 -1. 4	939 936	939	939	939	939	939	High Medium	. 86	4.0 3.9	
	27 28	51. 7 51. 2		15.7 15.7		12.3 12.3	942 940	1	9.7 9.7	1	3.0 2.9	933 933	934 933	933 933	933 933	933 933	933 933	Medium Medium	1.84 1.56	3.8 3.7	3.8 3.7
	29	51.5	7.1	15.9	8.0	12.4	939	939	9.7	6.6	2,7	932	933	933	933	933	933	None	. 89	3.7	

5	30	66,4	12.3	34.3	20.9	28, 5	1074	1073	24, 1	19.0	12, 3	1064	1064	1064	1064	1064	1064	None	0.89	13, 6	
1	31	66.3	12.3	31, 2	17.9	25, 6	1076	1075	21, 2	16.0	9,0	1067	1066	1066	1066	1068	1066	None	.92	13. 9	
1	32	66.3	12.3	29.2	15. 9	23, 6	1075	i	19, 2	14.0	7, 0	1065	1066	1066	1066	1068	1067	None	.91	13.9	
1	33	65, 6	12.1	26.9	13.9	21.4	1076	l	17.0	12.0	5, 2	1067	1068	1068	1068	1069	1068	High	.91	14.0	
	34	65.5	12.0	26.3	13, 2	20, 8	1076	1076	16.4	11.4	4,7	1068	1068	1068	1069	1070	1068	High	.89	14.0	
	35		12.0	25, 3	12. 4	19.8	1078	1078	15. 5	10.5	3, 9	1069	1069	1070	1070	1071	1070	Medium	.90	14. 1	
ĺ		65. 5						1	I .	9.4		1	1066	1070	1070	1069	1068	Medium			
L	36	64.9	11.8	24.1	11, 2	18.5	1076	1076	14.3	9,4	2,8	1066	1000	1001	1008	1009	1008	Medium	. 90	13, 9	
6	37	56.3	8.8	29.0	19.4	24.8	1083	1082	21, 7	13.0	12.8	1067	1068	1060	1055	1055	1054	Medium	2.00	14.0	12.5
	38	56.2	8.8	27.7	18.2	23.6	1061	1060	20.5	12.7	11,8	1050	1050	1050	1050	1051	1050	Medium	1.93	12.1	12, 1
Ι,	39	55.8	8.6	27.5	18. 1	23.5	1062	1061	20.4	14.4	11.8	1050	1051	1051	1052	1053	1053	High	1.48	12, 2	12, 3
	40	56.2	8.8	25, 9	16.3	21.8	1060	1059	18.6	14.9	9,9	1050	1049	1050	1050	1051	1050	None	. 92	12.0	
7		20.7	10.7	05.4	23, 4	30, 2	999	999	25, 2	20, 3	13, 9	991	200		200	201	200	None	0.04		
"		62.7	10.7	35.4		23.6	999	999	18.7	13,8	7.7		990	990	989	991	990	None	0.94	6.8	
	42	62.4	10.5	29.0	16.9	1			1 3			989	989	989	989	989	989		.92	6.8	
ÎΙ	43		1 1	26, 0	14.0	20.8	995	1	15.7	10.8	4.6	984	984	984	983	986	986	14 1	. 93	6.4	
1	44			24.6	12.6	19.4	996	997	14.3	9.4	3,0	988	988	988	988	989	988	! '	. 94	6.7	
	44a	Ţ		23.2	11.2	17.9			12.8	8.0	1.7	988						Medium	. 92	6.7	
	45	7	i I	27.2	15.0	21.7	997	997	17.0	7.1	5.6	987	986	986	985	988	986		1, 82	6,6	6,6
	46	62.2		26.8	14.9	21.6	997	997	16.6	7,0	5, 5	986	986	986	984	986	986		1.85	6.6	6, 6
	47	62.4	1	26.8	14.8	21.6	997	997	16.5	6, 3	5, 2	984	984	979	977	978	977	['	1.96	6.4	5.9
	48	62.4	7	26.5	14.4	21.1	1001	1000	16.8	5.9	5.4	988	988	983	972	972	972	Low	2.02	6.7	5, 7
	49	62.6	10.7	26.1	14. 2	20.9	1001	1001	16.8	5.9	5. 7	989	989		972	972	971	11 1	2.07	6.8	5.6
	50	62.5	10.6	25.0	13.0	19.9	1003	1001	17.0	5.9	5, 7	989	1	1 1	972	971	971	!	2, 14		5,6
	51	62.1	10.5	26,5	14.5	21.3	1003	1003	16.8	6.1	5, 6	989	1)	٧.	973	971	971) Y	2, 05	1	5.6
	52	- 1		26.9	14.8	21.6	1001	1001	17. 1	7.2	5, 9	990	† [98 9	988	990	989	Medium	1.86	₹	6.8
	53			26.8	14.8	21.6	1003	1003	17. 2	9.1	6.0	991	991	991	991	994	993	High	1.54	6.9	7.0
ĺĺ	54			24.1	12, 3	18.9	1001	1000	14.5	9.7	3.6	991	990	990	989	994	993	None	. 93	6.8	
	55	62.4		31.4	19.4	26.1	1000	999	21.8	17.0	10,9	989	989	989	989	989	989	None	. 91	6.8	
8	56	47.0	6.0	24.8	17.8	21, 7	1006	1005	19.4	16.5	12,7	994	994	994	994	994	994	None	0.96	7.1	
٦	57	46.6	5.9	19: 2	12.5	16.2	1006	1005	13.9	11.1	7.7	994	994	994	994	994	994	1	. 94	7. 1	
	58	46,6	5.9	16.0	9.2	13.0	1004	1003	.8	8.0	4.3	992	991	991	990	991	990	} }	.96	6.9	
1	59	47.0	6.0	14.8	8. 1	11.9	1005	1005	9,6	6.8	3.2	992	991	991	991	994	992	!	.94	6.9	
		47.0	0.0	13.6	6.8	10.5	1001	1001	8.3	5.5	2, 1	989	989	989	989	989	989	♦	.93	6.8	
	60			12.3		9.3	1001	1001	7.0	4.1	.6	990	990	990	989	991	990	None/High	.93	0.0	
	61	46.9			5, 5			1000	l		.6	989	989	989	988	989	989	High	.96		
1	62		1	12.2	5,4	9.2	1001	1000	7.0 6.6	4.1 3.7	(989	989	989	989	989	989	Low	.98	∤	
	63	- [, T	11.9	5.0	9.0					2			973	961	959		10%	l	6.3	1
ļ	64	-	5.9	17.0	10.3	14.0		1000	11.7	5.0	5.3	984	983	973 974	962		958		2, 23		4.9
	65	Ţ	5.9	16.6	9.9	13.7	1000	1001	11.7	5. 2	5.4	984	984			960	959		2,33	6.4	5.0
	66	7	5. 9	17.7	10.8	14.7	1003	1003	11.9	5. 2	5.4	984	985	976	963	962	961	\ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \ \	2.25	6.4	5.0
	67	47.3	6. 1	19, 1	12, 2	16.0	1001	1000	12.0	6, 2	5.3	986	986	979	974	976	976	Medium	1.86	6.5	5, 9
	68	47.3	6, 1	18.8	11.9	15.8	1000	1000	11.9	8.8	5.0	989	989	988	988	989	989	None	. 96	6.8	
9	69	62. 1	10, 3	29.5	17, 5	24.3	946	944	18. 5	13.8	7.7	934	934	935	934	936	935	None	0.90	3.9	
	69a	62, 1	10.3	22,0	10.0	16.9			11, 1	6, 1	6	944						High	.97	4.3	
	69b	62.1	10.3	21.4	9.6	16.4			10.6	5.9	6	949						Low	.95	4.4	
	70	56.1	8.5	22,0	12.1	17.7	967	966	12.9	5. 1	3.9	956	955	955	954	956	955	Low	1.80	4.8	4.8
						_						4000	40.55	10:5	10==	4000	1000	-	0.00		
10	71	61.7	10.4	32.3	20.3	27.1	1018	1018	21.5	16.7	10.5	1009	1008	1010	1007	1010	1009	Low	0.92	8.2	
İ	71a	61.7	10.4	23.9	12.0	18.8			13. 2	8.4	1.9	1005						High	. 96	7.9	
	71b	61.7	10.4	22.1	10.2	17.0			11.4	6.6	0	1006						Medium	.96	8.0	-
i I	72	50.1	6.9	22.7	14.8	19.3	1039	1038	15.6	7.2	8.2	1019	1019	1008	991	991	990	Low	2.44	9.2	6.8

 $^{^{2}}$ For quality values and remarks see table II(a). b Shown only for flashed runs.

TABLE III. - DETAILED DATA FOR VENTURI WITH ARTIFICIAL THROAT CAVITY (SERIES II)

(a) U.S. customary units

Set	Run		Dynamic		Contr	rol ventu	ıri					Tes	t venturi				Noise	Pressure-	Vapor	Vapor	Exit	Remarks
		rate, W,	head, q,		Pressure psia	₽,		rature,]	Pressur psia	e,		т	emperatui ^O F	re,		indica tion	drop ratio,	pressure at T _{in} ,	pressure at T _{out} ,	quality,	
'		lbm hr	psi	Inlet.		Outlet.	-		Inlet.	Outlet.	Throat.	Inlet.						P ₄ - P ₅	P _{vin} ,	P _{vout} ,	percent	
ļ		}		P ₁	Throat,	P ₃	Inlet, T _{C1}	Outlet, T _{C2}	P ₄	P ₅	P _t	T _{in}		nce from		Outlet, T _{out}		P ₁ - P ₃	psia	psia	}	
}			İ		 !							"	0.9 in., T ₂	1.3 in., T ₃	1.7 in., T ₄	out.				ļ	1	}
11	h	545	18.8	52.0	31, 3	43.3	1388	1382	42.0	32,9	20. 5	1372	1372	1371	1377	1375	None	1. 04	13, 0			All-liquid flow
1	j k	600 481	22.8 14.6	56.1 47.3	31, 2 31, 5	45. 8 40. 7	1380 1388	1374 1381	44.4 39.7	33, 2 32, 5	17.5 22.3	1368	1368 1371	1366	1370 1373	1369	}	1, 08 1, 10	12.8 13.0			calibration
	m	419	11.1	43.7	31.5	38.5	1368	1362	37. 8	32.3	24.8	1350	1350	1349	1352	1351	[]	1.10	11.6			
	n	360	8.2	40.5	31.5	36. 7	1364	1358	36, 1	32, 0	26.4	1346	1346	1344	1348	1347		1.07	11.3			
ì	р	297	5, 6	37.6	31.4	34.9	1383	1386	34.6	31.7	28.0	1360	1359	1358	1362	1361	1 1	1.06	12.8			1 1
1	q	240	3.6	35.3	31.3	33.5	1384	1378	33.3	31.5	29.2	1360	1358	1356	1359	1359		1.03	12.1			{
	Г	119	. 9	41.6	40. 5	41.1	1417	1414	41.0	40, 6	40.0	1388	1387	1384	1388	1386	<u> </u>	. 87	14. 2	⊥ <u></u> .		<u> </u>
12	73	486	14.7	54.5	38.4	48.0	1322	1316	38.8	31, 4	20, 4	1303	1303	1300	1306	1306	None	1, 14	8.9			Liquid
1	74	489	14.9	51.4	35.0	44, 6	1327	1322	35. 3	27.9	17.6	1309	1309	1305	1310	1309	} }	1.08	9.2			
	75	487	14.8	45.1	28.7	38.1	1327 1325	1322 1320	28.9 25.5	21.5	11.6 8.1	1309	1309	1304 1302	1310 1309	1309	1 1	1.05 1.07	9.2			
Ì	76	484 486	14.7 14.7	41.7	25, 5 23, 7	34.8 33.1	1325	1315	23.8	18.2 16.4	6.4	1302	1302	1299	1303	1303	None/High	1.06	9.1 8.8			Incipient cavitation
}	78	487	14.8	38.6	22. 1	31,6	1322	1318	22.1	14.6	4.4	1305	1305	1302	1308	1307	High	1.07	9.0			Cavitated
	79	487	14.8	37.0	20, 5	30, 0	1323	1318	20.4	13.0	3.0	1306	1306	1302	1308	1307	High	1.05	9.0			Cavitated
1	80	487	14.8	34.7	18.1	27.7	1323	1317	18.1	10.6	. 5	1307	1306	1302	1309	1308	Medium	1.06	9. 1			Incipient flashing
1	81	483	14.6	45, 1	29. 1	38.5	1340	1335	29.7	10, 7	12.7	1320	1319	1315	1319	1317	Low	2, 89	9.8	9.6		Flashed
	82	484		43.5 42.2	27. 1 25. 9	36.6 35.2	1335	1330	29.1	8.8	11.7	1310 1308	1299	1290 1280	1295	1293		2.92 2.99	9. 2 9. 1	8.3	0.37	
	83 84	484 484	}	41.5	25. 1	34.7	1331	1325	29.0	7.9	11.6	1303	1288	1275	1279	1278	1 1	3. 09	8.9	7.6	. 54]]
}	85	489	14.9	41.8	25.3	34, 9	1331	1325	29.3	8.3	11.8	1305	1290	1281	1288	1288	1 1	3.04	9.0	8.1	. 36	}
ĺ	86	486	14.8	43.0	26.6	36.0	1328	1325	29.0	10, 0	11.6	1310	1308	1302	1310	1309	†	2.74	9.2	9.2		1 1
	87	483	14.6	42,8	26, 3	35.7	1322	1318	28.9	11.1	11,4	1308	1305	1301	1309	1307	Medium	2. 54	9.1	9.1] ♥
	88	486	14.7	37, 2	20,7	30, 3	1301	1295	21.2	13.7	3.3	1289	1287	1281	1289	1288	High	1.09	8.1			Cavitated
	89	489	14.9	38, 5 40, 5	22.0 23.9	31.6	1308	1303	22.6 24.4	15. 1 16. 9	4. 7 6. 7	1290 1290	1290 1290	1289 1289	1290 1291	1289	High High	1,08	8, 2 8, 2			Cavitated Cavitated
	90	488 488	14,8 14,8	40.4	23.8	33.4	1310	1306	24. 4	16.9	6, 5	1291	1290	1289	1292	1290	None	1.08	8.2			Liquid
}	92	486	14.7	42.3	25. 7	35, 3	1305	1302	26, 3	18.8	8.5	1289	1289	1285	1290	1288	None	1, 07	8, 1			Liquid
	93	486	14.7	39.8	23, 2	32.9	1315	1310	23.8	16, 3	5, 7	1299	1299	1294	1300	1299	None	1,09	8.7			Liquid
1	94	486	14.7	37.7	21.3	30.9	1317	1310	21.8	14.3	3, 8	1299	1299	1294	1300	1299	11	1, 10	8.7			1 1
1	95	483	14.6	36.5	20. 2	29, 6	1325	1320	20.7	13.2	3.1	1306	1306	1301	1309	1308	1 1	1.08	9,0			
1	96	483	14.6	35.4	19, 1	28.5	1327	1320	19.5	1	2, 1	1309	1309	1306	1310	1309	11	1,07	9.2			1 1
	97	489	14.9	35. 1	18, 4	28.0	1326	1320	18.8	11.3	1, 1	1309	1309	1304 1308	1310	1310	Vich	1.06				Toginiant envitation
1	98 98a	484 485	14.7 14.7	33.6 33.3	17.0 16.7	26.6 26.2	1328	1323	17.5 16.9	10.0	2 4	1310 1310	1310	1308	1311	1310	High Medium/Low	1.07				Incipient cavitation Incipient flashing
1	99	483	14.6	42.4	26, 2	35.7	1333	1328	29.4	9.0	12.1	1310	1301	1299	1301	1301	Low	3.06	\ \	8. 7	0, 20	Flashed
	100	484	14.7	43.2	26.8	36.3	1338	1333	29.9	10, 6	12, 4	1319	1318	1313	1318	1318	Medium	2.80	9.7	9,6		Flashed
	101	484	14.7	43.3	26.8	36.4	1340	1335	30, 1	12, 4	12, 4	1321	1320	1319	1321	1321	High	2.57	9.8	9,8		Flashed
1	102	484	14.7	35.8	19.2	28.8	1335	1330	22.4	14.7	4.1	1319	1316	1311	1319	1318	High	1,10	9.7			Cavitated
1	103	483	14.6	37.1	20, 7	30, 3	1328	1322	23.8	16.2	5.6	1310		1305	1312	1311	None	1.11	9.2			Liquid
1	104	483	14.6	40.2	23.6	33.1	1323	1318	26.8	19.2	9.0	1305	1305	1302	1307	1307	None	1.07	9.0			Liquid

13	105	490	15.0	40.5	23.7	33.5	1325	1320	27. 0	19.3	8.4	1308	1308	1305	1310	1309	None	1.11	9. 1			Liquid)
	105a	490	15.0	31.3	14.6	24, 3			17.5	10.0	5	1310					High	1.07	9.2			Incloient equitation
	105b	490	15.0	29.7	13.0	22, 9	}		16. 2	8.7	-2.2	1311					High Low	1, 10	9.2			Incinient flaching
1	106	368	8.5	31.1	21.4	26.9	1385	1380	23. 2	8.9	12,6	1345	1319	1302	1300	1299	Low	3, 45	11.2	8,6	1.00	Flashed ramp
- 1	107	483	14.6	39.9	23. 5	33, 1	1324	1320	26.8	19, 2	8.8	1308	1306	1304	1308	1307	None	1.10	9.1		1.00	Liquid
 -	-	 		+	 -	+	+	+	+	-	 	+	 		_	+			<u> </u>			Diquid 5
14	108	361	8.1	44.3	35. 1	40.3	1290	1285	22.6	18.6	13.3	1268	1268	1267	1272	1270	None	1,02	7. 2			Liquid
	109	362	8.1	40.4	31.4	36.7	1290	1286	18.9		8.8	1271	1268	1266	1272	1269	None	1, 12	7.4			Liquid
- 1	109a	358	7.9	37. 3	28. 1	33.2			15.6	11.6	6.8	1270					None High	.97	7.4			Incipient cavitation
ì	110	358	7.9	36.9	28.1	33.1	1290	1286	15.5	11.6	6.4	1270	1268	1266	1272	1269	High	1.03	7.3			Cavitated
1	111	355	7.8	34.8	26.2	31.1	1288	1284	13.6	9.6	4.4	1268	1265	1263	1267	1265	1 1	1.07	7, 2			1 1
ļ	112	360	8.0	32.9	24. 1	29.1	1277	1273	12. 1	8.0	2.7	1258	1256	1253	1258	1256		1.06	6.8			
İ	113	355	7.8	31.1	22. 5	27.3	1275	1270	10.6	6.7	1.6	1254	1253	1250	1255	1254	. ↓	1,06	6.7			1 1
1	114	355	7.8	30.2	21.6	26, 5	1272	1268	9.7	5.7	. 4	1252	1250	1248	1252	1251	Medium	1.08	6,6			
1	115	358	7.9	29.6	20.9	25.8	1270	1265	8.9	4.9	2	1250	1248	1246	1250	1250	Low	1.04	6, 5			1 }
	116	353	7.7	28.9	20.4	25, 2	1270	1265	8.7	4.8	3	1248	1248	1245	1250	1248	1 1	1.06	6, 4			
1	117	363	8, 1	20.9	11.8	16.9	1265	1261	8.9	4.8	6	1248	1245	1243	1247	1245	11	1.04	6.4			} }
	118		1	26.8	18.1	23.1	1261	1255	8.7	4.6	9	1240	1238	1236	1240	1238		1, 10	6, 2			
l	118a	!	1	28.9	20, 0	25.1	1		10.0	6.0	. 5	1240						1, 05	(Incipient flashing
1	119			28.9	20, 1	25, 1	1261	1257	16.3	6.0	6.9	1240	1229	1225	1228	1226	1 1	2.75		5, 6	0.30	Flashed
1	120	1	+	31.2	22.5	27.6	1261	1258	16.4	7.8	7. 1	1241	1238	1237	1241	1240	} ↓	2.37		6.1		Flashed
1	121	360	8.0	33.2	24.4	29.4	1263	1260	13.6	9.7	4, 3	1242	1242	1238	1242	1240	High	1.06	\			Cavitated
1	122	360	8.0	35, 3	26. 5	31.5	1265	1262	15.8	11.8	6.6	1244	1245	1242	1247	1246	High	1.04	6.3			Cavitated
	123	361	8.1	37.0	28.0	33.1	1267	1263	17. 2	13. 1	7.6	1249	1246	1244	1248	1247	None	1.07	6, 4			Liquid
				-			-		├──							-						Biquid
15	124	361	8,2	36.9	28.0	33.2	1335	1330	17. 2	13. 1	7.6	1312	1311	1310	1313	1310	None	1.08	9.3			Liquid
15	125	360	8, 2	35.0	26.0	31.1	1335 1339	1330 1332	15.0	13.1	5.7	1315	1311	1310 1311	1313 1319	1310	None High	1.08	9.3 9.5			Liquid Incipient cavitation
15	125 125a			35. 0 33. 4	26.0 24.5	31.1 30.0	1339	1332	15. 0 13. 4	11.0 9.5	5. 7 3. 5	1315 1315	1315	1311	1319	1317	1 1			j	ļ	1 -
15	125 125a · 126			35. 0 33. 4 39. 7	26.0	31.1	1339 1340	1332 1335	15. 0 13. 4 20. 0	11.0	5.7	1315 1315 1315	1315	1311	1319 1301	1317 1300	High	1.04	9.5			Incipient cavitation
15	125 125a 126 127	360	8, 1	35. 0 33. 4 39. 7 40. 1	26.0 24.5 30.9 31.1	31. 1 30. 0 35. 9 36. 2	1339 1340 1345	1332 1335 1340	15. 0 13. 4 20. 0 20. 3	9.5 9.2 8.0	5. 7 3. 5 10. 8 11. 0	1315 1315 1315 1311	1315 1301 1290	1311 1299 1280	1319 1301 1281	1317 1300 1279	High High, Low	1.04 1.15	9.5 9.5			Incipient cavitation Incipient flashing
15	125 125a · 126			35. 0 33. 4 39. 7 40. 1 30. 4	26.0 24.5 30.9	31.1 30.0 35.9	1339 1340	1332 1335	15. 0 13. 4 20. 0	11.0 9.5 9.2	5. 7 3. 5 10. 8	1315 1315 1315	1315 1301	1311 1299	1319 1301	1317 1300	High High, Low	1.04 1.15 2.81	9.5 9.5 9.5	8.7	0, 33	Incipient cavitation Incipient flashing
15	125 125a · 126 127 128 129	360	8, 1	35. 0 33. 4 39. 7 40. 1	26.0 24.5 30.9 31.1	31. 1 30. 0 35. 9 36. 2	1339 1340 1345	1332 1335 1340	15. 0 13. 4 20. 0 20. 3	9.5 9.2 8.0	5. 7 3. 5 10. 8 11. 0	1315 1315 1315 1311	1315 1301 1290	1311 1299 1280	1319 1301 1281	1317 1300 1279	High High, Low	1. 04 1. 15 2. 81 3. 17	9.5 9.5 9.5 9.3	8.7 7.7	0. 33 . 70	Incipient cavitation Incipient flashing
15	125 125a 126 127 128	360 4 361	8, 1	35. 0 33. 4 39. 7 40. 1 30. 4	26.0 24.5 30.9 31.1 21.6	31. 1 30. 0 35. 9 36. 2 26. 6	1339 1340 1345 1340	1332 1335 1340 1335	15. 0 13. 4 20. 0 20. 3 20. 2	9.5 9.2 8.0 7.4	5. 7 3. 5 10. 8 11. 0 11. 1	1315 1315 1315 1311 1309	1315 1301 1290 1281	1311 1299 1280 1270	1319 1301 1281 1270	1317 1300 1279 1269	High High, Low	1. 04 1. 15 2. 81 3. 17 3. 38	9.5 9.5 9.5 9.3 9.2	8.7 7.7 7.2	0. 33 . 70 . 87	Incipient cavitation Incipient flashing
15	125 125a 126 127 128 129 130	360 361 360	8, 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5	26.0 24.5 30.9 31.1 21.6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6	1339 1340 1345 1340 1335 1335	1332 1335 1340 1335 1330 1330	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0	11.0 9.5 9.2 8.0 7.4 7.0	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3	1315 1315 1315 1311 1309 1301	1315 1301 1290 1281 1278	1311 1299 1280 1270 1261	1319 1301 1281 1270 1261	1317 1300 1279 1269 1260	High High, Low	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32	9.5 9.5 9.3 9.2 8.8	8.7 7.7 7.2 6.9	0. 33 . 70 . 87	Incipient cavitation Incipient flashing
15	125 125a 126 127 128 129 130	360 361 360 360	8, 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5	26.0 24.5 30.9 31.1 21.6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5	1339 1340 1345 1340 1335	1332 1335 1340 1335 1330 1330	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0	11.0 9.5 9.2 8.0 7.4 7.0 8.0	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8	1315 1315 1315 1311 1309 1301 1304	1315 1301 1290 1281 1278 1285	1311 1299 1280 1270 1261 1276	1319 1301 1281 1270 1261 1280	1317 1300 1279 1269 1260 1278	High High, Low	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08	9.5 9.5 9.5 9.3 9.2 8.8 8.9	8.7 7.7 7.2 6.9 7.6	0. 33 . 70 . 87 . 89	Incipient cavitation Incipient flashing
15	125 125a 126 127 128 129 130	360 361 360 360 360	8, 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5	26.0 24.5 30.9 31.1 21.6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6	1339 1340 1345 1340 1335 1335	1332 1335 1340 1335 1330 1330	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0 20. 1	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8	1315 1315 1315 1311 1309 1301 1304 1310	1315 1301 1290 1281 1278 1285 1305	1311 1299 1280 1270 1261 1276 1301	1319 1301 1281 1270 1261 1280 1309	1317 1300 1279 1269 1260 1278 1302	High High, Low	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05	9.5 9.5 9.5 9.3 9.2 8.8 8.9	8.7 7.7 7.2 6.9 7.6 8.8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing
15	125 125a 126 127 128 129 130 131 132 133	361 360 360 360 363 363	8.1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 5 29. 6 27. 6	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6 25. 7 23. 7	1339 1340 1345 1340 1335 1335 1332 1329	1332 1335 1340 1335 1330 1330 1328 1322 1321	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0 20. 1 20. 0 16, 9	11. 0 9. 5 9. 2 8. 0 7. 4 7. 0 8. 0 9. 7 10. 6 12. 8	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 8 10. 5 7. 6	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305	1315 1301 1290 1281 1278 1285 1305 1305	1311 1299 1280 1270 1261 1276 1301 1301	1319 1301 1281 1270 1261 1280 1309 1309 1308	1317 1300 1279 1269 1260 1278 1302 1302	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05	9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2	8.7 7.7 7.2 6.9 7.6 8.8 8.8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid
15	125 125a 126 127 128 129 130 131 132 133	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 5 29. 6 27. 6	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6 25. 7 23. 7	1339 1340 1345 1340 1335 1335 1332 1329 1328	1332 1335 1340 1335 1330 1330 1328 1322 1321	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0 20. 1 20. 0 16. 9	11. 0 9. 5 9. 2 8. 0 7. 4 7. 0 8. 0 9. 7 10. 6 12. 8	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 8 10. 5 7. 6	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305	1315 1301 1290 1281 1278 1285 1305 1305 1304	1311 1299 1280 1270 1261 1276 1301 1301 1301	1319 1301 1281 1270 1261 1280 1309 1309 1308	1317 	High High, Low Low	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05	9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2	8.7 7.7 7.2 6.9 7.6 8.8 8.8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid
15	125 125a 126 127 128 129 130 131 132 133 134	361 360 360 360 363 363	8.1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 5 29. 6 27. 6	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6 25. 7 23. 7 25. 0 23. 5	1339 1340 1345 1340 1335 1332 1329 1328 1330 1331	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1325	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6	11. 0 9. 5 9. 2 8. 0 7. 4 7. 0 8. 0 9. 7 10. 6 12. 8 14. 3 12. 5	5.7 3.5 10.8 11.0 11.1 10.3 10.8 10.8 10.5 7.6 9.0 7.3	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1309	1311 1299 1280 1270 1261 1276 1301 1301 1305 1305	1319 1301 1281 1270 1261 1280 1309 1309 1308 1310	1317 	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03	9.5 9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2 9.2	8.7 7.7 7.2 6.9 7.6 8.8 8.8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid
15	125 125a · 126 127 128 129 130 131 132 133 134 135	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6 25. 7 23. 7 25. 0 23. 5 21. 8	1339 1340 1345 1340 1335 1335 1332 1329 1328 1330 1331 1335	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1325	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0	11. 0 9. 5 9. 2 8. 0 7. 4 7. 0 8. 0 9. 7 10. 6 12. 8 14. 3 12. 5 10. 9	5.7 3.5 10.8 11.0 11.1 10.3 10.8 10.5 7.6 9.0 7.3 5.5	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1310 1318	1315 1301 1290 1281 1278 1285 1305 1304 1309 1309 1318	1311 1299 1280 1270 1261 1276 1301 1301 1305 1305 1314	1319 1301 1281 1270 1261 1280 1309 1308 1310 1310	1317 1300 1279 1269 1260 1278 1302 1302 1306 1308 1308 1316	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05	9.5 9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2 9.2 9.0	8.7 7.7 7.2 6.9 7.6 8.8 8.8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid
15	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 6 25. 7 23. 7 25. 0 23. 5 21. 8 20. 7	1339 1340 1345 1340 1335 1335 1332 1329 1328 1330 1331 1335 	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1325	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0 13. 5	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5	5.7 3.5 10.8 11.0 11.1 10.3 10.8 10.5 7.6 9.0 7.3 5.5 3.9	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1310 1318 1318	1315 1301 1290 1281 1278 1285 1305 1304 1309 1309 1318	1311 	1319 1301 1281 1270 1261 1280 1309 1308 1310 1310 1318	1317 1300 1279 1269 1260 1278 1302 1306 1308 1308 1316	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05 1. 05	9.5 9.5 9.5 9.3 9.2 8.8 9.2 9.2 9.0 9.2 9.7	8. 7 7. 7 7. 2 6. 9 7. 6 8. 8 8. 8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
15	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 3	31.1 30.0 35.9 36.2 26.6 25.6 25.5 25.6 25.7 23.7 23.7 25.0 23.5 21.8 20.7 27.5	1339 1340 1345 1335 1335 1329 1328 1330 1331 1335 	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1330 1335	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0 13. 5 20. 6	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1	1315 1315 1315 1311 1309 1301 1304 1309 1305 1310 1310 1318 1318	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1318 1306	1311 	1319 1301 1281 1270 1261 1280 1309 1309 1308 1310 1310 1318 1303	1317 1300 1279 1269 1260 1278 1302 1306 1308 1308 1316 1300	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05 2. 88	9.5 9.5 9.5 9.3 9.2 8.8 9.2 9.2 9.0 9.2 9.7 9.7	8. 7 7. 7 7. 2 6. 9 7. 6 8. 8 8. 8	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid
15	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 3 22. 2	31.1 30.0 35.9 36.2 26.6 25.6 25.5 25.6 25.7 23.7 25.0 23.5 21.8 20.7 27.5	1339 1340 1345 1335 1335 1332 1328 1330 1331 1335 1340 1341	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1330 1335 1335	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0 13. 5 20. 6 20. 5	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0	1315 1315 1315 1311 1309 1301 1304 1310 1305 1310 1310 1318 1318 1318	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1309 1318 1306 1290	1311 1299 1280 1270 1261 1301 1301 1301 1305 1305 1314 1300 1279	1319 1301 1281 1270 1261 1280 1309 1309 1310 1310 1318 1303 1281	1317 1300 1279 1269 1260 1278 1302 1306 1308 1308 1316 1300 1280	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05 2. 88 3. 24	9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2 9.0 9.2 9.7 9.7 9.7	8.7 7.7 7.2 6.9 7.6 8.8 8.8 	0. 33 . 70 . 87 . 89 . 57	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
15	125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138 139	360 361 360 360 360 363 360 355	8. 1 8. 2 8. 1 7. 9	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2 32. 0	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 3 22. 2 23. 0	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 7 23. 7 25. 0 23. 5 21. 8 20. 7 27. 5 27. 4 28. 2	1339 1340 1345 1340 1335 1332 1329 1328 1330 1331 1335 1340 1341 1341	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1325 1330 1335 1335	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0 13. 5 20. 6 20. 5	11.0 9.5 9.2 8.0 7.4 7.0 8.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0 7.5	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0 11. 1	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1318 1318 1318 1318 1310 1310	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1318 1306 1290 1281	1311 1299 1280 1270 1261 1301 1301 1305 1305 1314 1300 1279 1270	1319 1301 1281 1270 1261 1280 1309 1308 1310 1318 1303 1281 1270	1317 1300 1279 1269 1260 1278 1302 1306 1308 1308 1316 1300 1280 1269	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05 2. 88 3. 24 3. 44	9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2 9.0 9.2 9.7 9.7 9.7 9.2	8.7 7.7 7.2 6.9 7.6 8.8 8.8 8.7 7.7	0. 33 . 70 . 87 . 89 . 57 	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138 139 140	361 360 360 360 363 360 355 360	8.1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2 32. 0	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 3 22. 2 23. 0 22. 9	31. 1 30. 0 35. 9 36. 2 26. 6 25. 6 25. 5 25. 7 23. 7 25. 0 23. 5 21. 8 20. 7 27. 5 27. 4 28. 2 28. 3	1339 1340 1345 1340 1335 1332 1329 1328 1330 1331 1335 1340 1341 1341	1332 1335 1340 1335 1330 1328 1322 1321 1325 1325 1335 1335 1336 1335	15. 0 13. 4 20. 0 20. 3 20. 2 20. 0 20. 1 20. 0 16. 9 18. 3 16. 6 15. 0 13. 5 20. 6 20. 5 20. 4	11.0 9.5 9.2 8.0 7.4 7.0 8.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0 7.5 7.3	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0 11. 1	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1318 1318 1318 1318 1310 1310 1310	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1318 1306 1290 1281 1281	1311 	1319 1301 1281 1270 1261 1280 1309 1309 1308 1310 1318 1303 1281 1270 1268	1317 1300 1279 1269 1260 1278 1302 1306 1308 1316 1300 1280 1269 1265	High Low Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 06 1. 03 1. 05 1. 05 2. 88 3. 24 3. 44 3. 49	9.5 9.5 9.5 9.2 8.8 8.9 9.2 9.2 9.7 9.7 9.7 9.7 9.7	8.7 7.7 7.2 6.9 7.6 8.8 8.8 8.7 7.7 7.2	0. 33 . 70 . 87 . 89 . 57 	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138 139 140 141	360 361 360 360 363 360 353 360	8. 1 8. 2 8. 1 7. 9 8. 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2 32. 0 31. 8	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 2 22. 2 23. 0 22. 9 22. 9	31.1 30.0 35.9 36.2 26.6 25.5 25.6 25.7 23.7 25.0 23.5 21.8 20.7 27.5 27.4 28.2 28.3	1339 1340 1345 1340 1335 1335 1332 1328 1330 1331 1335 1340 1341 1341 1340 1343	1332 1335 1340 1335 1330 1328 1322 1321 1325 1325 1330 1335 1336 1335 1340	15.0 0 13.4 20.0 20.3 20.2 20.0 20.1 20.0 16.9 18.3 16.6 6 15.0 13.5 20.6 20.5 20.4 20.4	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0 7.7 8.0 9.7	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0 11. 1	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1318 1318 1318 1318 1310 1310	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1318 1306 1290 1281 1281 1309	1311 	1319 1301 1281 1270 1261 1280 1309 1309 1310 1310 1318 1303 1281 1270 1268 1305	1317 1300 1279 1269 1260 1278 1302 1306 1308 1316 1300 1280 1269 1265 1302	High Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 05 1. 05 1. 05 2. 88 3. 24 3. 44 3. 49 2. 89	9.5 9.5 9.3 9.2 8.8 8.9 9.2 9.2 9.0 9.2 9.7 9.7 9.7 9.2	8.7 7.7 7.2 6.9 7.6 8.8 8.8 8.7 7.7 7.2 7.1	0. 33 . 70 . 87 . 89 . 57 0. 40 . 65 . 89 . 83 . 35	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138 139 140 141 142	360 361 360 360 363 363 360 355 360	8. 2 8. 1 7. 9 8. 1 8. 0 8. 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2 32. 0 31. 8 32. 0	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 3 22. 2 23. 0 22. 9 22. 9	31.1 30.0 35.9 36.2 26.6 25.5 25.6 25.7 23.7 25.0 23.5 21.8 20.7 27.5 27.4 28.2 28.3 28.0 28.2	1339 1340 1345 1340 1335 1332 1329 1328 1330 1331 1335 1340 1341 1341 1343 1343	1332 1335 1340 1335 1330 1330 1328 1322 1321 1325 1335 1335 1335 1335 1335 1335	15.0 13.4 20.0 20.3 20.2 20.0 20.1 20.0 16.9 18.3 16.6 15.0 20.5 20.5 20.5 20.4 20.4 20.6	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0 9.7 10.6 12.8	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0 11. 1 10. 9 11. 1	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1318 1318 1318 1318 1310 1310 1310	1315 	1311 	1319 1301 1281 1270 1261 1280 1309 1308 1310 1311 1318 1303 1281 1270 1268 1305 1312	1317 1300 1279 1269 1260 1278 1302 1306 1308 1316 1300 1280 1269 1265 1302 1310	High Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 05 1. 05 1. 05 2. 88 3. 24 3. 44 3. 49 2. 89 2. 71	9.5 9.5 9.5 9.2 8.8 8.9 9.2 9.2 9.7 9.7 9.7 9.7 9.7	8.7 7.7 7.2 6.9 7.6 8.8 8.8 8.7 7.7 7.2 7.1 8.8 9.2	0. 33 . 70 . 87 . 89 . 57 	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid
	125 125a 126 127 128 129 130 131 132 133 134 135 136 136a 137 138 139 140 141	360 361 360 360 363 360 353 360	8. 1 8. 2 8. 1 7. 9 8. 1 8. 0 8. 1 8. 1	35. 0 33. 4 39. 7 40. 1 30. 4 29. 5 29. 5 29. 6 27. 6 28. 8 27. 4 25. 8 24. 5 31. 3 31. 2 32. 0 31. 8	26. 0 24. 5 30. 9 31. 1 21. 6 20. 6 18. 7 20. 0 18. 4 16. 7 15. 4 22. 2 22. 2 23. 0 22. 9 22. 9	31.1 30.0 35.9 36.2 26.6 25.5 25.6 25.7 23.7 25.0 23.5 21.8 20.7 27.5 27.4 28.2 28.3	1339 1340 1345 1340 1335 1335 1332 1328 1330 1331 1335 1340 1341 1341 1340 1343	1332 1335 1340 1335 1330 1328 1322 1321 1325 1325 1330 1335 1336 1335 1340	15.0 0 13.4 20.0 20.3 20.2 20.0 20.1 20.0 16.9 18.3 16.6 6 15.0 13.5 20.6 20.5 20.4 20.4	11.0 9.5 9.2 8.0 7.4 7.0 8.0 9.7 10.6 12.8 14.3 12.5 10.9 9.5 9.7 8.0 7.7 8.0 9.7	5. 7 3. 5 10. 8 11. 0 11. 1 10. 3 10. 8 10. 5 7. 6 9. 0 7. 3 5. 5 3. 9 11. 1 11. 0 11. 1	1315 1315 1315 1311 1309 1301 1304 1310 1309 1305 1310 1318 1318 1318 1318 1310 1310 1310	1315 1301 1290 1281 1278 1285 1305 1305 1304 1309 1318 1306 1290 1281 1281 1309	1311 	1319 1301 1281 1270 1261 1280 1309 1309 1310 1310 1318 1303 1281 1270 1268 1305	1317 1300 1279 1269 1260 1278 1302 1306 1308 1316 1300 1280 1269 1265 1302	High Low Low None	1. 04 1. 15 2. 81 3. 17 3. 38 3. 32 3. 08 2. 05 2. 39 1. 05 1. 05 1. 05 1. 05 2. 88 3. 24 3. 44 3. 49 2. 89	9.5 9.5 9.5 9.2 8.8 8.9 9.2 9.2 9.7 9.7 9.7 9.7 9.7	8.7 7.7 7.2 6.9 7.6 8.8 8.8 8.7 7.7 7.2 7.1	0. 33 . 70 . 87 . 89 . 57 	Incipient cavitation Incipient flashing Flashed Liquid Liquid Liquid Liquid Liquid Liquid Liquid Liquid

aShown only for flashed runs.

TABLE III. - Continued. DETAILED DATA FOR VENTURI WITH ARTIFICIAL THROAT CAVITY (SERIES II)

(a) Concluded. U.S. customary units

																<u> </u>		I	T			
Set	- 1	- 1	Dynamic		Con	trol ven	turi					Tes	t venturi				Noise indica-	Pressure-	Vapor	Vapor	Exit	Remarks
1)	rate, W,	head,		Pressur	e,		rature,] 1	Pressur	e,		T	emperatu	re,		tion	drop ratio,	pressure at T _{in} ,	pressure at T _{out} ,	quality,	
		lbm	q, psi		psia			F		psia				^o F			1	P ₄ - P ₅	1 _	1	percent	
	Ì	hr		Inlet,	Throat,	Outlet,	Inlet,	Outlet,	Inlet.	Outlet,	Throat,	Inlet,	Dista	nce from	inlet	Outlet.	Í		P _{vin} ,	P _{vout} ,		
1	l			P ₁	P ₂	P ₃	T _{C1}	T _{C2}	P ₄	P ₅		T _{in}				Tout		P ₁ - P ₃	psia	psia		
	j			- 1	- 2	3	CI	-02	4	5		ın	0.9 in.,	, ,	I.7 in.,	out						
	- {								į		ĺ		T ₂	т ₃	T ₄				{	ļ		
1.0		050		00.5	05.5	20.0	1445	1440	25.4	21.3	15. 7	1419	1419	1416	1420	1419	None	1, 10	16.7			Liquid
1 1	145 146	352 352	7.9 7.9	36.5 34.7	27.7 25.9	32.8	1445	1440 1440	25. 4 23. 5	19.4	13.8	1421	1420	1419	1421	1420	None	1, 11	16.8			Liquid
	147	354	8.0	29.0	20.2	25. 2	1447	1440	17, 7	13, 6	8.2	1422	1421	1419	1421	1420	None	1.06	16.9			Liquid
	147a	357	8,1	27.5	18.7	23.9			16.0	12.0	6.2	1422					Medium	1,11	16.9			Incipient cavitation
1 1	147b	t	I	27. 2	18.4	23.6			15.7	11.9	6.4	1422					Low	1.06	16.9			Incipient flashing
	148			37.6	28.7	33.8	1455	1446	26.3	12.3	16.8	1408	1372	1353	1352	1352	1	3.65	15.7	11.7	1.23	Flashed
1 1	149		∳	37.5	28,6	33, 7	1455	1450	26.2	11.9	16.8	1409	1372	1351	1349	1348		3.81	15.8	11.4	1.33	1
	150	354	8.0	37, 3	28.5	33.6	1455	1448	26.1	12.4	16.8	1409	1376	1358	1355	1353		3,71	15.8	11.7	1.23	[
1 1	151	352	7.9	37.7	28.9	34.1	1459	1452	26.4	13. 1	17.1	1411	1381	1367	1365	1365]]	3.67	16.0	12, 5	1.01	
1	152	354	8.0	37.7	28.8	34.0	1455	1445	26.4	13,9	17.0	1411	1384	1376	1379	1378		3, 35	16.0	13.5	. 72	Í
1 1	153	354	8.0	37.7	28.8	34.0	1450	1445	26, 5	14.9	17.1	1415	1391 1401	1389 1399	1389 1400	1389 1399]]	3.14 2.98	16.3 16.7	14.3	. 58]
	154	352	7.9	37.8	29.1	34.2	1449	1440	26.8	16.0 17.4	17.5	1419	1415	1412	1415	1413	1 1	2.77	16.7	15. 1 10. 1	. 44	
1 1	155	354 352	8.0	39. 0 38. 8	30, 2 30, 1	35, 3 35, 1	1445	1440 1447	27.8	18.3	19. 2	1429	1421	1420	1422	1420	1 🛊	2, 76	17.5	16.7	. 20]]
1	156 157	352	7.9 8.1	39.0	30, 1	35.3	1452	1447	28.5	19.3	19.1	1430	1426	1422	1430	1428	Medium	2, 45	17.5	17.3		! *
1 1	158	355	8.1	45. 2	36.3	41.5	1450	1445	25, 1	21.0	15.2	1426	1422	1421	1426	1423	None	1, 11	17. 2			Liquid
	150	330	0.1	30.2	30.0	11.0	1100	1110		1					Į							1
-	159	360	8.3	36, 1	26.8	32.5	1448	1442	24.7	20.7	14.6	1424	1422	1420	1424	1422	None	1.08	12.0			Liquid
	160	358	8.2	32.9	24.0	29.0		1442	22.0	17.9	12.6	1422		1418	1423	1420	None	1.06	16.9			Liquid
1 1	161		[30.0	21.2	26. 1	1450	1445	19.1	15.0	9.9	1425	1	1423	1424	1425	1	1.04	17.1			Liquid Incipient cavitation
11	161a	1 1	1 1	28.1	19.3	24.3			17, 1 16, 6	13.2	8.1	1425	1				None/Medium Medium/Low	1, 03 1, 03	17.1			Incipient flashing
	161b	257	8.1	27. 6 37. 5	18.9	23.9	1 .		26.6	12.8	17.1	1414		1365	1364	1364		3, 54	16.2	12.5	1. 01	Flashed
1	163	357 360	8.3	38, 5	29.6	34.8	1	1	27.7	14.6	18. 2	1428	1	1386	1385	1386	1	3, 50	17.3	14.0	. 92	Flashed
	100	ļ	}		1	1		ļ	1	ļ	1	1	1	ļ		Į.	1					
	164	358	8.2	33.4	24.5	29.5		1451	22, 6	18. 5	13. 2	1432	i	1428	1432	1431	1	1,06	17.7			Liquid
	165			31.7	22.8	27.8		1461	20.7	16.6	11.3	1442	1	1438	1442	1440		1.06	18.5			Liquid
	166			29, 5	20.5	25, 6	1		18.5	14.4	9,0	1445		1440	1442	1441		1.06	18.8			Liquid Incipient flashing
	166a	1	! !	28.2	19.4	24.3		1462	17.1 27.0	13.2	8. 4 17. 8	1445		1369	1369	1369	. [1,00 3,81	18.8	13.5	1.06	Flashed
	167 168	354 357	8.0	44.6	35.8	40.8			29.3	19.1	20.0	144		1430	1433	1432	, ,	2, 69	18.5	17.7	.31	Flashed
	169	360	8.3	44.6	35.6	40.8	J	I .	29.0	1	19.5	1442	1	1440	1447	1442	1 1	1,06	18.6			Liquid
] ***]		ł	1								1								
	170	357	8.2	39.3	30.4	35.4		1	23.7		14.6	144	I .	1438	1441	1440	1	1.02	18.4			Liquid
	171	352	8.0	36.1	1	32.4		1	20, 6	1	11.4	143	Ī	1432	1435	1434	1 1	1.06	18.0			
	172	357	8.1	34.3	25. 5	30, 4	1	1	18.5	1	9.4	1420	1	1424	1427	1426	L	1.03	17.2			1 1
1	173	358	8.2	32, 6	1	28.7	1	i	16.7		7.5		1	1422	1426	1424	None/High/Lov	1,03 v 1,11	17.1			Incipient cavitation and flashing
i	173	a 357	8.1	30. 7	22.2	27.2	3		15. 1	11.2	5.4	142]				None/High/Lov	1,11	1 11.1			meipient cavitation and manning
1	174	355	8.1	35. 5	26.8	31.7	7 1446	1440	20.0	16.0	10.7	142	2 1420	1418	1420	1420	None	1.06	16.9		1	Liquid
	175	357	8.1	33.6	1	29.8		1438	17.8		8.4		1	1416	1418	1418	1	1.06	16.7			Liquid
1	175		8.1	31.8		28.1	1		15.9	,	6.9	[1				None/Low/Nor		16.7			Incipient cavitation and flashing
	176	297	5.6	32.7	26.4	30.	1 145	1442	21.	12.0	15.0	140	0 1363	1350	1350	1350	None	3,64	15.1	11.6	1.10	Flashed

_	,					,			-										,			
17	1	481	14.7	47. 2	31.0	40.5	1425	1420	31.5	24.2	14.0	1408	1405	1401	1409	1406	None	1. 08	15.7			Liquid
	178	479	14.7	44.8	28.5	38.0	1430	1425	29, 0	21.6	11.5	1411	1410	1409	1411	1410	1 (1.07	16.0			
1	179	482	14.8	42.9	26, 5	35.9	1430	1425	26. 9	19.4	9.4	1411	1410	1409	[411	1410	}	1.06	16,0			1 1
	180	481	14.7	40.9	24.4	33.8	1428	1420	24,8	17.3	7.4	1410	1409	1405	1410	1409		1.06	15.9			
- }	181	482	14.8	39.0	22, 5	31.9	1429	1423	22.8	15. 2	5, 3	1410	1409	1406) !		1 1		1 1		}	} ↓
	1	l I		I .		1 1			1					J	1411	1409	l'	1.06	15.9			
- 1	182	481	14.7	37, 1	20.6	30.1	1430	1425	21.0	13.5	3.1	1410	1410	1409	1411	1410	None High Low	1.09	15.9			Incipient cavitation and flashing
	183	482	14.8	45.6	29.0	38.5	1430	1425	35,8	13.3	17.8	1400	1379	1369	1370	1369	Low	3.15	15.1	12,5	0,68	Flashed
	184	479	14.6	45.9	29, 2	38.8	1435	1430	35.9	12.7	17.9	1400	1378	1360	1360	1360	}	3.31	15.1	12, 2	. 88	l 1
1	185	479	14,6	45.4	29.1	38.6	1 l	1431	35.8	14.2	18.2	1402	1385	1379	1380	1379	i	3,20	15.3	13, 5	. 62	
	186	481	14.8	48.2	31.9	41.4		1430	36.2	16.1	18.5	1412	1403	1400	1402	1401	} •	2,94	16, 1	15, 2	. 24	1 1
	187	481	1	50.6	34.2	43.7	- ↓	1429	36, 4	17.8	18.7	1412	1410	1409	1411	1410	Medium	2.73	16.1	15, 9		
- 1	188	481	- 1	51, 6	35, 1	44.6	1430	1425	36.2	19.3	18.4	1411	1410	1409	1411	1410	Medium	2,42	16.0	15, 9		l l
	1		1	52. 5	ŀ				36.0	20.8	1 '	i !							1 1			'
	189	482			36.1	45.5	1428	1422		l	18.2	1410	1409	1406	1410	1409	Medium	2, 07	15.9	15.8		1 .
	190	484	14.9	46.5	29,8	39,5	1431	1425	29.8	22.2	11.7	1411	1411	1410	1412	1411	None	1.08	16.0			Liquid
	191	481	14.7	48.8	32, 2	41.6	1430	1422	32.]	24.6	15.0	1410	1410	1408	1410	1409	None	1, 03	15.9			Liquid
						ا ا			ا ـ '	l												
	192	481	14.7	41.6	25.0	34.7	1425	1416	24.9	17,3	6.7	1405	1403	1402	1406	1404	None	1.09	15.5			Liquid
1	193	1 1	-	39.2	22.7	32.2	1425	1416	22.5	14.9	4.6	1408	1405	1402	1408	1406	None	1.08	15.7			Liquid
	193a	111	- }	38.1	21.3	31.1			21.3	13.9	3,4	1408					None High	1.06	15.7			Incipient cavitation and flashing
1	194		¥	47.3	30.9	40.7	1425	1420	35.3	13.3	17.5	1398	1378	1369	1370	1369	Low	3, 31	15.0	12,8	0, 33	Flashed
-	195		14.8	46,9	30.3	39.7	1435	1430	36.7	17.5	18.8	1418	1413	1411	1418	1416	Low	2.69	16.6	16.3		Flashed
	196		14.7	49.2	32,6	42.2	1430	1423	36, 2	20, 7	18.3	1410	1410	1405	1411	1410	Medium	2, 23		15.9		Flashed
-	196						- 1		29.2		1 1								15.9	- 1		
		1	14.7	45.0	28.5	38.1	1427	1422		21.6	11.2	1410	1409	1405	1410	1409	None	1,09	15, 9			Liquid
1	198	*	14.7	48.4	31,9	41.5	1425	1420	32.7	25. 1	14.5	1408	1405	1402	1408	1407	None	1. 10	15.7			Liquid
1	199	481	14.7	61.0	44.8	54.0	1427	1422	32.6	25, 1	15.2	1410	1409	1408	1411	1409	None	1 00	150			Llautd
l			14. /			1	- 1		, ,		1 1		1		- 1	- 1	None	1.08	15.9			Liquid
-	200	479		55.9	39.7	49.1	1427	1421	27.3	19.8	9.5	1409	1409	1403	1410	1408		1, 10	15.8			
	201	479	1	52.3	36.1	45.6	1427	1420	23, 6	16.1	5.6	1409	1408	1403	1410	1410		1, 11	15.8			
	202	478		50.5	34, 4	43.8	1422	1417	21.7	14.3	3.8	1404	1402	1400	1405	1404	₹	1.11	15.4			Ŧ
1	202a	478	† †	49.8	33.5	43.1			20.4	13.1	2.6	1404					None High, Low	1,09	15.4			Incipient cavitation and flashing
	203	485	14,5	49.0	32,6	42.1	1422	1416	35.3	12.7	17. 1	1391	1370	1360	1360	1360	Low	3,30	14,5	12, 2	0, 68	Flashed
1	204	481	15.0	47.9	31.5	41.0	1415	1410	28.5	21.0	10.7	1400	1399	1393	1400	1399	None	1,08	15.1			Liquid
<u> </u>	انتا																		10.1			214010
18	205	427	11.6	38.7	25.8	33.2	1425	1420	26.5	20.6	12.7	1401	1401	1399	1402	1402	None	1.07	15.2			Liquid
1	206	429	11.7	34.1	21.1	28.5	1425	1420	21.7	15, 8	8.0	1405	1405	1401	1409	1406	None	1,06	15. 5			Liquid
	207	424	11.5	31, 5	18,7	26.0	1429	1421	19,3	13,5	5.6	1409	1407	1402	1409	1407	None	1.07	15.8			Liquid
	208	429	11.7	30.3	17.1	24. 7	1424	1419	17.8	11.8	3.7	1403	1401	1400	1403	1402	High	1.07		- 1		I
	209	424		27.9	15. 1	22, 4	- 1	1422	15.7	9.8	2.1	1	1409	1404	1		- 1		15, 3			Inciplent cavitation
	- 1		11.5				1430			1 1		1410		1	1410	1408	High	1,06	15.9			Cavitated
	210	421	11.3	25. 5	12.9	20. 1	1431	1435	13.5	7.6	3		1409	1405	1410	1409	Low	1.09				Cavitated
	210a	425	11.5	25.0	12.2	19.5	~		12.8	7.3	. 1						.	1.00				Cavitated
	210ь	425	11.5	29.8	17.1	24.3			17.6	11.9	4.3	' †					'	1.04	i (Incipient flashing
	211	424	11.4	36.8	24.0	31.3	1435	1430	30. 2	11,9	16.3	1398	1369	1350	1350	1350		3.33	15.0	11.6	1.05	Flashed
	212	424	11.5	40.0	27.4	34.7	1445	1440	30.8	12.4	17.0	1402	1375	1359	1359	1358	i 1	3, 43	15.3	12.1	.97	Flashed
	213	421	11.3	42. 2	29.6	37.0	1439	1430	30.7	13.4	17.0	1402	1380	1370	1370	1369	1 1	3, 30				
	214	424	- 1	39.0	26.2	33.8			27.3	21.3	12.6	1411		1410			None		15.3	12.8	. 73	Flashed
$\vdash \vdash$	214	424	11.5	39.0	40, 4	33.8	1433	1427	21.3	٤١.٥	14.0	1411	1411	1410	1412	1411	None	1.15	16,0			Liquid
19	215	427	11.6	42.5	29,4	37.0	1431	1425	30.6	24, 5	16. 1	1410	1410	1408	1411	1409	None	1, 11	15.9			Limid
1"	216	427	11.6	26.8	13.9	21, 2	1435	1427	14.7	8.8	1. 1	1110	1410	1409	1				10.0	- 1	1	Liquid
	- 1							1421						1	1411	1410	None,'High	1.05				Incipient cavitation Pressure
	217	425	11,5	25. 2	12.3	19.7			12, 9	7.0	8						Low	1.07				Cavitated ramp
1 1	218	425	11.5	29.7	16.8	24.3		(17.6	11.7	3.5	•	([{	[Low	1.09	† [Incipient flashing
]	219	424	11.4	40.6	27.9	35.1	1432	1425	29.9	11.8	16.6	1392	1368	1350	1350	1349	Low	3, 32	14.5	11.5	0.94	Flashed
100		104	1	47 0	40.0	40.0		000		41.0	10.5	210			210							
20	s	124	0.9	43.0	42.0	42.6	965	962	41.7	41.3	40.7	949	949	942	946	945	None	1.00	0.7]	All-liquid flow calibration
	t	248	3,6	45, 4	41.5	43.7	924	922	43.4	41.6	39.3	905	903	900	903	900	1 1	1.06	.4	{		1
	u	373	8.0	38.6	29.6	34.7	828	828	34.1	29.9	24.4	822	820	818	820	818]	1.08	.2]	, <u>,</u> !
	v	495	14.0	45.4	29.6	38.6	851	851	37, 6	30.4	20.9	842	845	842	845	841	1 1	1,06	- 1 L			
1	w	619	21.9	54.1	29.7	43.7	838	835	42, 2	31.1	16.1	828	830	828	830	829] [1.07				j l
			3			1			1	31.3		842	845	843	846		. ↓ . [1.07	† [1	- 1	₩ 1
1 1	у	660	25.0	57.4	29,6	45, 6	853	850	43.9		14.2					845				~		

aShown only for flashed runs.

TABLE III. - Continued. DETAILED DATA FOR VENTURI WITH ARTIFICIAL THROAT CAVITY (SERIES II)

											(b) S	I units	a							
Set	Run		Dynamic		Con	trol ven	turi					Tes	t venturi				Noise	Pressure-	Vapor	Vapor
		rate, W, g/sec	head, q, N/cm ²		Pressur N/cm ² al		Tempo	erature, K	1	Pressur N/cm ² a	re, lbs	1	Т	emperatu K	re,		indica- tion	drop ratio, P ₄ - P ₅	pressure at T _{in} , P _{vin} ,	pressure at T _{out} , P _{vout} ,
			}	Inlet,	Throat,	Outlet,	Inlet,	Outlet,	Inlet,	Outlet,	Throat,	Inlet,	Dista	nce from	inlet	Outlet,		P ₁ - P ₃		N/cm ² abs
				P ₁	P ₂	P ₃	T _{C1}	T _{C2}	P ₄	P ₅	Pt	Tin	2.3 cm, T ₂	3.3 cm, T ₃	4.3 cm, T ₄	Tout			Nyoni abs	N/CHI abs
11	h	68.7	13, 0	35.9	21.6	29.9	1026	1023	29.0	22.7	14.1	1018	1018	1017	1020	1019	None	1.04	9.0	
	j (75.6	15, 7	38.7	21.5	31,6	1022	1019	30.6	22.9	12.1	1015	1015	1014	1016	1016	. 1	1.08	8.8	
	k	60.6	10.1	32.6	21.7	28. 1	1026	1023	27, 4	22.4	15.4	1017	1017	1016	1018	1017		1.10	9.0	
	m	52,8	7.7	30.1		26.5	1015	1012	26. 1	22.3	17.1	1005	1005	1005	1006	1006		1.07	8.0	
] n	45.4	5. 7	27.9	1	25.3	1013	1010	24. 9	22.1	18.2	1003	1003	1002	1004	1004)]	1.07	7.8	
	р	37.4	3.9	25.9	*	24.1	1024	1025	23.9	21.9	19.3	1011	1010	1010	1012	1011	1 1	1.06	8,8	
!	q	30, 2	2, 5	24. 3	21.6	23.1	1024	1021	23.0	21.7	20, 1	1011	1010	1009	1010	1010	}	1.03	8, 3	
	r	15.0	.6	28.7	27.9	28.3	1043	1041	28.3	28.0	27. 6	1026	1026	1024	1026	1025	· · · · · · · · · · · · · · · · · · ·	. 87	9.8	
12	73	61.2	10.1	37.6	26.5	33.1	990	986	26.8	21.7	14, 1	979	979	978	981	981	None	1, 14	6.1	
Į	74	61.6	10.3	35.4	24.1	30.8	993	990	24.3	19.2	12.1	983	983	980	983	983	ll	1.08	6.3	
	75	61.4	10, 2	31.1	19.8	26.3	993	990	19.9	14.8	8.0	983	983	980	983	983	ļ <u> </u>	1.05	6.3	
	76	61.0	10.1	28.8	17.6	24.0	991	989	17.6	12.5	5.6	981	981	979	983	982		1.07	6, 3	
1	77	61.2	1	27.6	16.3	22.8	989	986	16.4	11.3	4.4	979		977	979	979	None/High	1.06	6.1	
i	78	61.4		26.6	15.2	21.8	990	988	15. 2	10.1	3.0	980	1	979	982	981	High	1.07	6.2	
ĺ	79	61.4	1	25.5	14.1	20.7	990	988	14. 1	9,0	2.1	981		979 979	982 983	981 982	High Medium	1.05 1.06	6.2	
	80	61.4		23.9	12.5	19.1	990	987	12.5	7.3	8.8	989	1	986	988	987	Low	2.89	6.8	6.6
l	81	60.9	1	31.1		26.5	997	994	20. 1	6.1	8.1	983	1	972	975	974	2011	2.92	6.3	5,7
	82	61.0	1 1	30.0	1	24.3	995		19.9	5,6	8.0	982	1	966	967	966	1 1	2.99	6.3	5, 2
ĺ	84	61.0	1 1	28.6		23.9	995	1	20.0	1	8.0	979	1	964	966	965]]	3, 09	6, 1	5, 2
)	85	61.6	1	28.8	}	24. 1	995	ì	20, 2	1	8.1	980	972	967	971	971	} }	3.04	6, 2	5, 6
1	86	61.2		29.6	1	24.8	993	991	20.0	6.9	8.0	983	982	979	983	983	\	2.74	6.3	6.3
	87	60.9	1 .	29, 5	18.1	24,6	990	988	19.9	7.7	7.9	982	980	978	983	981	Medium	2.54	6.3	6.3
(88	61, 2	10.1	25.6	14.3	20.9	978	975	14.6	9.4	2, 3	971	970	967	971	971	High	1.09	5, 6	~
1	89	61.6	10.3	26. 5	15, 2	21,8	982	979	15.6	10, 4	3.2	972	972	971	972	971	High	1.08	5. 7	
	90	61.5	10.2	27. 9	16.5	23. 1	983	980	16.8	11.7	4.6	972	1	971	973	972	High	1.07	5. 7	
}	91	61.5	10, 2	27.9		23.0	983	1	16.8	1	4.5	973		971	973	972	None	1.08	5. 7	
1	92	61, 2	10.1	29, 2	2 17.7	24.3	980	979	18.1	13.0	5.9	971	971	969	972	971	None	1.07	5.6	
}	93	61, 2	10.1	27.4	16.0	22.7	986	983	16.4	11.2	3.9	977	977	974	978	977	None	1.09	6.0	
1	94	61.2		26.0		21, 3	987	1	15,0	1	2.6	977	977	974	978	977	1 1	1.10	6.0	
	95	60.9	1 1	25.2		1	991	1	14.3	9,1	2.1	981	981	978	983	982		1.08	6.2	
	96			24.4	13.2	19.7	993	989	13.4	8.3	1.4	983	983	981	983	983	1 [1.07	6.3	
	97	61.6	10,3	24.2	12, 7	19.3	992	989	13.0		8.	1	983	980	983	983	!	1,06		
1	98	61.0	10.1	23.	2 11.7		993	990	12. 1	1	1	1 1	983	982	984	983	High	1.07		
1	98	a 61. 1	1 1	23.	1 '				11.7	1	3	1 1				070	Medium/Lov	1 -	1	6.0
}	99		1 1	29.		1			20.3	1	8.3		978	977	978	978	Low	3.06	6.7	6.0
1	100	1	1 1	29,		1	1	1	1	1	8.5	1	1	985	988	988	Medium High	2,80	6.8	6.8
1	101	1	} }	29.					20, 8	1	8.5	1	1	988	989	989	High	1, 10	6.7	0.8
	102	1	1 1	24.	1		999		15.	1	3.9	1	. 1	980	984	984	None	1.11	6, 3	
	103	1		25.		1	- 1	i .	1 .			- 1	1	1	981	981	None	1.07	6, 2	

			40.0																	
13		61.7		27.9	16.3	23, 1	991	989	18.6	13.3	5.8	982	982	, 980	983	983	None	1.11	6.3	
į		61.7		21,6	10.1	16.8			12.1	6.9	3	983					High	1.07	6.3	
ì		61,7	10.3	20, 5	9, 0	15.8			11.2	6.0	-1.5	984					High Low	1, 10	6.3	
}	106	46.4	5. 9	21.4	14.8	18.5	1025	1022	16.0	6.1	. 8.7	1003	988	979	978	977	Low	3.45	7.7	5. 9
<u> </u>	107	60, 9	10. 1	27. 5	16.2	22.8	991	989	18.5	13.2	6,1	982	981	980	983	981	None	1.10	6.3	
14	108	45.5	5. 6	30.5	24, 2	27.8	972	969	15.6	12.8	9.2	960	960	9 59	962	961	None	1.02	5, 0	
1	109	45.6	5.6	27.9	21.7	25.3	972	970	13.0	10.1	6.1	961	960	959	962	960	None	1.12	5, 1	
ì	109a	45, 1	5.4	25.7	19.4	22, 9			10.8	8.0	. 4.7	961					None/High	.97	5. 1	
	110	45.1	5.4	25.4	19.4	22.8	1 972	970	10.7	8.0	4.4	961	960	959	962	960	High	1.03	5, 0	
ĺ	111	44.7	5.4	24.0	18.1	21,4	971	969	9.4	6.6	3.0	960	958	. 957	959	958	Ĭ	1.07	5.0	
	112	45.4	5, 5	22,7	16.6	20.1	965	963	8.3	5. 5	1.9	954	953	951	954	953	1	1,06	4.7	
	113	44.7	5.4	21.4	15.5	18.8	964	961	7.3	4,6	1.1	952.	951	950	953	952	†	1,06	4.6	
i	114	44.7	5.4	20.8	14.9	18.3	962	960	6, 7	3.9	. 3	951	950	949	951	950	Medium	1.08	4.6	
	115	45.1	5.4	20.4.	14.4	17.8	961	958	6. 1	3.4	-, 1	950	949	949	950	950	Low	1.04	4, 5	
	116	44.5	5, 3	19,9	14.1	17.4	961	958	6.0	3.3	2	949	949	947	950	949	1	1.06	4.4	
١.,	117	45.7	5. 6	14.4	8. 1	11. 7	958	956	6, 1	3, 3	-, 4	949	947	946	948	947	ı	1. 04	4.4	
	118	- 1	1	18.5	12, 5	15.9	956	953	6.0	3.2	6	944	943	942	944	943	- 1	1.10	4.3	
	118a			19.9	13.8	17.3			6.9	4.1	.3	944					- 1	1.05	1	
	119		1	19.9	13.9	17, 3	956	954	11.2	4.1	4.8	944	938	936	938	936		2.75		3.9
	120	•	ŧ	21. 5	15.5	19.0	956	954	11.3	5.4	5.4	945	943	943	945	944	• 🛊	2.37	,] .	4.2
	121	45.4	5.5	22.9	16,8	20.3	957	955	9.4	6.7	3.0	945	945	943	945	944	High	1.06		
	122	45.4	5. 5	24. 3	18.3	21.7	958	956	10.9	8.1	4.6	946	947	945	948	948	High	1.04	. ↓ ;	
1	123	45, 5	5. 6	25, 5	19.3	22.8	959	957	11.9	9.0	5.2	949	948	946	949	948	None	1.07	4.4	
-				+		-														
15	124	45, 5	5, 7	25.4	19.3	22. 9	997	994	11.9	9.0	5.2	984	984	983	985	983	None	1.08	6.4	
- 1	125	45, 4	5, 6	24. 1	17. 9	21.4	999	995	10.3	7.6	3.9	986	986	984	988	987	High	1.04	6.6	
	125a	1	i	23.0	16.9	20.7			9.2	6.6	2.4	986					High/Low	1.15	6.6	
- 1	126	- 1 1		27.4	21.3	24.8	1000	997	13.8	6.3	7.4	986	978	977	979	978	Low	2.81	6.6	6.0
- 1	127	7	Y	27.6	21.4	25.0	1003	1000	14.0	5.5	7.6	984	972	966	967	966	1 1	3. 17	6.4	5. 3
- 1	128	45, 5	5.7	21.0	14.9	18.3	1000	997	13.9	5, 1	7.7	983	967	961	961	960		3.38	6, 3	5. 0
- 1	129	45.4	5, 6	20.3	14.2	17.7	997	994	13, 8	4.8	7.1	979	965	956	956	955	1	3.32	6.1	4,8
J	130	45.4	ļ	20.3		17.6	997	994	13,8	5.5	7.4	980	969	964	966	965	i	3.08	6.1	5, 2
	131	45.4	- 1	20.3	1	17.7	995	993	13.9	6.6	7.4	983	980	978	983	979	1 1	2.05	6.3	6. 1
- 1	132	45. 7	1	20.4	•	17.7	994	990	13, 8	7.3	7.2	983	980	978	983	979	, ₹	2.39	6.3	6.1
Į	133	45.4	7	19.0	12.9	16.3	993	989	11.7	8.8	5. 2	980	980	978	982	981	None	1.05	6.2	
- 1	134	44.7	5. 4	19.9	13.8	17, 2	994	991	12, 6	9.9	6, 2	983	983	980	983	982	None	1.06	6,3	
ł	135	45.4	5. 6	18.9	12.7	16, 2	995	991	11.4	8.6	5.0	983	983	980	983	982	1	1.03	6.3	
	136		0.0	17.8	11.5	15.0	997	994	10, 3	7.5	3.8	988	988	985	988	986		1.05	6.7	
l	136a	-	- {	16.9	10.6	14.3			9.3	6.6	2, 7	988					<u> </u>	1.05	6.7	
ļ	137			21.6	15.4	19.0	1000	997	14.2	6.7	7. 7	988	981	978	979	978		2.88	6,7	6.0
1	138		- 1	21.5	15.3	18.9	1000	997	14.1	5, 5	7.6	983	972	966	967	966		3, 24	6.3	5, 3
-	139			22. 1	15.9	19.4		998	1	5. 2	7. 7	983	967	961	961	961		3.44	6.3	5.0
ı	140	. ↓ l	¥	22. 1	15.8	19.5		997		5.0	7. 5	983	967	960	960	958		3.49	6.3	4.9
- 1	141	45.0	5.5	21.9	15.8	19.3	1001	1000	 	6.6	7.7	988	983	978	980	979	♦	2.89	6,7	6.1
- 1	142	45. 1	5. 6	22, 1	15.8	19.4	999	995	14. 2	7. 0	7.7	300	984	983	984	983	Low	2. 69	";'	6, 3
- 1			5.6	22. 1	15.8	19.4	999	996	14. 1	8.1	7.6		985	984	988	986	Medium	2.71		6.6
	143	45.1		1 1	1		999	996	11.9	9.0	5.1	1	986	984	988	986	Medium None	2.28 1.11	. ↓	6. 6
	144	45, 4	5.6	19.9	13.7	17. 2	333	990	11.9	5. U	J. 1	_ ' _	900	204	206	307	Hone	1, 11		

^aFor quality values and remarks see table III(a). ^bShown only for flashed runs.

(b) Concluded. SI unitsa

Set Run	n I	Flow	Dynamic		Con	trol ven	turi					Tes	t venturi					Pressure	Vapor	Vapor
	١,	rate,	head,		Pressur	e.	Temp	rature.		Pressur	e,		Т	emperatu	re,		indica - tion	drop ratio,	pressure	pressure b
	ę	W, g∕sec	q, N/cm ²		N/cm ² al		,	к	1	√cm² a	bs			K			tion	P ₄ - P ₅	at T _{in} , P _{vin} ,	at Tout'
				Inlet,	Throat,	Outlet,	Inlet,	Outlet,	Inlet,	Outlet,	Throat,	Inlet,	Dista	nce from	inlet	Outlet,		P ₁ - P ₃	N/cm ² abs	N/cm ² abs
1	1			P ₁	P ₂	P ₃	TC1	T _{C2}	P ₄	P ₅	Pt	Tin	2.3 cm,	3.3 cm,	4.3 cm,	Tout			1	
					1								т2	т ₃	Т4					
16 145	,	44.3	5. 4	25. 2	19.1	22,6	1058	1055	17. 5	14.7	10.8	1044	1044	1042	1044	1044	None	1.10	11.5	
146	;	44.3	5.4	23.9	17.9	21.4	1058	1055	16.2	13.4	9.5	1045	1044	1044	1045	1044	None	1.11	11.6	
147	7	44. ß	5.5	20, 0	(17.4	1059	1055	12.2	9.4	5.7		1045	1044	1045	1044	None	1,06	11.7	
147	7a.	45.0	5, 6	19,0		16.5			11.0	8.3	4.3	l I					Medium	1.11	11.7	
147	7b	1	1 1	18.8	12.7	16.3			10, 8	8.2	4.4						Low	1.06	11.7	
148	3			25.9		23.3	1064	1059	18.1	8.5	11.6	1038	1018	1007	1006	1006	l I	3,65	10.8	8.1
149	1	*	1	25.9		23.2	1064	1061	18, 1	8.2	11.6	1038	1018	1006	1005	1004		3.81	10.9	7.9
150	- 1	44.6	5.5	25, 7		23.2	1064	1060	18.0	8.5	11.6	1038	1020	1010	1008	1007		3.71	10.9	8, 1
151	- 1	44.4	5.4	26.0	1	23.5	1066	1061	18.2	9.0	11.8	1039	1023	1015	1014	1014		3.67	11.0	8.6
152		44.6	5.5	26.0		23.4	1064	1058	18.2	9.6	11.7	1039	1024	1020	1021	1021		3.35	11.0	9.3
153	- 1	44.6	5.5	26.0		23.4	1061	1058	18.3	10.3	11.8	1041	1028	1027	1027	1027	1 1	3.14	11.2	9.9
154	- 1	44.4	5.4	26.1	1	23, 6	1060	1055	18.5	11.0	12. 1	1044	1034	1033	1033	1033	1	2.98	11.5	10.4
155	5	44,6	5.5	26.9	1	24.3	1058	1055	19.2	12.0	12, 7	1044	1041	1040	1041	1040	{ 1	2.77	11.5	11.1
156	6	44.4	5, 4	26,8	1	24.2	1063	1059	19.7	12.6	13.2	1049	1045	1044	1045	1044	, v	2.76	12.1	11.5
157	7	44.7	5.6	26, 9	1	24.3	1062	1059	19.7	13.3	13.2	1050	1048	1045	1050	1049	Medium	2.45	12.1	11.9
158	8	44.7	5, 6	31.2	25.0	28.6	1061	1058	17. 3	14.5	10.5	1048	1045	1045	1048	1046	None	1, 11	11.9	
159	9	45,4	5.7	24.8	18.5	22,4	1060	1056	17.0	14.3	10.1	1046	1045	1044	1046	1045	None	1.08	8.3	
160	0	45, 1	1	22.	16.5	20.0	1059	1056	15.2	12.3	8.7	1045	1043	1043	1046	1044	None	1.06	11.7	
161	1	1	1	20.1	7 14.6	18.0	1061	1058	13.2	10.3	6.8	1047	1047	1046	1046	1047	None	1.04	11.8	
161	1a		1 1	19.4	13.3	16.8			11.8	9.1	5.6	1047				1	None/Medium	1.03	11.8	
161	1b		+	19.6	13.0	16.5			11.4	8.8	5.2	1047				:	Medium/Low	1.03	11.8	,
162	2	45.0	5.6	25.	9 19.7	23.2	1067	1064	18.3	8.9	11.8	1041	1023	1014	1013	1013	Low	3, 54	11.2	8.6
163	3	45, 4	5.7	26.	20.4	24.0	1072	1069	19.1	10.1	12.5	1049	1032	1025	1025	1025	Low	3.50	11.9	9.7
164	4	45.1	5.7	23.	16.9	20.3	1065	1061	15.6	12.8	9.1	1051	1050	1049	1051	1050	None	1.06	12, 2	!
165	5	lι	! 1	21.9	15.7	19.2	1071	1067	14.3	11.4	7.8	1056	1055	1054	1056	1055	1 1	1.06	12.8	
160	6]]	1	20.	3 14.1	17.7	1072	1069	12.8	9.9	6.2	1058	1057	1055	1056	1056	1 1	1,06	13.0	
160	6a		1	19.	4 13.4	16.8			11.8	9.1	5.8	1058						1.00	13.0	
16	7	44.6	5.5	25.	9 19.9	23.4	1072	1068	18.6	9.2	12.3	1044	1025	1016	1016	1016	1 1	3.81	11.5	9.3
16	8	45.0	5.7	30.	B 24.7	28.1	1071	1069	20, 2	13.2	13.8	1056	1051	1050	1051	1051	1.1	2.69	12.8	12, 2
169	9	45.4	5.7	30.	8 24.5	28.1	1071	1067	20.0	17.2	13,4	1056	1056	1055	1059	1056	*	1.06	12.8	
170	0	45.0	5.7	27.			1069	1066	16.3	13.6	10.1	1056	1055	1054	1056	1055	None	1.02	12.7	
17	71	44.4	5.5	24.	9 18.9	22.3	1065	1065	14.2	11.4	7.9	1053	1051	1051	1053	1052	11	1.06	12.4	
17	72	45.0	5.6	23.	6 17.6	21.0	1060	1058	12.8	10.0	6, 5	1048	1047	1046	1048	1048	1.1	1.03	11.9	
17	13	45.4	5.7	22.	5 16.3	19.8	1061	1057	11.5	8.7	5.2	1047	1046	1045	1048	1046	1	1,03	11.8	·
17	73a	45.0	5.6	21.	2 15.3	18.8			10.4	7.7	3.7	1047					None/High/Low	1, 11	11.8	
17		44.7	5.6	24.	5 18.5		1059		13.8			1045	1	1043	1044	1044	None	1.06	11.7	
17		45.0	5.6	23.			1057	1054	12.3			1044		1042	1043	1043	None	1.06	11.5	
17	75a	44.	5,6	21,	9 15.9	19,4			11.0			1044	1			 -	None/Low/Non-		11.5	
17	76	37.4	3.9	22.	5 18.2	20.8	1061	1056	14.8	8.3	10.3	1033	1013	1005	1005	1005	None	3,64	10.4	8.0

	1 1 25	T				7			·				7					,		<u>-</u> -	_
1		60.6	t .	37.5			. 1047	, 1044	21.7	16.7	9.7	1038	1036	1034	1038	1036	None	1.08	10.8		
	178	60.4	,	, 30, 9		26, 2	1050	1047	20.0	14.9	7.9	1039	1039	1038	1039	1039	()	1.07	11.0		
	179	60.7		29,6	1	24.8	1050	1047	18. 5	13.4	6.5		1039	1038	1 1	1039	i	1.06	1 1		
	180	60,6	1	28. 2	1	23, 3	1049	1044	17.1	11.9	5. 1	11	1038	1036		1038	11	1.06			ŀ
	181	60.7	10, 2	26.9	15, 5	22.0	1049	1046	15.7	10, 5	3.7	1	1038	1036		1038	1	1,06	i l		- 1
	182	60, 6	10.1	25.6	14.2	20.8	1050	1047	14.5	9.3	2. 1	1	1039	1038	†	1039	Low/High/Low	1.09	†		
	183	60.7	10.2	31.4	20.0	26.5	1050	1047	24.7	9.2	12.3	1033	1021	1016	1016	1016	Low	3, 15	10.4	8.8	
1	184	60.4	10.1	31.6	20.1	26.8	1053	1050	24.8	8.8	12.3	1033	1021	1011	1011	1011	1 .	3.31	10.4	8.4	-
i	185	60, 4	10, 1	31.3	20.1	26,6	1 1	1050	24.7	9.8	12.5	1034	1025	1021	1022	1021	1 1	3,20	10, 5	9.3	ì
i	186	60, 6	10, 2	33.2	22, 0	28, 5		1050	25.0	11.1	12.8	1040	1035	1033	1034	1034	†	2.94	11.1	10.5	-{
- }	187	60, 6	1	34.9	23, 6	30, 1	1 🕴	1049	25, 1	12, 3	12.9	1040	1039	1038	1039	1039	Medium	2, 73	11.1	11,0	-
ŀ	188	60.6		35.6	24, 2	30.8	1050	1047	25.0	13, 3	12, 7	1039	1039	1038	1039	1039	Medium	2, 42	11, 0	11.0	
1	189	60, 7	 	36, 2	24, 9	31.4	1049	1045	24.8	14.3	12.5	1 .	1038	1036	1039	1038	Medium	2,07	1	10.9	
	190	61.0	10, 3	32, 1	20. 5	27. 2	1050	1047	20. 5	15.3	8, 1		1039	1039	1040	1039	None	1.08	1 1		- (
	191	60.6	10, 1	33.6	1	28.7	1050	1045	22.1	17.0	10, 3		1039	1038	1039	1038	None	1, 03	1 1		ĺ
	1	1	10.1	35.0	22.2	20. 1	1000	1010		1	10.0	'	1000	1000	1000	1000	Hone	1,00	1		-
	192	60, 6	10.1	28.7	17.2	23.9	1047	1042	17.2	11.9	4.6	1036	1035	1034	1036	1035	None	1.09	10, 7		-
i	193	1 1	1 1	27.0	15.7	22.2	1047	1042	15. 5	10.3	3.2	1038	1036	1034	1038	1036	None	1,08	10, 8		ļ
1	193a			26.3	14.7	21.4			14.7	9.6	2.3	1038					None/High	1,06	10.8		1
	194		🕴	32, 6		28, 1	1047	1044	24.3	9.2	12.1	1032	1021	1016	1016	1016	Low	3, 31	10.3	8.8	
- (195		10.2	32,3	20.9	27.4	1053	1050	25, 3	12.1	13.0	1043	1040	1039	1043	1042	Low	2, 69	11,4	11.2	1
	196		10.1	33.9	22.5	29. 1	1050	1046	25.0	14.3	12.6	1039	1039	1036	1039	1039	Medium	2, 23	11.0	11, 0	
-	197	1 1	10.1	31.0	19.7	26.3	1048	1045	20. 1	14.9	7.7	1039	1038	1036	1039	1038	None	1.09	11.0		1
	198	↓	10.1	33. 4	22.0	28.6	1047	1044	22. 5	17.3	10.0	1038	1036	1034	1038	1037	None	1.10	10.8		1
	130	'	10.1	35. 4	22.0	20.0	1041] 1044	22.0	11.0	10.0	1000	1000	1007	1000	1001	None	1.10	10.0]	}
	199	60.6	10.1	42.1	30.9	37.2	1048	1045	22.5	17, 3	10.5	1039	1038	1038	1039	1038	None	1.08	11.0		
	200	60.4	l i	38.5	27.4	33.9	1048	1045	18.8	13.7	6.6	1038	1038	1035	1039	1038		1.10	10.9		
1	201	60.4	ii	36.1	24.9	31,4	1048	1044	16.3	11.1	3.9	1038	1038	1035	1039	1039	1 1	1.11	10.9		1
	202	60, 2		34.8	23, 7	30,2	1045	1043	15.0	9.9	2.6	1035	1034	1033	1036	1035	†	1.11	10.6		1
1	202a	60.2	,	34.3	23, 1	29.7			14. 1	9.0	1.8	1035					None/High/Low	1,09	10.6		1
	203	61.1	10.0	33.8	22, 5	29.0	1045	1042	24.3	8.8	11,8	1028	1017	1011	1011	1011	Low	3.30	10,0	8.4	Ì
J	204	60, 6	10.3	33.0	21.7	28.3	1041	1039	19.7	14.5	7.4	1033	1033	1029	1033	1033	None	1.08	10, 4		
\vdash							├─-						<u> </u>		 	 					4
18		53.8	8.0	26.7	17.8	22.9	1047	1044	18.3	14.2	8.8	1034	1034	1033	1034	1034	None	1.07	10.5		
	206	54.1	8.1	23.5	14.5	19.5	1047	1044	15.0	10.9	5, 5	1036	1036	1034	1038	1036	None	1,06	10.7		1
	207	53.4	7.9	21.7	12.9	17.9	1049	1045	13, 3	9.3	3, 9	1038	1037	1034	1038	1037	None	1.07	10.9		
	208	54.1	8. 1	20.9	11.8	17.0	1046	1044	12.3	8.1	2.5	1035	1034	1033	1035	1034	High	1,07	10, 5		1
	209	53, 4	7.9	19.2	10.4	15.4	1050	1045	10.8	6.8	1.4	1039	1038	1035	1039	1038	High	1.06	11.0		1
1	210	53.0	7.8	17.6	8.9	13.9	1050	1053	9.3	5. 2	-, 2		1038	1036	1039	1038	Low	1.09]]		J
1	210a	53, 6	7.9	17. 2	8.4	13.4			8.8	5.0	. 1	i I						1,00			1
1	210b	53.6	1	20.5	11.8	16.8			12. 1	8.2	3,0	1						1.04	1		1
1	211	53.4		25.4	16, 5	21.6	1053	1050	20.8	8.2	11, 2	1032	1016	1005	1005	1005		3.33	10.3	8.0	İ
1	212	53.4	†	27.6	18, 9	23.9	1058	1055	21. 2	8.5	11,7	1034	1019	1010	1010	1010		3, 43	10.5	8.3	
1	213	53.0	7.8	29.1	20. 4	25. 5	1055	1050	21. 2	9.2	11,7	1034	1022	1017	1017	1016	†	3,30	10.5	8.8	1
	214	53, 4	7.9	26.9	18.1	23.3	1051	1048	18.8	14.7	8.7	1039	1039	1039	1040	1039	None	1, 15	11.0		
-	\vdash	-	-	 			 					<u> </u>		ļ	 			 	 _		4
19	215	53.8	8.0	29.3	20.3	25.5	1050	1047	21.1	16.9	11, 1	1039	1039	1038	1039	1038	None	1.11	11.0		
1	216	53.8	8.0	18, 5	9.6	14.6	1053	1048	10. 1	6.1	. 8	1	1039	1038	1039	1039	None/High	1.05			
	217	53.6	7.9	17.4	8, 5	13.6			8.9	4.8	-, 6						Low	1,07			
1	218	53.6	7.9	20.5	11.6	16.8			12.1	8.1	2, 4	7					Low	1.09	1		İ
1	219	53.4	7. 9	28.0	19. 2	24. 2	1051	1047	20. 6	8. 1	11, 4	1029	1015	1005	1005	1005	Low	3, 32	10.0	7. 9	1
20	9	15,6	0.6	29.6	29.0	29.4	791	790	28.8	28.5	28, 1	783	783	779	781	780	None	1.00	0, 5		1
20	s l	31.2	2.5	31, 3	28,6	30.1	769	768	29.9	28.7	27, 1	758	757	755	757	755	1,0116	1.00	3		1
1		. 1		26, 6	20, 4	23.9	715	715	23.5	20.6	16.8	712	711	710	711	710	[1, 08	1		
	u	47.0	5.5	31.3	20.4	26.6	728	728	25. 9	21.0	14.4	723	725	723	725	710]	1,08	.1		
1	v	62.4	9.7				728	719	29.1	21.4	11.1	715	716	715	716	723		1,00			
1	w	78.0	15.1	37.3	20, 5	30.1								724	725		' ↓				1
<u></u>	у	83, 2	17.2	39,6	20.4	31.4	729	728	30.3	21.6	9.8	723	725	724	720	725	7	1,07	l ' l		Ł

y 83.2 17.2 39.6 20.4 31.4 aFor quality values and remarks see table III(a). bShown only for flashed runs.

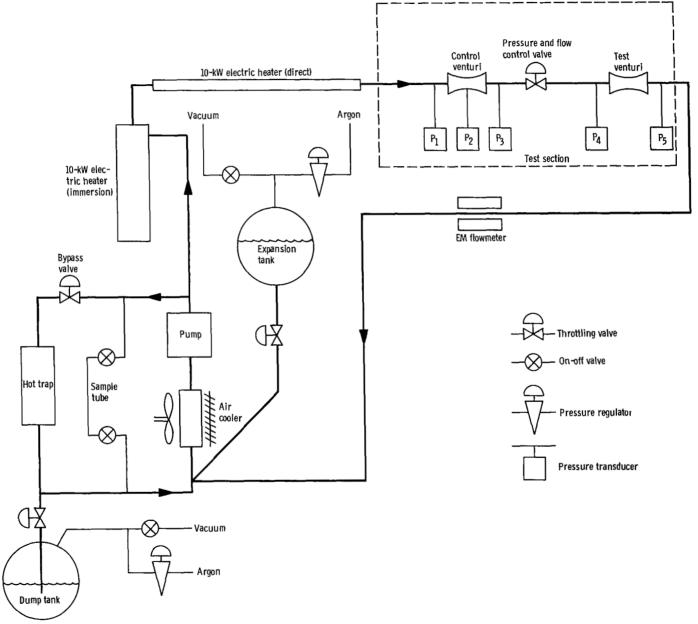


Figure 1. - Schematic diagram of test equipment.

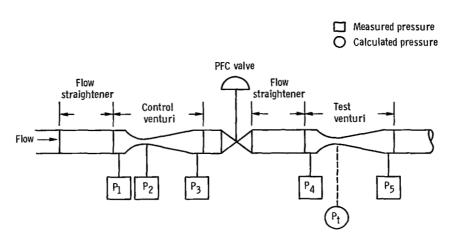


Figure 2. - Diagram of test section showing how test-venturi throat pressure is calculated from control-venturi-measured throat pressure, $P_t = P_4 - (P_1 - P_2)[(P_4 - P_5)/(P_1 - P_3)]$.

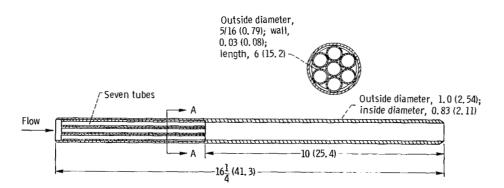
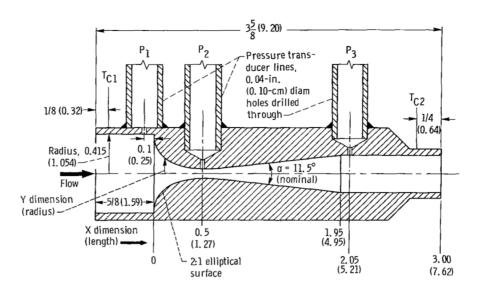
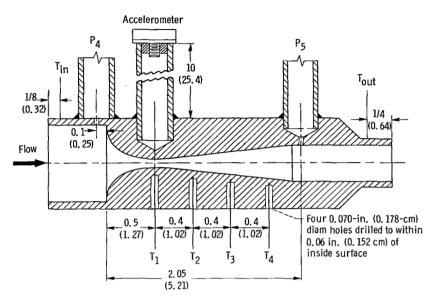


Figure 3. - Flow straighteners used directly upstream of both venturis. Material, type-316 stainless steel; dimensions are in inches (cm).



Venturi dimensions											
dime		rad	ius_	Toler in		dime		rad		Tolerance in Y	
in.	cm	in.	cm	in.	cm	in.	cm	in.	cm	in.	cm
0 .050 .100 .150 .200 .250 .350 .400 .450	0 .127 .254 .381 .508 .635 .762 .889 1.016 1.143 1.270 1.397	0.300 .189 .150 .121 .100 .084 .071 .062 .055 .051	. 480			0. 750 . 800 . 850 . 900 . 950 1. 000 1. 100 1. 200	1. 905 2. 032 2. 159 2. 286 2. 413 2. 540 2. 794 3. 048 3. 307 3. 556 3. 810 4. 064	. 079 . 080 . 085 . 090 . 095	0. 178 . 191 . 203 . 216 . 229 . 241 . 257 . 292 . 318 . 343 . 369 . 394	+0.002 +.004 +.004 +.005	+. 010 +. 010 +. 013
.600	1. 524 1. 651 1. 778	.055	. 140 . 152 . 165	+.002 +.002 +.002	+.005 +.005 +.005		4. 318 4. 572 4. 826 4. 953 5. 207	. 165 . 175 . 185 . 190 . 190	. 419 . 445 . 470 . 483 . 483		

Figure 4. - Control venturi. Dimensions are in inches (cm); all tolerances, -0.000.



(a) Test venturi without artificial throat cavity.

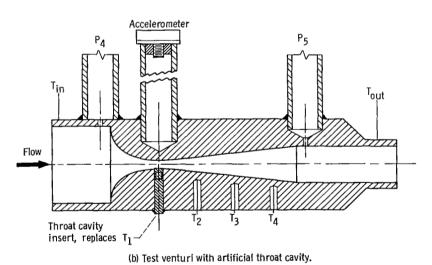


Figure 5. - Test venturi. Dimensions are in inches (cm).

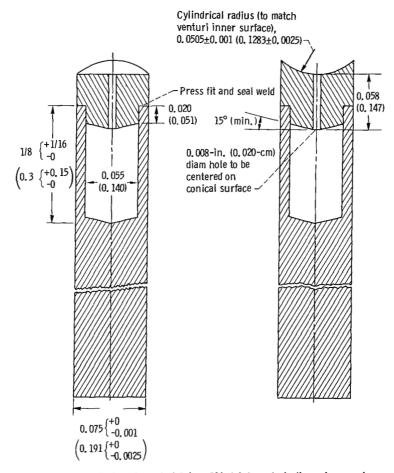


Figure 6. - Throat cavity insert. Material, type-316 stainless steel; dimensions are in inches (cm).

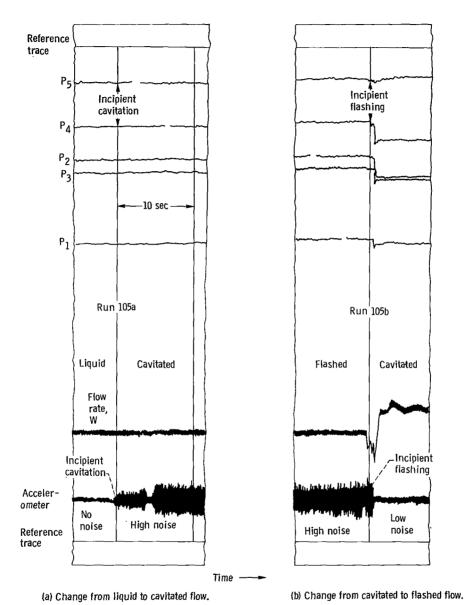


Figure 7. - Pressure decrease ramp between runs 105 and 106, set 13. Sections of oscillogram showing points of incipient cavitation and incipient flashing.

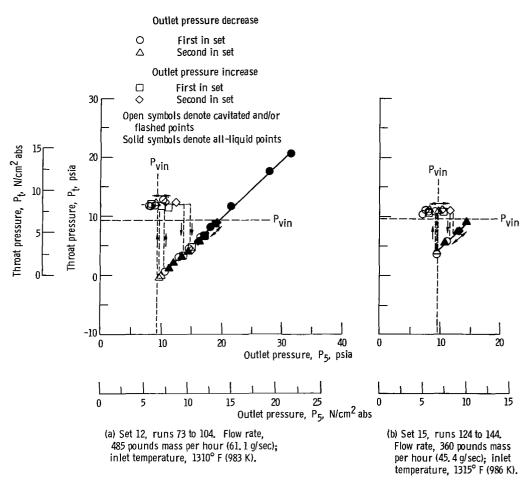
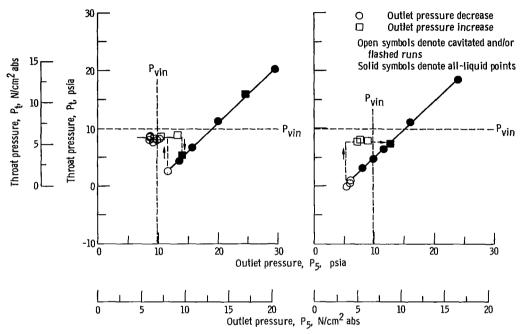


Figure 9. - Test venturi with artificial throat cavity: throat pressure as function of outlet pressure.



ture, 1315° F (986 K).

(a) Set 7, runs 41 to 55. Flow rate, 495 pounds mass per hour (62.4 g/sec). Inlet tempera-mass per hour (47.0 g/sec). Inlet temperature, 1315° F (986 K).

Figure 8. - Test venturi without artificial throat cavity: throat pressure as function of outlet pressure.

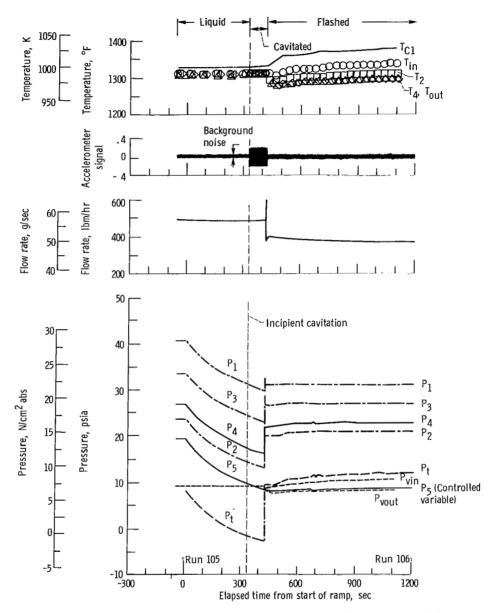


Figure 10. - Behavior of test venturi during pressure ramp between runs 105 and 106. Exit quality at 1200 seconds, approximately I percent; controlled variable, $\rm P_5$.

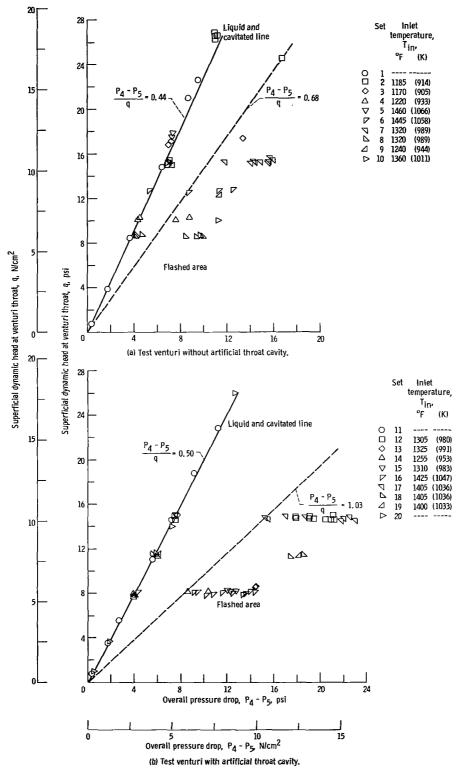


Figure 11. - Overall pressure drop as function of superficial dynamic head for all runs.

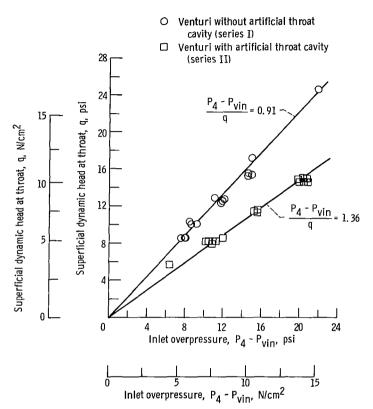


Figure 12. - Flashed venturi performance. Difference between venturi inlet pressure and potassium vapor pressure corresponding to inlet temperature $P_4 - P_{vin}$ (inlet overpressure) as function of superficial dynamic head at throat.

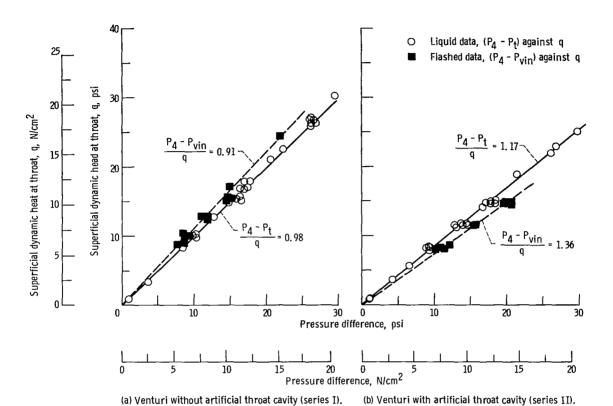
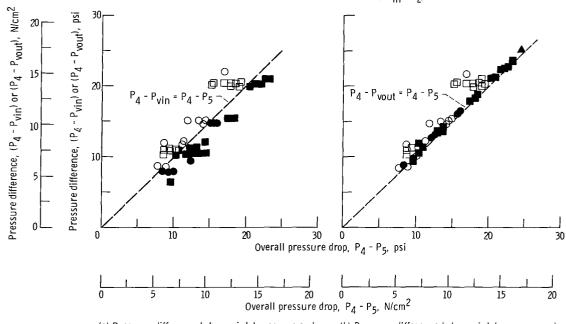


Figure 13. - Flashed venturi performance, nozzle section. Comparison of inlet overpressure for flashed runs P_4 - P_{vin} with all-liquid nozzle pressure drop to the throat P_4 - P_t as function of superficial dynamic head at throat.

Venturi without artificial throat cavity (series I) Venturi with artificial throat cavity (series II) Open symbols denote no temperature depression in venturi diffuser, T_{in} = T_{2} ; X = 0. Solid symbols denote temperature depression in venturi diffuser, $T_{in} > T_{2}$; X > 0.



(a) Pressure difference between inlet pressure and vapor pressure at inlet temperature, $\,{\rm P_4}$ - ${\rm P_{vin}}$.

(b) Pressure difference between inlet pressure and vapor pressure at outlet temperature, $\,{\rm P_4}$ - ${\rm P_{vout}}$.

Figure 14. - Flashed venturi performance, diffuser section. Effect of venturi backpressure on diffuser temperature and pressure drop.

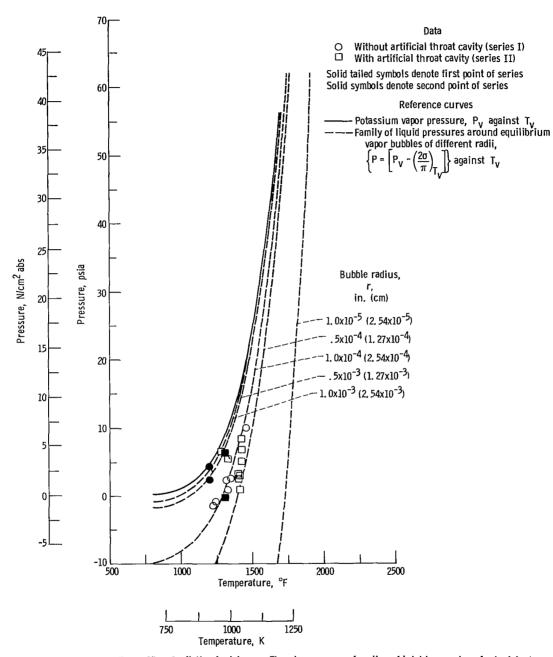


Figure 15. - Cavitation incipiency. Throat pressure as function of inlet temperature for incipient cavitation.

Data

O Without artificial throat cavity (series I)

☐ With artificial throat cavity (series II)

Solid tailed symbols denote first point of series

Solid tailed symbols denote first point of serie. Solid symbols denote second point of series

Reference curves

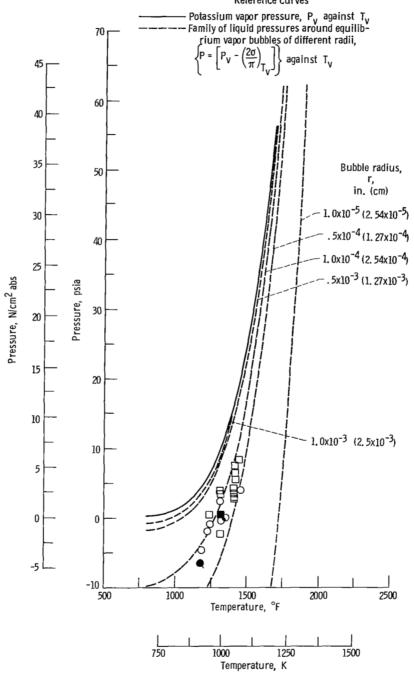
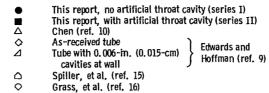


Figure 16. - Flashing incipiency. Throat pressure as function of inlet temperature for incipient flashing.



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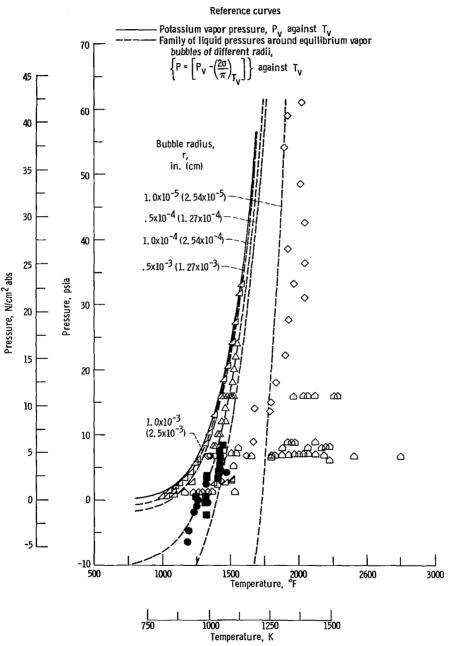
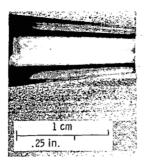
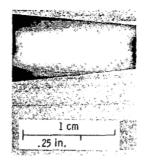
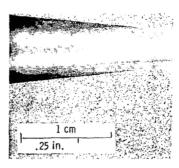


Figure 17. - Comparison of incipient flashing data with potassium data from other investigators; liquid minimum pressure as function of liquid temperature. See table in corresponding section of tests for comparison of test conditions.





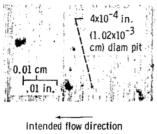


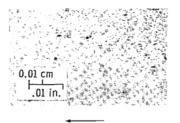
(a-1) As-received venturi.

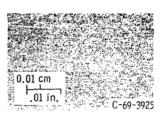
(a-2) Test venturi.

(a-3) Control venturi.

(a) Longitudinal sections of portion of diffusers. As-received venturi was not used. Sections from test and control venturis exposed to potassium flow for approximately 250 hours; note change in surface shine.







h. 1) As received wenturi

Flow direction

Flow direction

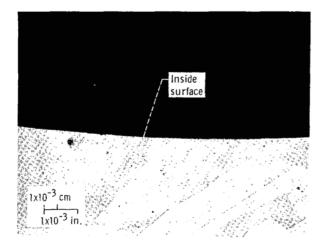
(b-1) As-received venturi.

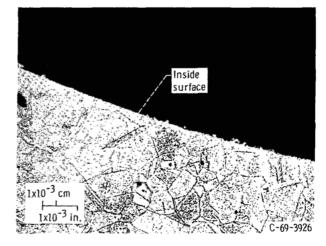
(b-2) Test venturi.

(b-3) Control venturi.

(b) Photomicrographs of venturi diffusers inside surfaces. Note polishing scratches and large-size pits in as-received venturi, and disappearance of these features in test and control venturis.

Figure 18. - Photographs of venturi taken normal to inside surface at diffuser.





(a) As-received venturi. Very smooth inside surface; no disturbances in surface can be appreciated. Notice large grains and absence of carbide precipitation in metal. (b) Test venturi. Rougher surface; small cavities in range of 10^{-4} to 10^{-5} inch $(2.54 \times 10^{-4}$ to 2.54×10^{-5} cm) can be seen on surface. Notice change in structure within metal and presence of intergranular and matrix carbide precipitation.

Figure 19. - Photomicrographs of venturi cross section showing edge of inside surface, taken at beginning of diffuser near throat. Material, type-316 stainless steel.

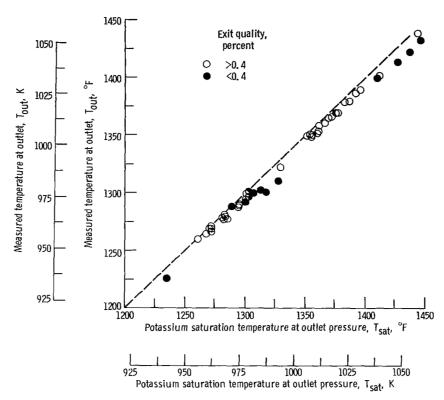


Figure 20. - Comparison of test venturi measured outlet temperature with corresponding potassium saturation temperature at outlet pressure. Flashed runs.

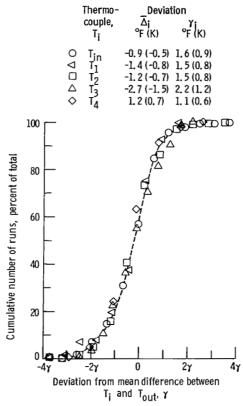


Figure 21. – Distribution of thermocouple reading deviations for thermocouples T_{in} , T_1 , T_2 , T_3 , and T_4 when compared to thermocouple T_{out} . All-liquid runs. $\gamma_i = \left[\Sigma(\Delta_i - \overline{\Delta_i})^2/N_i \right]^{1/2}; \ \overline{\Delta}_i = \Sigma \Delta_i/N_i;$ $\Delta_i = (T_i - T_{out})$ where $N_i =$ number of readings (56 for T_1 , 158 for all others).

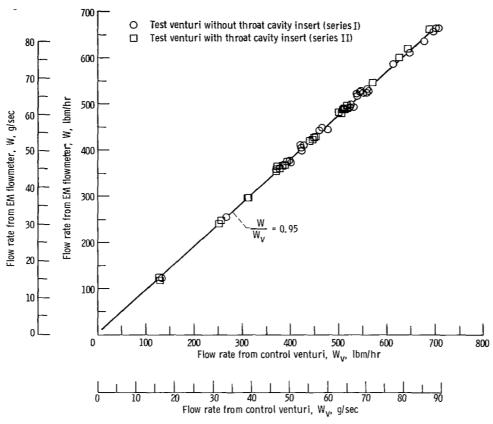


Figure 22. - Comparison of potassium flow rate data from electromagnetic flowmeter with those obtained from control venturi using results of water calibration of as-received venturi.

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